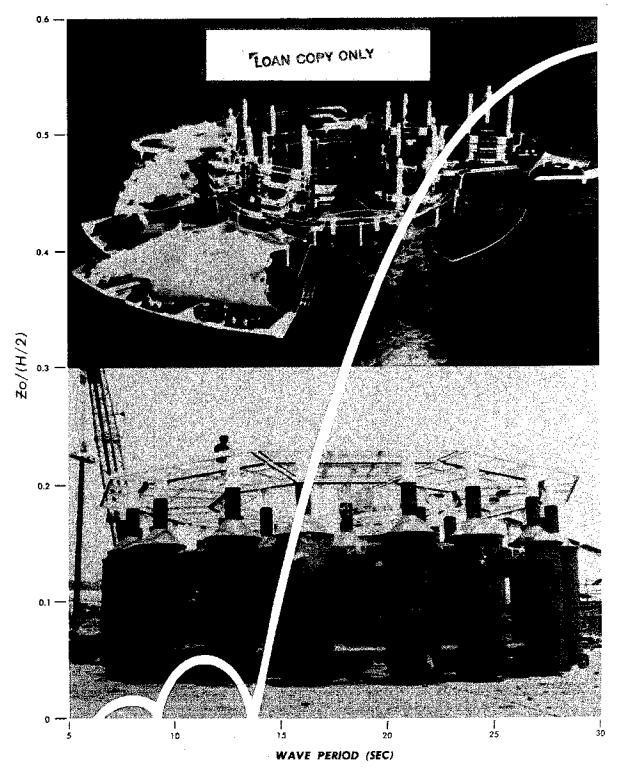
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INTERNAL THERMAL AND HUMIDITY CONTROL



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HAWAII'S FLOATING CITY DEVELOPMENT PROGRAM

Technical Report No. 3

UNIHI-SEAGRANT-CR-74-01

Internal Thermal and Humidity Control

by

Yoshihiko Yamashita Department of Mechanical Engineering University of Hawaii

November 1973

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ABSTRACT

This report is an investigation of some design aspects of a large floating platform to support urban activities in the Hawaiian Islands area. A brief account of weather and sea conditions in Hawaii is presented, with an analysis of human comfort requirements. Various types of air conditioning systems are described and choices are made for specific locations within the Floating City. Equations are presented and sample calculations are performed for determining cooling load, by the response factor method, for a superstructure and a buoyancy tank case. Preliminary air duct design is performed for both cases. Absorption-cycle refrigeration is discussed, and a flow diagram and calculations are given. A computer program which performs the response factor calculations is presented. Finally, several conclusions drawn from this work are reported.

AN INTRODUCTORY NOTE

During the time the research documented in this report was being conducted, Mr. Yamashita was pursuing his Master of Science degree at the University of Hawaii. His thesis, "A Calculation of Cooling Loads with Response Factors," developed the technique employed in this work, and this is its first professional application. Mr. Yamashita has been awarded his M.S. degree and is now a doctoral candidate. I believe the reader will agree that this is a thoroughly professional product and will understand the pleasure we take in Mr. Yamashita's association with the project.

The following Oceanic Foundation personnel contributed to the study: Mr. Guy N. Rothwell provided the bulk of the technical guidance for this work; Ms. Bonnie M. Rhodes was responsible for editing the manuscript; Ms. Diane J. Henderson prepared the illustrations and final manuscript; Ms. Joyce Miller assisted with the early writing and typing.

> Joe A. Hanson Program Manager

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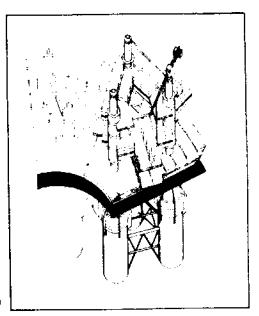
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INTRODUCTION

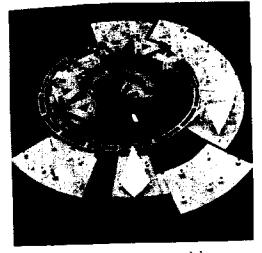
Hawaii's Floating City Project had its formal inception in 1970, with the award of a grant by the State of Hawaii to the Department of Architecture, University of Hawaii, for a project to investigate the

possibilities and opportunities that might lie in the construction of an urban center aboard a very large, deep-sea, floating platform. This work resulted in the conceptual design of a ring-shaped floating city with inner and outer rings consisting of up to thirty independently stable modules, all rigidly connected to form the final city, but separately removable for repair or renovation. The typical module would be supported from three or four vertically oriented, fully submerged buoyancy chambers, each topped by a structural column which would pass through the elevated main deck structure to form the core of a moderately high-rise superstructure building.



Typical module

The city was envisaged as housing a broad range of domestic, commercial, recreational, industrial and public activities, all served and supported by a complete suite of on-board public utilities, and linked with Honolulu and the world by a variety of transportation and communications services. In general, the industrial, utility and commercial services would utilize available space in the submerged buoyancy chambers. At the lowest levels would be found fuel and water storage, as well as sewage treatment facilities and variable ballast tanks. Above these would be power generation, air conditioning and desalination plants, as well as other machinery spaces. Also included would be warehousing and cold storage, maintenance and repair shops, and some commercial spaces, such as stores and offices. At the top of the buoyancy chambers, where windows on the sea could be provided, would be restaurants, apartments and places of public assembly.



Superstructure model

The main deck structure, located above the highest waves, would contain commercial and recreational facilities and transportation terminals. The weather surface of the main deck structure would be landscaped as a park. Finally, the superstructure would contain mainly living spaces, either apartments or hotel rooms.

Principal structural material was to be concrete. The city site was chosen as five miles south of Honolulu in the open ocean, where water depth is 600 meters.

In subsequent years, engineering studies of various aspects of this concept have been made, including environmental conditions of the site, hydrostatics and hydrodynamics of the city's form and feasibility of the modular approach. Studies for the current year include an analysis of concrete as a suitable material, a structural design investigation, a review of applicable transportation methods, a survey of potential construction sites and methods, and the study contained in this report.

Objectives, Scope, and Limits of the Present Study

The purpose of this study is to examine the requirements for internal environmental control, given the on-site environmental conditions and the configuration and projected occupancies of the city's enclosed spaces. Emphasis is placed on weather, air conditioning, duct design, and utilization of waste heat from the city's power plant. The report also develops a mathematical model for determining (and optimizing) the values of the various sources of heat gain, and suggests a total-energy approach to the design of the city's power plant, air conditioning plant, and freshwater distillation plant.

In view of the highly conceptual and schematic nature of the architectural design upon which this report (and others in this year's effort) are based, it has not been possible to make a detailed, realistic and quantitative inventory of occupancies, with their associated heat loads. Neither has it been possible to provide more than a schematic representation of the thermal properties of the exterior covering materials of the main deck and superstructure. Therefore, reasonable assumptions have been taken in both categories. Thus, though the results of the computer runs appear reasonable to the extent that certain important conclusions can be drawn from them, the numerical values obtained are not meant to apply for any specific floating platform that may in the future be built. This report does, however, claim to present a convenient method by which such values may be calculated when they are required.

<u>Contents of the Report</u>

Section I describes the analysis of weather conditions in Hawaii based on statistical data. Criteria for human confort are also established for Hawaiian weather conditions.

Section II describes several types of air-conditioning systems and their applications, according to the economic and thermal requirements of various classes of interior space.

Section III is a theoretical investigation of heat gains for the superstructure and buoyancy tanks in the Floating City. Section IV outlines the proposed procedure for calculation of cooling load in relation to Section III.

Section V contains sample calculations of cooling load for a superstructure element and for a buoyancy tank. The major effort has been put on the computer simulations for the analysis of cooling load in the superstructure.

Section VI describes the utilization of waste heat from the city's power plant. An absorption cycle using waste steam is suggested for refrigeration.

Section VII contains the design of ducts for the superstructure and buoyancy tanks, yielding the physical dimensions of ducting in relation to other space requirements.

The summary and conclusions are presented in Section VIII.

I. CLIMATE AND COMFORT

A. <u>Weather Data</u>

Hawaii's thermal and climatic conditions are well characterized by its exposure to the prevailing trade winds and its mid-oceanic location. The influence of the surrounding waters upon climate is considerable. In general, the trade winds flow in an east to west direction. Owing to the trades, showers are very common and cloudless skies are rare. The trade winds provide natural ventilation for the Hawaiian islands, bringing in mildly warm air that has moved great distances across subtropical seas. During the winter months, the persistent North Pacific cell of high barometric pressure tends to be displaced and occasionally broken up, allowing frontal storms to reach the islands. Accompanying these storms are sharp changes in wind direction, increased wind velocity and moderate to heavy precipitation. However, air temperature changes are not drastic, being moderated by the great temperature stability of the surrounding ocean surface.

There is relatively slight variation in the length of the daylight period in Hawaii in contrast with other areas, as shown in Table 1.

	North	Longe	est Day	Shortest Day	
City	latitude	hr	min	hr	min
Anchorage	61	24	0	7	30
Seattle	48	17	20	9	30
St. Louis	39	16	0	10	20
Atlanta	34	15	30	10	50
Honolulu	21	1 4	10	11	40

Table 1 - Comparative daylight periods (1)

An outstanding feature of the climate of Hawaii is the small annual temperature variation (Figure 1). In downtown Honolulu, the warmest

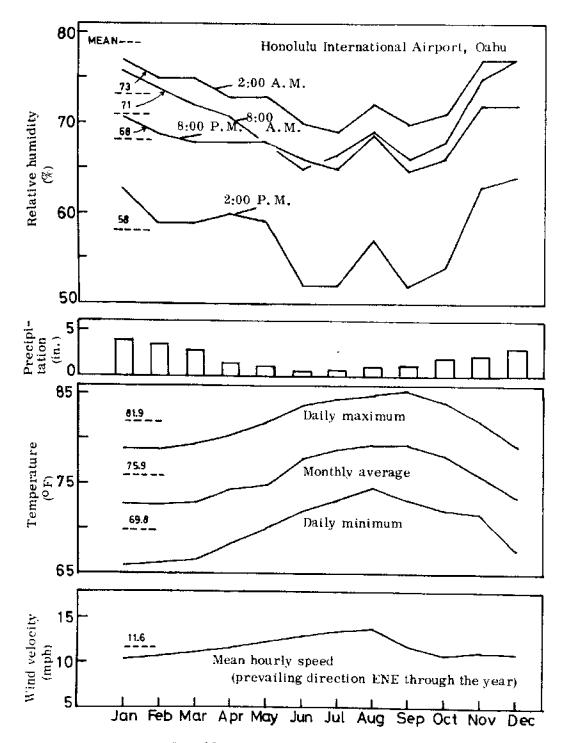


Figure 1 - Monthly average weather data in Honolulu (2).

month is August, with an average daily temperature of 78. 4° F, which is only 6.5° F higher than that for the coldest month of February.

Comparison of mean temperature ranges among the different cities in the Hawaiian islands is presented in Table 2. It shows fairly similar temperature variations except for the data taken at Mauna Loa.

	Elevation	Mean temperatures (^O F)			
Station	(ft)	January	August		
Hilo	40	71	76		
Olaa	280	70	75		
Mountain View	1,530	65	70		
Mauna Loa	11,150	41	47		
Honolulu Airport	7	73	78		

Table 2 - Mean temperature ranges in Hawaii (2)

August and September are the warmest months of the year throughout Hawaii. Figure 1 shows the monthly average temperatures at Honolulu Airport, which were taken for ten years from 1951 to 1960. In the same figure, the mean hourly speed of wind is plotted and the average of 11.6 mph is shown. Wind direction frequency is given in Table 3, as well as wind speed frequency, for the months of January and August.

Table 3 - Wind direction and speed in Honolulu (1, 2,)

Wind Direction Frequency January August Direction		Wind Speed Frequence Speed January Augus				
50%	93%	NNE to E	0-12 mph	68 <u>%</u>	38 ^G	
			13-24 mph	29%	58%	

The average relative humidity in the coastal areas and along the mountain ranges is 70 to 80 percent, while that for the leeward areas is 60 to 90 percent. Figure 1 shows the fairly constant relative humidity in Honolulu, which is largely due to the influence of the surrounding ocean.

The Hawaiian Sugar Planters Association has measured the total solar radiation, which is the sum of direct and diffuse solar radiation. Data from 16 years of measurements are plotted in Figure 2 in conjunction with the average temperature of outside air taken at the Honolulu Airport.

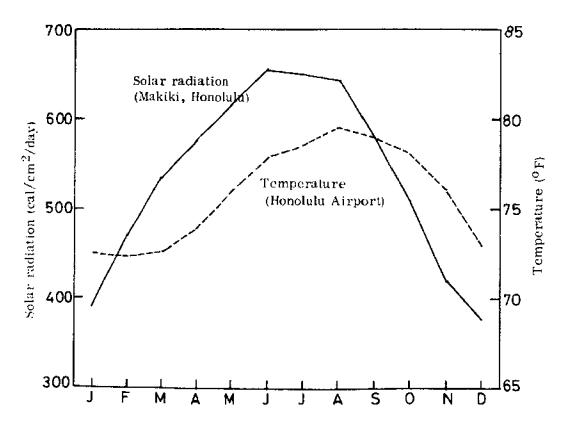


Figure 2 - Monthly averages of daily accumulation of solar radiation and outdoor temperature (3).

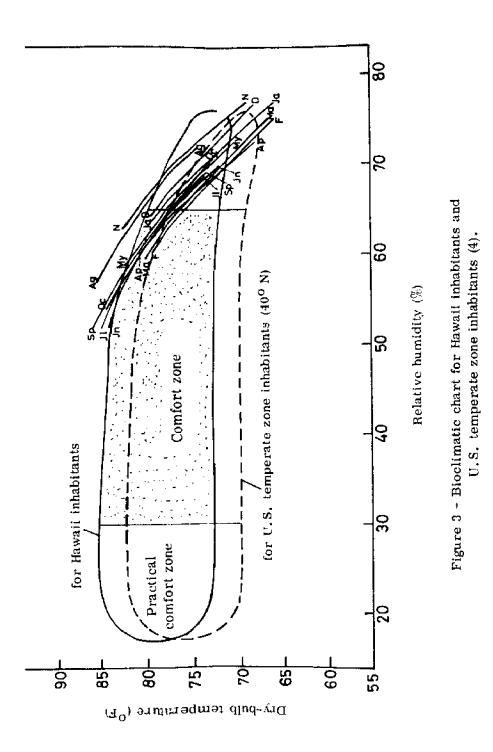
B. Human Response to Climatic Conditions

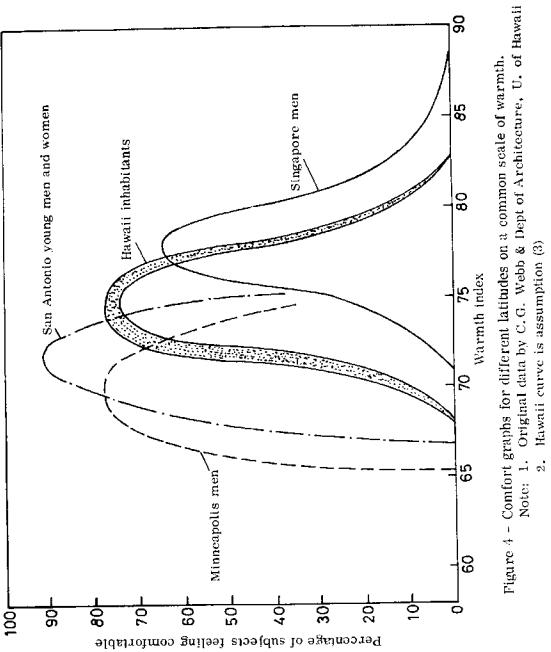
The major climatic elements that affect human comfort are air temperature, radiation, air movement and humidity. Minor elements are the chemical composition of air, its physical impurities, and its electrical properties. In general, ordinary temperature readings are not adequate to describe thermal environment. Air movement, humidity and radiation are all relevant as external thermal stimuli of the human body. They all affect the rate of heat loss of the body.

The most commonly used climatic scale is effective temperature (E. T.) introduced by Houghton and Yaglou in 1923 and again by Yaglou and Miller in 1925. Their index covers temperature, humidity and air movement without radiation. There have been numerous proposals on comfort conditions in many countries which have their own respective climatological and racial conditions. For a normally clothed American man at rest during the summer, Yaglou and Drinkers found that the comfort range is 66 to 75° F (E. T.) with 71° F(E. T.) as the optimum point.

Figure 3 shows the comfort zone for inhabitants in the U.S. temperate zone (40 deg N. lat.) and the estimated comfort zone for Hawaiian inhabitants by Olgray's method (4). He suggested that when the bioclimatic chart is applied to climatic regions other than 40 deg north latitude, the lower perimeter of the summer comfort line should be elevated about $3/4^{\circ}$ F for every 5 deg north latitude change toward the lower latitude. The upper perimeter may be raised proportionally, but not above 85° F. In the same figure, temperature and humidity are plotted to indicate monthly variations.

Sugiyama (3) proposed the comfort curve that is applicable to Hawaii inhabitants (Figure 4). It shows the percentage of subjects who feel comfortable under the specific warmth index.







C. Sea Conditions

Vertical temperature distribution of seawater has not been measured around the Floating City site. However, measurement taken by Wyrtki (5,6), Patzert (7), et al., may provide the general characteristics of vertical temperature distribution in Hawaiian seawater. These are plotted in Figure 5. It is seen that the characteristics of vertical temperature distribution are fairly similar at different places in the Hawaiian area. This may permit us to assume that a modified and generalized curve for vertical temperature distribution in Hawaiian seawater is possible. Therefore, vertical temperature distribution of seawater at the Floating City site is represented by the previously assumed curve and is given in Figure 5.

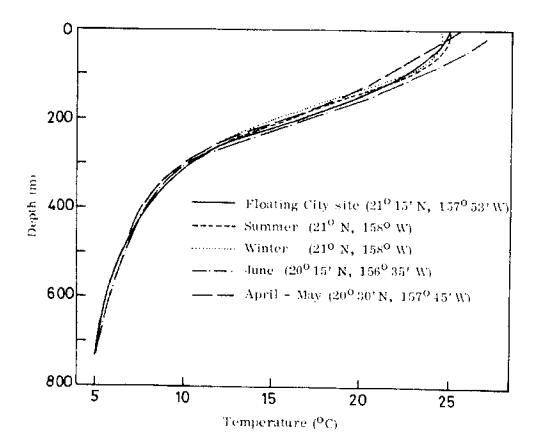


Figure 5 - Thermocline for Floating City site (5, 6, 7).

Surface temperature of Hawaiian seawater varies approximately from 25° C to 27° C throughout the year: 25° C to 26° C in winter, 26° C to 27° C in summer. In 1965, Wyrtki reported that the yearly temperature variation of the surface water is about 1.5° C.

Surface salinity of Hawaiian seawater ranges approximately from 34.5 °/oo to 35.0 °/oo (Figure 6). Salinity changes very slightly with depth; minimum salinity of 34.2 °/oo is obtained at a depth of about 500 to 600 meters in Hawaiian seawater.

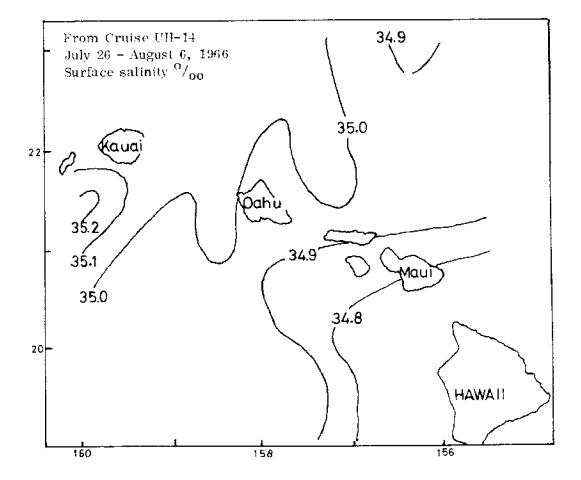


Figure 6 - Surface salinity of Hawaiian seawater (summer) (5).

According to the data taken by During in 1969 (8) at a depth of 25 meters in Hawaiian seawater, current velocity varies from 5 cm/sec to 50 cm/sec (Figure 7). Twenty cm/sec of current velocity is assumed to be an average for most of the time at a depth of 25 meters. However, further measurements relating temperature, depth and current velocity at the Floating City site are needed.

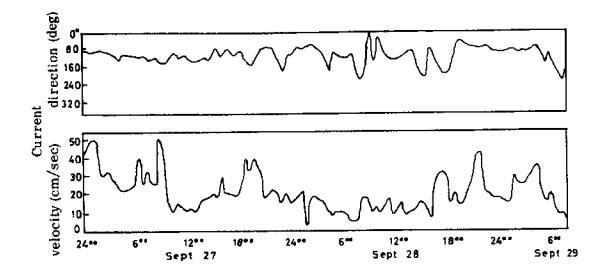


Figure 7 - Typical current velocity for Hawaiian seawater at a depth of 25 m (1969) (8).

II. AIR CONDITIONING SYSTEMS

The bioclimatic chart for Hawaii residents shown in the preceding section (Figure 3) suggests that air conditioning should rarely be needed for comfort reasons. However, the climatic data in the figure represent ambient conditions. In so compactly organized a structure as the Floating City, these ambient conditions could not be maintained throughout its interior without air conditioning unless the city could be designed so as to allow the passage of outside air through each compartment essentially unimpeded and unchanged, which is manifestly impossible. These data, therefore, establish a basis for the amount and kind of air conditioning the interior spaces will need to maintain them within comfort limits.

The American Society of Heating and Ventilating Engineers in 1929 defined comfort air conditioning as "the process of treating air so as to control simultaneously its temperature, humidity, cleanliness and distribution". The same definition applies today, with certain refinements. Comfort air conditioning, or climate control, means the maintenance of those atmospheric factors affecting human comfort. Specifically, it is the maintenance of the following variables:

- o Desired temperature
- o Acceptable humidity
- o Minimum number of atmospheric particles, including pollens and bacteria
- o Uniform air pattern and proper air motion.

A. Preliminary Planning

Preliminary design of an air-conditioning system requires an awareness of the esthetic, structural, and economic factors in the overall design from its very early stages. The machine room and air ducts require considerable floor area and space, which must be provided for during preliminary design.

In most respects, the air-conditioning requirements for a superstructure element on the Floating City will not differ from those of a high-rise office building in a similar climate. Therefore the following procedures used in air-conditioning system design for an office building are representative. 1. Selection of the air-conditioning system

Considerations of the equipment cost, operation cost, required space for the air-handling unit, structures, and zones within the building all contribute to the determination of a reasonable air-conditioning system. However, the final decision may rest with the designer, based on his experience and preference.

2. Placement of the machine room and air ducts in each zone

Once the air-conditioning system has been selected, a rough estimation of the required supply air is needed to determine the placement of machine rooms and ducts of appropriate sizes.

3. Determination of capacities required for heat source equipment

The capacities of the boiler and refrigerator can be determined by heat load estimations, so that the physical dimensions of the machine room may be designed accordingly.

The general procedures above may be further subdivided in order to determine more detailed procedures:

- 1. Detailed heat load estimations for each room in a building for the determination of peak load.
- 2. Selection of boilers and refrigerators.
- 3. Selection of air-handling devices such as cooling and heating coils.
- 4. Placement of the devices into the machine room for the determination of suitable machine room dimensions.
- 5. Selection of fans in accordance with the pressure drop in the ducts.
- 6. Sizing of the pipes in conjunction with the capacity and location of the boiler and refrigerator.
- 7. Determination of the capacity of the cooling means in accordance with the thermal performance of the boiler and refrigerator.

- 8. Placing of the apparatus, ducts and pipelines on the drawings.
- 9. Necessary corrections and/or revisions.

B. Various Systems

Table 4 shows typical characteristics of three types of air-conditioning systems that are applicable for office buildings. These are: 1) all-air-duct systems, 2) air-water systems, and 3) all-water systems. The first two are central station apparatus systems, while the all-water systems are primarily individual room or zone unit systems. Depending on the thermal requirements and function of the building, one may select the most efficient and economical system. Energy costs in Table 4 involve the sum of electric power and fuel for the refrigerator and boiler. The recommended floor area for these systems is 200,000 square feet or more.

Classification	System	Energy cost	Equipment cost	Power cost	Individual control	Fresh air cooling	Space requirements
All-Air-Duct Systems	Single duct Multi-zone unit High velocity dual duct	Low High High	Medium Medium Medium	High High Maximum	No Possible Possible	Possible Possible Possible	Iarge Iarge
	Single duct reheat Floor unit Induction unit	Medium Low Medium	High Medium Medium	Higb Righ Medium	Passible No Possible	Possible Possible No	Large Maximum Small
Air-Water Systems	(2-pipe) Induction unit (3-pipe)	Low	High	Medium	Possible	No	Small
	Primary air fan-coli unit	Low	Maximum	Low	Possible	No	Small
All-Water Systems	Fan-coll unit Package	Low Low	Low Low	Low Low	Possible Possible	No No	Minimum Small

Table 4 -	Classification	of	various	air	conditioning	systems
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1. <u>All-Air-Duct Systems</u>

In this type of system, the air treatment and refrigeration plants are located some distance away from the conditioned space. Only the cooled or heated air is brought into the conditioned space through ducts. A central station cleans, humidifies, dehumidifies, cools and heats the air. Figure 8 shows a typical all-air-duct system. The space designated as "room" represents the entire space in a building, and the supply and return ducts represent the whole network of ducts.

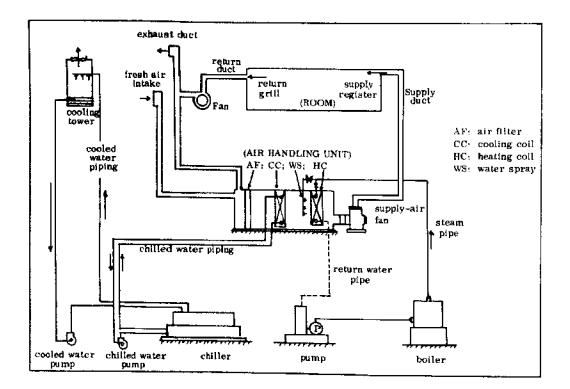


Figure 8 - All-air-duct system.

Single Duct System. This central station system (Figure 9) supplies a single stream of either hot or cold air into the conditioned spaces. Components of this system are mainly the air-handling unit, heat conveyance apparatus, heat sources and automatic control devices.

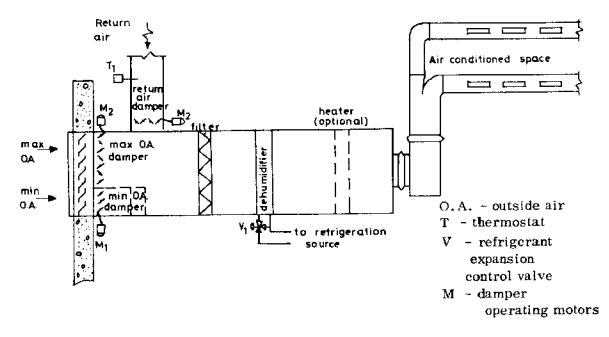


Figure 9 - Single duct system.

Merits of this system are as follows:

- Operation and maintenance can be done very easily, as the air-handling equipment is placed in a machine room. Dust can be eliminated completely from the supply air.
- o Supply air quantity is large enough to provide sufficient ventilation in the room.
- o Noise and vibration can be controlled easily.
- o If the building is divided into a few zones, equipment cost becomes low in comparison with other all-air-duct systems.

Demerits are given as follows:

- o Large duct space is required if there are many zones.
- o Equipment cost is considerably higher than the all-water system.

<u>Multi-Zone Unit System</u>. Heating and cooling coils are placed in an air-handling unit so that the hot and cold air are built up separately by these coils. Mixing dampers are installed in each zone to adjust the quantity of hot and cold air. It operates in response to the thermal requirements of a room. Figure 10 illustrates a typical application of this system.

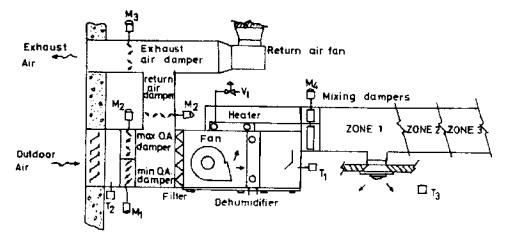


Figure 10 - Multi-zone unit system.

Merits of this system are given as follows:

- o It is useful in buildings that are divided into many different spaces and zones. This system offers excellent control of all spaces in accordance with their thermal requirements.
- Space can be utilized for diverse purposes, as both the heating and cooling are available separately.
- When the temperature difference between outside air and room air is large, outdoor air can be used for cooling or heating. This eliminates the operation cost of a boiler or refrigerator.

However, the multi-zone unit system requires large duct spaces if the building is divided into many different zones. In addition, boiler and refrigerator capacity must be large in order to deal with the mixing heat loss.

<u>High Velocity Dual Duct System</u>. This system supplies hot and cold air to each room separately through ducts. Air velocity is approximately 3,000 feet per minute or more in the ducts. Hot and cold air may be mixed in the air blenders which are installed and controlled by thermostats in each room (Figure 11). This system has characteristics similar to those of the multi-zone unit system, for both the hot and cold air are available separately. A small duct size is required for this system in comparison with other all-air-duct systems. This feature is a great advantage in tall buildings as it requires a fairly small space for ducting. Round ducts are commonly used in this system because of small frictional resistance and economy. Besides the excellent characteristics mentioned above, this system has other merits as follows:

- Thermal response of the room is very quick as the air is a heat-transfer medium. Hence, control of room air is fairly easy.
- No apparatus is exposed in the room.
- Maintenance of the unit's air filters is unnecessary.

However, the heat loss due to mixing of hot and cold air is very large, especially in winter.

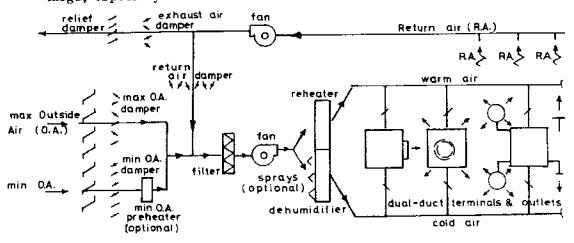


Figure 11 - Systematic diagram of high velocity dual duct system.

2. Air-Water Systems

This type of system has primary and secondary air treatment units. The primary air treatment plant is located some distance away from the conditioned space, as in the all-air-duct system. The function of the primary air treatment plant is identical to that of the all-air-duct system. The secondary air-handling unit is located in the room, ceiling, floor or corridor. Water is used to cool the media and to heat the coils in the air-handling unit. Local adjustment of room air is possible by using the secondary air-handling unit in accordance with the thermal requirements of the room and the condition of primary supply air into the room.

<u>Single Duct Reheat System.</u> This system is primarily the same as the single duct system except that the reheaters are installed in air diffusers or in branch ducts (Figure 12). Control valves for the steam or hot water are connected to the reheaters, and thermostats installed in the room regulate the control valves. Besides the merits described for the single-duct system, this system has another advantage in that it provides convenient zoning within a building.

However, the operation cost of the refrigerator increases in comparison to that for the single duct system due to the reheat load.

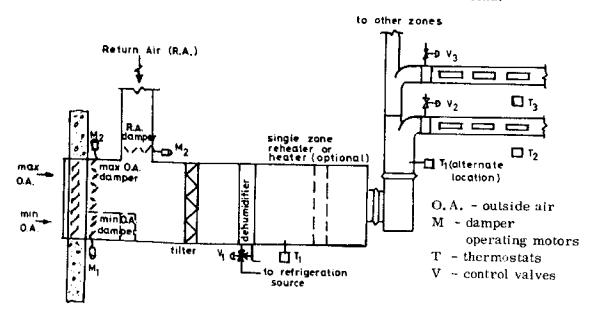


Figure 12 - Single duct reheat system.

<u>Floor Unit System</u>. The air-handling apparatus is placed on each floor in this system as shown in Figure 13. This system has merits such as:

- o Air conditioning can be done separately on each floor.
- o Horizontal duct size can be reduced.

However, the equipment cost is comparatively high and requires large spaces for air-handling equipment.

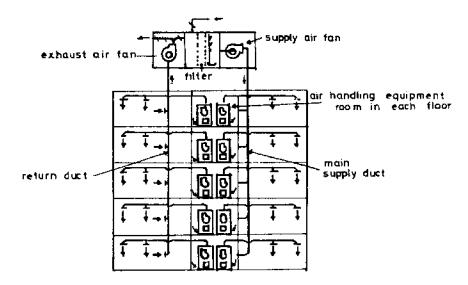


Figure 13 - Floor unit system.

Induction Unit System (2 Pipe). The induction unit system is a very interesting, compact and efficient, high-velocity air-conditioning method. Instead of carrying all of the air back to a central air-handling unit as in the dual duct system, room air is recirculated through a cabinet below a window. A small amount of fully conditioned outdoor air may be brought in through a single high-velocity duct. It flows through a jet after attenuation to induce room air circulation so that the room air and supply are mixed properly (Figure 14). Therefore, this system requires no air supply fans and no outdoor ventilation grills for fresh air. Chilled water and conditioned fresh air are supplied to the unit, and a two-way valve that is controlled by the room thermostat adjust the flow rate of

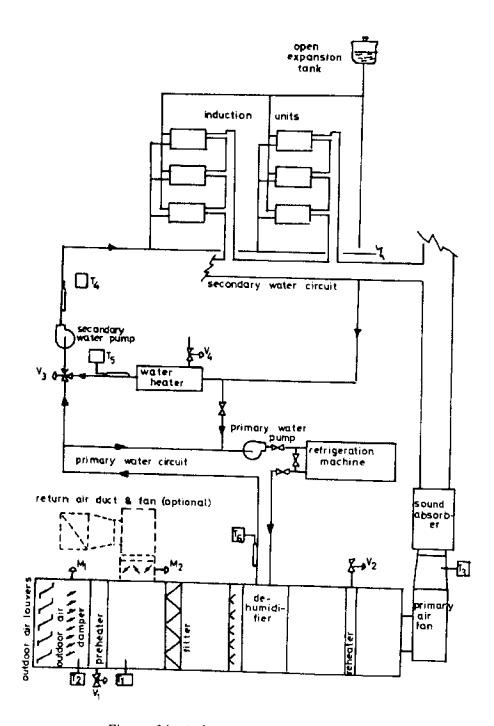


Figure 14 - Induction unit system (2 pipe).

chilled water. In general, heat loads from solar heat, people and lights are removed by chilled water, and the heat loads due to conduction, convection and radiation through the walls and roof are removed by conditioned air. As in the previous discussion, a smaller space is required in comparison with the dual duct system. However, heating and cooling energy offset each other in the same air-handling unit. Hence, operation cost increases. In addition, zoning of chilled water and conditioned fresh supply air is necessary.

Induction Unit System (3 Pipe). The 3-pipe induction unit system is more flexible than the 2-pipe system in that it supplies hot and chilled water simultaneously, while the 2-pipe system carries only hot or chilled water into an induction unit. According to the heating or cooling needs of a building, the return pipe is used in common for both hot and cold water return.

The flow rate of hot and chilled water is controlled by a sequence control valve (or three-way valve) operated by a room thermostat. This system has other merits in addition to those of the 2-pipe system: no zoning is required for either supply water or air, and mixing loss can be minimized when the return water pipes are divided into many zones. Hence, the operation cost can be reduced in comparison with the 2-pipe system.

On the other hand, as it requires a more complicated system, the equipment cost increases in comparison to the 2-pipe system.

<u>Primary Air Fan-Coil Unit System</u>. This system is similar to the induction unit system (Figure 15). The main difference is that conditioned air and chilled or hot water are supplied to the fan-coil unit instead of the induction unit. In turn, instead of inducing the room air, the supply air fan mixes the room and conditioned air properly. The most suitable applications for this system are multi-room buildings such as hotels, offices, hospitals and apartment houses. If we emphasize the importance of air-conditioning performance, this system may be the most suitable, but the initial cost of a fan-coil system is very high.

The fan-coil unit can be located along the perimeter of a building, and the primary air (conditioned air) is supplied to the fan-coil unit directly or is supplied to the room through ducts in the corridor (Figure 15). Application of this system is popular in Hawaii.

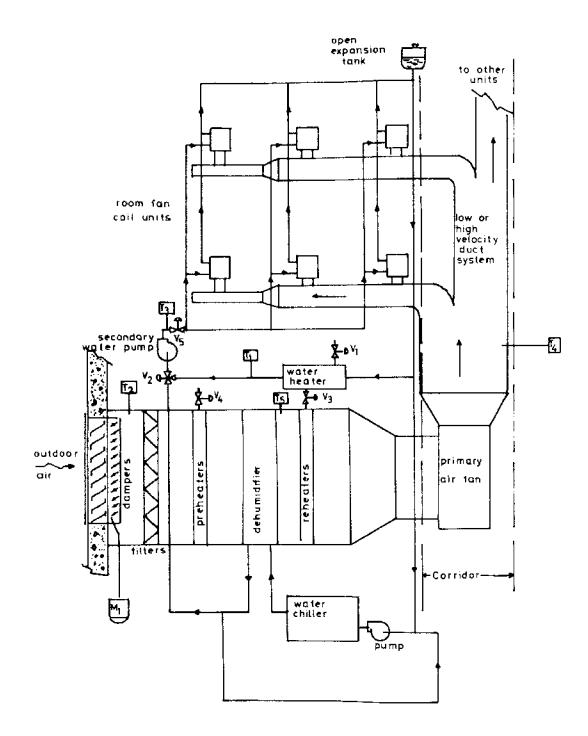


Figure 15 - Primary air fan-coil unit system.

Merits of this system are as follows:

- The system is ideally adapted for control of individual room air temperatures, as each fan-coil unit has integral heating and cooling coils.
- Motion and distribution of air in the room can be easily controlled by this system.
- Wherever the effect of cold radiation and convection from windows causes discomfort, this system is advantageous. Fan-coils along the perimeter of the windows supply the upward hot air and remove the effect of cold radiation and convection.

However, this system requires a relatively high equipment cost if the total floor area of a building is less than 200,000 square feet (i.e., a small or medium size office building).

3. All-Water Systems

The all-water systems are mainly fan-coil and packaged types of room terminals to which may be connected one or two water circuits. The cooling medium such as chilled water or brine may be supplied from a central station and circulated through the coils in the fan-coil or package unit terminal which is located in the room. Ventilation is obtained through an opening in the wall or by infiltration.

a. Fan-Coil Unit System.

This system is particularly applicable to multi-room buildings where large-sized duct work is impossible. It is not recommended for applications having high latent loads. Hotels, motels, hospitals, apartment houses and office buildings can use the system to advantage. The unit may be located under the window, over the closets, or in dropped ceilings.

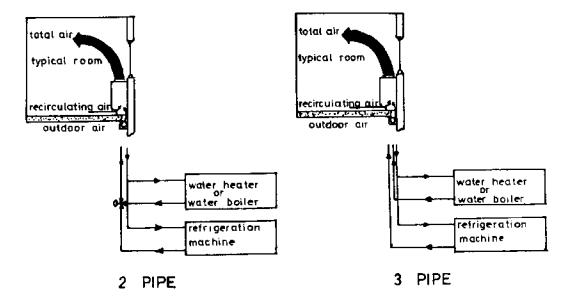
There are two types of fan-coil unit systems: single piping (2 pipe), and multi-piping (3 pipe, 4 pipe). In the former, a single supply medium such as cold or hot water is available at each fan-coil unit, and a single return piping system is utilized. In the latter, hot and cold media are available at each fan-coil unit, and a single (3 pipe) or double (4 pipe) return piping system is utilized. <u>Single Piping (2 Pipe) System</u>. This system (Figure 16) consists of central heating-cooling equipment and a fan-coil unit. The fan-coil unit system is designed to control individual space without connecting to the central air-handling station and duct. Either a mixture of fresh and return air or return air alone is supplied into the conditioned room. Although fresh air is generally supplied through a low pressure duct, it may be taken directly from the wall openings. This latter method costs less initially and gives greater flexibility in utilizing the system. However, wall openings for outdoor air are not generally recommended in multistory buildings. Stack and wind effects may adversely affect the performance of the units. In some cases, infiltration air through windows and doors is sufficient for ventilation. The room air temperature can be adjusted by means of control switches for fan speed and water flow. Merits of the system are:

- It is suitable for individual control of room air temperature. As it has integral heating-cooling coils, adjustment of room air is quick and easy.
- o Operation and equipment costs are comparatively low.
- Minimal duct work is required.

However, the quantity of supply air is not enough to humidify the room.

<u>Multi-Piping (3 Pipe, 4 Pipe) System</u>. This system provides hot and cold water through each fan-coil unit in the room (Figure 16). Each unit can be used for many different zones and functions by controlling the hot and cold water with control valves. Merits of the multi-piping system in addition to those for the single piping system are as follows:

- Quick thermal response is obtained through hot and cold water in the unit.
- Zoned piping and allied controls are eliminated due to the flexibility of using both hot and cold water.
- Complaints of occupants during the intermediate seasons are eliminated because of the availability of both heating and cooling.



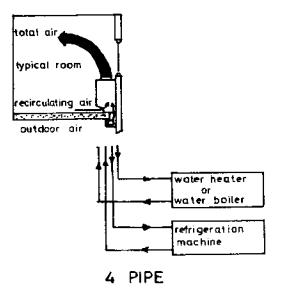


Figure 16 - Fan-coil unit system.

b. Packaged Air-Conditioners

Packaged air-conditioners, as in Figure 17, which are also called self-contained equipment, provide a complete heating and cooling system in the package unit. This unit is composed of compressor, condenser, fans, evaporator, heater, filter and controller. Commercial self-contained air conditioners are available in sizes up to 66 tons. Units of 2 to 7.5 tons are designed for the room usage and the larger units are located away from the rooms. Major refinements of this system are its low cost, compactness and easy operation. The packaged air conditioners are either air or water-cooled systems. The former has evaporative condensers while the latter has cooling towers. Merits of this system are as follows:

- The initial costs of packaged units are low due to less volume, and they can be installed easily with minimum disturbance to the occupants.
- The units are compact and easy to maintain because of their accessibility.

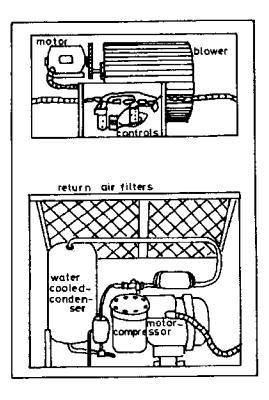
However, room air is not properly distributed and humidity control is insufficient. Additional expense is required to improve the performance of the system. Also, as maintenance is required fairly frequently, maintenance cost is comparatively high.

c. <u>Room Air Conditioners</u>

Packaged air conditioners with capacities of 0.5 to 2 tons are usually defined as room air conditioners. These are mainly air-cooled conditioners, but larger sizes may require water-cooled systems. Aircooled units may be located on the wall, roof, window or any other place facing the outside air to reject the heat and to dispose of the condensed water from the cooling coil.

C. Applications

Typical applications for the various systems described above are shown in Table 5. Detailed explanations are found in the Handbook of Air Conditioning System Design (9), which was the source of most of the figures and tables in this section.



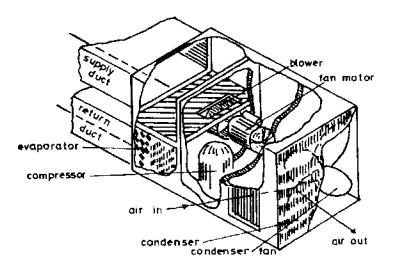


Figure 17 - Packaged air conditioners.

				Individ	ual Room or	Zone Ur	nit Systems		с	entral Stat	ion Appar	atus Syste	ems	
APPLICATIONS		DX Self-Contained All-Water			All-Air					Air-Woter				
			Room	Zone	Room Fan-Cail			Sin	gle Air Str	am		Prim. Ai	r Systems	
				V3 to 2 2 tons	2 tons Recir.	With			Re	ieat	Multi- Zone	Secndry. Water	Room Fan-Coi	
			73 10 2 tons	2 tons and over	Air	Outdoor Air	Variable Volume	Bypass	At Terminal	Zone in Duct	Single Duct	H-V H-P Induction	with	
			Page	(9–8)	(9-8)	(98)	(9–8)	(9–9)	(9–9)	(9–10)	(9–10)	(9–10)	(9–11)	(9–8)
	Residential	Medium Large	(9–13)	×	x	x						×		
	Restaurants	Medium Large	(9–13)		x x				×	x	x x	x		
65	Variety & Sj Bowling All		(9–13) (9–14)		x x				x					
cupanci	Radio and TV Studios	Sma'l Large	(9-14)		x x			l	x x		× ×	x x		
pose Uc	Country Clu Funeral Hon		(9–14) (9–14)		x x				×		×	x x		
Single-Purpose Occupancies	Beauty Sala Barber Shop		(9– 14) (9–15)	×	× ×									
2	Churches Theaters	,	(9–15) (9–15)		4 x ²				××			x		
	Auditoriums Dance and F Pavilions		(9-15) 9 (9-15)		x			x	×					
	Factories (ca	mfort)	(9-15)		×				×		×			
	Office Buildi Hotels, Dorn	•	(9–16) (9–18)			×	x	×				×	x x	×
	Motels Aportment E	Buildings	(9–18) (9–18)			×	×						. x	x
tainundasso	Hospitals Schools and	Colleges	(9–18) (9–19)				x x	x	×	×	x x		×	· ·-
	Museums		(9–20)								×	x		
send in L-IIIniv	Libraries	Standard Rare Books	(9-20)		x x				x		x x	x		
	Department Shopping Ce		(9–19) (9–19)		×				× ×			x		
	Laboratories	Small Lge Bldg	(9-20)		x			x x		×	×	×	x	
	Marine		(9-21)							×			x	

Table 5 - Systems and applications

¢.,

3. Numbers in parentheses are page numbers of the text describing the particular system or application.

III. HEAT GAINS

The thermal factors affecting the superstructure and buoyancy tanks of the Floating City are numerous and, as these are intricately interrelated, the evaluation and analysis of these factors should be performed carefully.

Heat gain is defined as the rate at which heat enters into or is generated within a space. It can be influenced by weather, location of a building, time, construction materials, usage of a building, equipment, lighting and occupancy.

In this section, equations are developed for determining heat gains through the windows, walls and roof of the superstructure, as well as heat gains due to ventilation and infiltration of outside air. The heat generated by people, lights, and equipment within the building is briefly discussed. Finally, consideration is given to heat gains through the walls of the buoyancy tanks.

A. Heat Gain through Windows of Superstructure

At any instant, the total instantaneous heat gain through glass is the sum of solar radiation transmitted through glass and the heat flow due to convection from the inner glass surface and conduction caused by the temperature difference between outside and inside air. For glazing materials, heat gain Q_g is expressed in the 1972 ASHRAE Handbook (10) as

$$Q_{g} = (SC) \left[\left(I_{nd} \sum_{j=0}^{5} \tau_{j} \cos^{j} \gamma \right) + 2 I_{d} \sum_{j=0}^{5} \tau_{j} (j+2)^{-1} \right) \\ + \left(I_{nd} \sum_{j=0}^{5} \alpha_{j} \cos^{j} \gamma \right) + 2 I_{d} \sum_{j=0}^{5} \alpha_{j} (j+2)^{-1} (h_{o}) (h_{o} + h_{i})^{-1} \right] \\ + U (\theta_{o} - \theta_{i})$$
(3-1)

$$\approx (SC) (SHGF) + U (\theta_0 - \theta_i)$$
(3-2)

SHGF is the abbreviation for solar heat gain factor, which is the rate of heat flow due to transmitted solar radiation and convection from the inner surface of glass; SC is the shading coefficient, defined as the ratio of solar heat gain through a fenestration under a specific set of conditions to the solar gain through a plain double-strength glass under the same set of conditions. The effect of reflected radiation is neglected in Equation 3-1, which must be modified in the case of high intensity of reflected radiation. Shading coefficients applicable to some of the widely used types of insulating glass and internal shading coefficients for curtains and venetian blinds are given in air-conditioning handbooks. Calculation of the solar heat gain factor is made following the ASHRAE's recommended procedures.

B. Heat Gain through Walls or Roof of Superstructure

Figure 18 illustrates the factors which affect the heat balance at the outside surface of a wall at time $n\Delta t$. The X_j, Y_j and Z_j are called response factors (8,11). The heat-balance equation at the outside surface is

$$\sum_{j=0}^{J} Y_{j} \theta_{i,n-j} + \alpha_{s} I_{t,n} - h_{o} (\theta_{s,n} - \theta_{o,n}) - \sum_{j=0}^{J} X_{j} \theta_{s,n-j} = 0$$
(3-3)

where Q_8 is the absorptivity of the wall surface. The value of J is to be selected arbitrarily, depending upon the degree of accuracy of calculations. Rearrangement of Equation 3-3 gives

$$\theta_{s,n} = (X_{o} + h_{o})^{-1} \left[Q_{s}I_{t,n} - \sum_{j=1}^{J} X_{j}\theta_{s,n-j} + \sum_{j=0}^{J} Y_{j}\theta_{i,n-j} + h_{o}\theta_{o,n} \right]$$

$$(3-4)$$

The inside air temperature $\theta_{i,n-j}$ is usually considered to be constant. By taking appropriate prior values of outside surface temperature $\theta_{s,n-j}$ to start the calculation, the value of $\theta_{s,n}$ can be determined by the above equation. By increasing the number n, accurate values of outside surface temperature can be found subsequently. For a constant inside air temperature $\theta_{i,n-j}$, the effective excitation of outside surface temperature is $(\theta_{s,n-j} - \theta_{i,n-j})$. Then the heat flux for the wall area A_w is

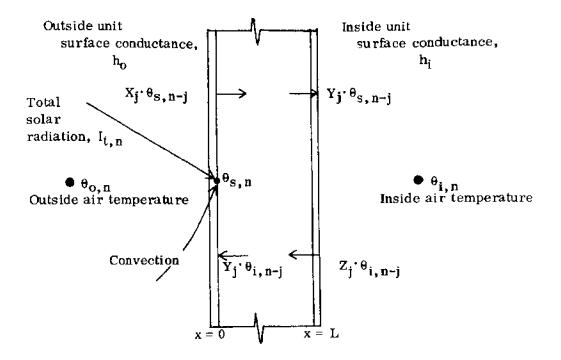


Figure 18 - Heat balance at outside surface.

$$Q_{w} = A_{w} - \sum_{j=0}^{J} Y_{j}(\theta_{s,n-j} - \theta_{i,n-j})$$
(3-5)

Physical interpretations of response factors X_j , Y_j and Z_j as depicted in Figure 19 are as follows:

- X_j : Heat rate at time $t = j\Delta t$ at the surface x = o in Btu/hr-ft^{2-o}F when the unit temperature excitation is applied to the same surface.
- Y_j: Heat rate through the wall at time $t = j\Delta t$ at x = 0 or x = L in Btu/hr-ft²-^OF when the unit temperature excitation is given to the surface at the opposite side of the wall. Y_j at x = 0 is the same as that at x = L because of the reciprocity theorem.
- Z_j : Heat rate at time $t = j\Delta t$ at the surface x = L in Btu/hr-ft^{2-o}F when the unit temperature excitation is given to the surface at x = L.

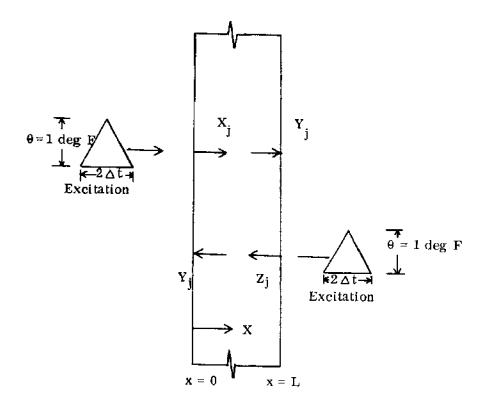


Figure 19 - Physical representation of response factors.

C. Heat Gain from Lights, Equipment and People

Lights, equipment and people are the main heat generating sources within a room. The precise prediction of the number of people and lights is not possible. In general, the number of people in a room and power consumption of lights and equipment are estimated according to the functions of the building. The heat generated per average person for various types of activities can be found in handbooks (9, 10).

D. Heat Gain from Ventilation and Infiltration

Comfort criteria require a certain amount of outside air to be supplied continuously through a ventilation duct to the conditioned space. The heat gain in Btu per hour due to ventilation at G cfm of outside air (10) is given by Q_{vent} = sensible gain + latent gain

$$= G \times 60 \times 0.075 \times 0.245 (\theta_0 - \theta_i)$$

+ G x 60 x 0.075 x 1076 (W_0 - W_i)

Infiltration of outside air into a building is affected largely by wind velocity, temperature difference between outside and inside air, and construction of the building. If N is the recommended rate of air change per hour for the room of V cu ft, the heat gain in Bu per br due to infiltration (8, 10) is

$$Q_{infilt} = 0.0183 \times N \times V(\theta_0 - \theta_i) + 79.5 \times N \times V(W_0 - W_i)$$
(3-7)

E. Heat Gain through Walls of Buoyancy Tank

Application of an overall heat transmission coefficient is a convenient way to calculate the heat gain through the walls of the buoyancy tank. By taking into consideration Figure 5, temperature of seawater is assumed to be constant at a specific depth. Therefore, the application of response factors is not practical, as the condition of heat flow is steady. In general, the heat flow through the wall due to conduction in cylindrical coordinates is expressed by

$$\mathbf{Q} = \mathbf{U}(\mathbf{\theta}_{i} - \mathbf{\theta}_{0}) \, 2\pi \mathbf{l} \qquad (3-8)$$

$$U = 1/\left[(h_i r_i)^{-1} + \sum_{n=1}^{N} \ln (\rho/k)_n + (h_0 r_0)^{-1} \right]$$
(3-9)

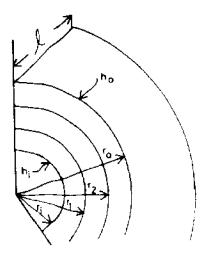


Figure 20 - Wall of cylindrical coordinates

$$\rho_1 = r_1/r_1$$
; $\rho_2 = r_2/r_1$; $\rho_n = r_0/r_{n-1}$

(3-6)

IV. COOLING LOADS

A. Heat Gain

The heat gains described in the preceding section are considered to be instantaneous heat gains in the new ASHRAE procedures for cooling load calculation. As we have seen, instantaneous heat gains may originate from a number of sources: solar radiation admitted through windows, heat transmitted through walls and roof, infiltration, ventilation, lighting, people, and machinery inside the space. The heat gains from different sources undergo different delays before they become cooling loads.

In the 1972 ASHRAE Handbook of Fundamentals (10), the instantaneous heat gain from each source is separated into a convective portion and a radiant portion. The radiant portion is first absorbed by the walls and by the contents in the space, and then transferred to the inside air over an extended period of time through the mechanism of convection. The total instantaneous cooling load is the sume of the convective portion and the average of the radiant portion over a period of time. The recommended period of time is 2 to 3 hours for lightweight construction and 6 to 7 hours for heavyweight, without a clear definition to differentiate lightweight from heavyweight.

B. Cooling Load Evaluation

Exact evaluation of the space cooling load involves the solution of simultaneous equations of heat balance for many parts of the building. Stephenson and Mitalas (12) demonstrated the exact method by formulating eight simultaneous equations for a room of simple configuration. Mitalas and Arsenault (13) later proposed a weighting factor method based on the assumption that the instantaneous heat gain and the corresponding component of the cooling load can be expressed in the form of a characteristic transfer function. Their weighting factors are the sets of transfer functions which relate the heat gains to cooling loads, being determined by the z-transfer method.

C. Response Factor Method

It would be advantageous to express weighting factors in terms of response factors. This idea was first introduced by Kimura and Stephenson (14). For 1 Btu/hr-ft² of radiant heat impinging upon a surface

whose absorptivity is \mathbf{a} , the heat flow through the surface is \mathbf{a} Btu/hr-ft². Assume the heat transfer coefficient of the convective film to be h_i Btu/hr-ft²-°F. If the temperature at the outside surface of the convective film is \mathbf{a} /h_i degrees higher than the temperature at the wall's surface, as depicted in Figure 21, the heat flow is also \mathbf{a} Btu/hr-ft².

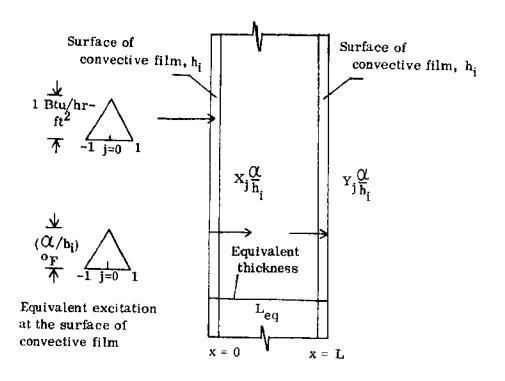


Figure 21 - Equivalent excitation for wall of equivalent thickness.

D. Equivalent Thickness Approximation

Hypothetically one may assign an equivalent excitation Q/h_i degrees at the outside surface of the film to evaluate the transient flow of heat through the wall due to the unit radiant heat.

If the response factors X_j , Y_j and Z_j are evaluated for a solid wall of equivalent thickness L_{eq} together with the convective films as shown in Figure 21, the outside surfaces of the composite wall should be the exterior surfaces of the rilms. The magnitude of response factor Y_j is relatively

small in comparison with X_j as shown in Figures 18 and 19, in which one also finds that X_j at j = 0 has a sign opposite to the sign of other X_j 's and the sign of Y_j 's to signify that the heat is first driven into the wall momentarily by the excitation at j = 0 and then flows out from both sides of the wall.

Referring to the definitions of X, and Y, in Section III, the amount of heat which remains in the space after 1 Btu/hr-ft² of radiative heat from an internal source impinges upon the wall, can be evaluated by the following two equations:

$$W_{j} = 1 - \frac{\alpha}{h_{i}} (X_{j} + Y_{j}) \stackrel{\sim}{=} 1 - \frac{\alpha}{h_{i}} X_{j}, \text{ at } j = 0$$

$$(4-1)$$

$$W_{j} = -\frac{Q}{h_{j}} X_{j}, \text{ at } j \ge 1$$
(4-2)

The W, is known as the weighting factor, which may appear in different versions by different ways of evaluation.

Takeda and Matsuo (15) studied the thermal characteristics of composite walls and found that the transient behavior of multi-layer walls can be approximated with an equivalent wall having a single layer. The thickness L_s of the equivalent wall for a composite wall of M layers is given by

$$L_{s} = \sum_{m=1}^{M} (C_{p} L/\rho)_{m} / (C_{p}/\rho)_{k}$$
(4-3)

where the subscript k is used to indicate the thermal properties of the equivalent wall.

To simplify the calculation of weighting factors, it is proposed here to use an equivalent thickness L_{eq} for all the walls in a room by extending Takeda and Matsuo's idea:

$$L_{eq} = \sum_{m=1}^{M} (A \cdot L_s)_n / \sum_{n=1}^{N} (A)_n$$
(4-4)

where A is the surface area of the wall with the respective thickness of L_s , and N is number of walls in a room. The degree of validity of Equation 4-4 has yet to be checked by other methods, and some empirical constants may have to be added to improve its applicability.

After the heat gains and weighting factors are found, the cooling load at time $n \Delta t$ can be calculated by the equation,

$$CL_{n} = \sum_{j=0}^{J} W_{j} HG_{n-j} + HC_{n}$$
(4-5)

where HG_{n-j} is the sum of radiative heat gains of a room at $j \Delta t$ hours prior to time $n \Delta t$, and HC_n is the sum of convective heat gains at time $n \Delta t$. The proportioning of radiative heat gains and convective heat gains from various heat sources has been recommended by ASHRAE (10).

The cooling loads for the superstructure and buoyancy tanks were calculated with the proposed concept of equivalent wall thickness. The results, as shown in Section V, appear reasonable in relation to the total heat gains.

V. CALCULATIONS OF COOLING LOAD FOR SUPERSTRUCTURE AND BUOYANCY TANK

Sample cooling load calculations have been made for the superstructure and for a buoyancy tank, to illustrate the application of the foregoing heat-flow model to the design of an environmental control system for the Floating City. The calculations were performed on an IBM 360/65 computer using a program written for this report in FORTRAN IV. Appendix B contains the program flow diagram and a brief description of the subroutines used in the calculations. The program listing and sample outputs are presented in Appendix C.

A. Superstructure

The top floor of the superstructure in the Floating City is used as the model for sample calculations. Figures 22, 23, and 24 show the floor plan, a typical room, and the elevation of the building.

For satisfactory control of indoor conditions in large buildings, zones of heating and air conditioning are usually established according to thermal requirements (16). The building shown in Figure 22 is divided into nine zones, labeled A through I. The cooling load of a typical room in each zone has been calculated and reported hereupon.

The structure is mainly made of lightweight concrete. Table 6 shows the composition of walls and roof, and the physical properties of the pertinent materials; in the same table are the equivalent thicknesses (L_{eq}) , which are determined by Equation 4-4.

The following input data are required for the calculation of cooling load:

- o Physical properties of materials from Table 6
- o Weather data from Table 7
- o Input data given in Table 8

Table 8 summarizes the indoor design conditions; the assumed temperature of the outside surface to start the calculations; areas of outside walls, windows and roof; absorptivities of outside surfaces; volumes of rooms and orientation of walls. Also shown in Table 8 are sample input values for the number of people and the power input from lights, both of which are functions of time of day, and these are further specified in Tables 9 and 10. The rate of heat gain per occupant is an input code selected from Table 11 according to type of building and degree of activity. Ventilation requirements, based on anticipated smoke levels, are selected from coded values in Table 12. Infiltration rate depends upon type of construction, and the input codes are selected from Table 13. Finally, the glazing material is selected from Table 14, which lists shading coefficients and U values for various types of glass. (In this case, input code 3 denotes 1/8-inch double strength glass).

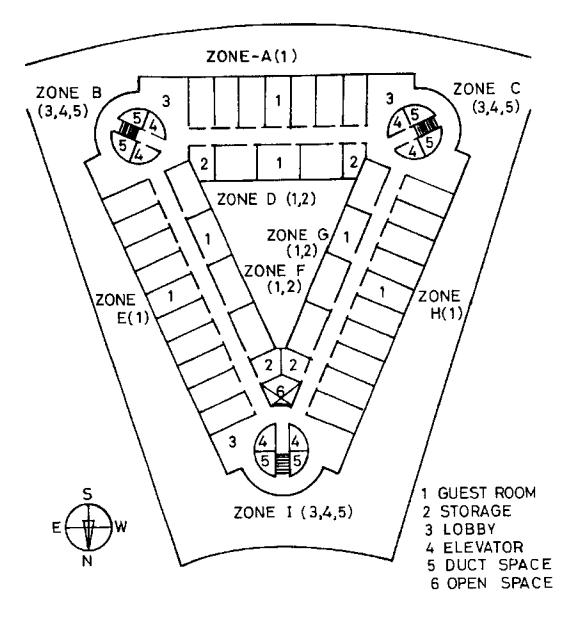


Figure 22 - Top floor plan of superstructure.

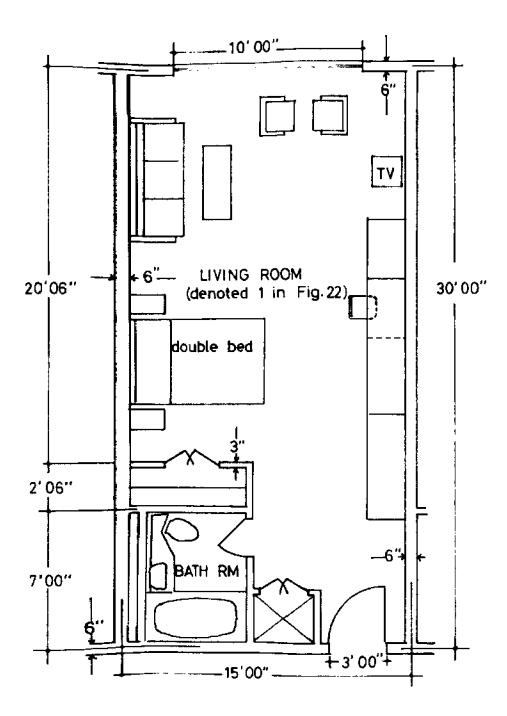


Figure 23 - Typical room of superstructure

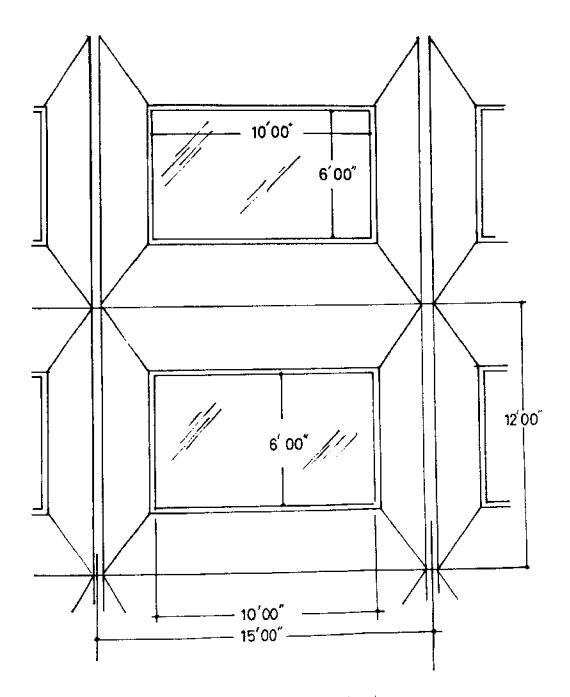


Figure 24 - Elevation of superstructure

	DESCRIPTION	Ľ	¥	م	Cp	Я	a	Symbola:
	1" Stucco	0.0833	0.40	116.0	0.2		0.61	T = Equivalent-thickness wall,
	6" Lightweight concrete	0.50	0.10	40.0	0.2	ł	1	a = Zone A, D, E, F, G, and H,
	_	0.0833	0.025	2.0	0.2	1	ł	b = Zone B, C, and I,
116		0.0625	0.420	100.0	0.2	ļ	}	Let - Equivalent thickness,
M		0.0	0.0	0.0	0.0	0.50	{	Eq. (4-4),
	FNOL = 5.0, $IREF = 1$							$\mathbf{L} = \mathbf{T}$ hickness of layer (ft),
_	1" Waterproof cement	0.0833	0.40	116.0	0.70	ł	0.73	$O = Density (lb/ft^3)$,
	mortar							k = Thermal conductivity
-	3/8" Asphalt	0.0417	0.83	55.0	0.40	ł	ł	(Btu/hr-ft- ^o F),
J	6" Lightweight concrete	0.50	0.10	40.0	0.20	1	l 1	C _n = Specific heat
003	12" Celling air space	0.0	0.0	0.0	0.0	1.0	ļ	$\begin{bmatrix} F & (Btu/lb^{0}F), \\ \end{bmatrix}$
ł	3/4" Acoustic tile	0.0625	0.035	30.0	0, 20	;	1	R = Resistance
·	Inside air film	0.0	0.0	0.0	0.0	0.50	ļ	$\int (hr-ft^2 - F/Btu)$
	FNOL = 6.0 , IREF = 2							Q = Absorptivity,
	Inside air film	0.0	0.0	0.0	0.0	0.50	1	FNOL - Number of layers,
	8.2" (L _{eq}) lightweight	0.87	0.1	40.0	0.20	ł	0.573	IREF - Kind of response
e.								factor.
Т	Inside air film	0.0	0.0	0.0	0.0	0.50	1	
	FNOL = 3.0							
	Inside air film	0.0	0.0	0.0	0.0	0.50	1	F
	13.2" (L _{ed}) lightweight	1.10	0.10	40.0	0.20	ł	0.546	
q								
ί.		0.0	0.0	0.0	0.0	0.50	ł	
	FNOL = 3.0							

Table 6 - Physical properties of wall and roof of superstructure

Time (hr)	Temperature (^O F)	Relative humidity (%)	Time (hr)	Temperature	Relative humidity (%)
0100	75.90	71.0	1300	88.80	51.5
0200	76.10	70.0	1400	88.60	52.0
0300	76,80	69.6	1500	87.90	54.0
0400	77.80	69.0	1600	86.90	56.8
0500	79.10	68.5	1700	85.60	59.5
0600	80.70	68.0	1800	84.00	61.5
0700	82.40	67.0	1900	82.40	63.3
0800	84.00	66.0	2000	80.70	65.0
0900	85.60	64.2	2100	79.10	66.5
1000	86.90	62.1	2200	77.80	68.0
1100	87.90	59.5	2300	76.80	69.0
1200	88.60	55.1	2400	76.10	70.0

Table 7 - Average hourly temperature and humidityon September 1 in downtown Honolulu (18)

Computer		· · · · · · · · · · · · · · · · · · ·
program	Description	
label	Description	Value
tabel		· · · · · · · · · · · · · · · · · · ·
TR, WR	Design air temperature (^{O}F) and specific	78.0, 0.0125
	humidity of the room, (lb/lb)	1010, 010120
IDOY	Time of year, (Sept. 1)	244
NDAY	Length of calculation (days)	2
TDB	Initial surface temperature of wall and roof (^{0}F)	80.0
FO, FI	Outside and inside unit thermal conductances,	6.0, 2.0
	$(Btu/br-ft^2-oF)$	0.0, 2.0
ww	Number of different delayed surfaces (wall	2.0
	and roof)	1 2.0
FNS	Number of spaces in the building (Zone A to I)	9.0
ARE	Outside wall and roof surface areas (ft^2)	0.0
	Spaces 1 of Zone A, D, E, F, G, and H	60 (6)
	Space 3 of Zone B (ENE, E, ESE, S)	445, 295, 295, 445
	Space 3 of Zone C (S, WSW, W, WNW)	
	Space 3 of Zone I (N, ENE, WNW)	445, 295, 295, 445
ААВ	Absorptivities of outside wall and roof surface	590,445,445
VOL	Spaces 1 of Zone A, D, E, F, G, and H	
	Space 1 of Zone D	5400 (5) 6000
-	Spaces 3 of Zone B, C, I	6000
IREF	Wall orientations as given in the note (first	21672 (3)
	8 numbers) and roof (last number)	
	$0 = \text{no wall}, 1 \neg \text{wall}, 2 = \text{roof}$	
	Zone A	000010000
	Zone B	000010002
	Zone C	00000002
-	Zone D	00000002
	Zone E	10000002
		010000002
	Zone F	000001002
	Zone G	000100002
	Zone H	00000012
ALFA	Zone 1	000000002
ALFA	Absorptivity for the wall of equivalent thickness	
	Zone A, D, E, F, G, H	0.5725 (6)
NORD	Zone B, C, I	0,5458 (3)
NOPP	Reference number of people	2
(NOP)	Number of people (Table 9)	
WAAT	Reference power input from lights (watt)	160
(WATT)	Power input from lights (Table 10)	
150	Rate of heat gain per occupant (Table 11)	3
151	Ventilation requirement (Table 12)	4
152	Infiltration rate (Table 13)	1
153	Type of glass (Table 14)	3
TTO	Dry-bulb temperature of outside air	
WWO	Specific humidity of outside air	

Table 8 - Input for the sample calculation

Note: Code for orientation of wall

<u>Wall o</u> rienta	tion N	ENE	E	ESE	s	WSW	W	WNW
Wall azimuth	n (deg) 180	112.5	90	67.5	0	67.5	90	112.5

	Zone	
Time of day	A, D, E, F, G, H	B , C , I
0100 to 0800	2	10
0900 to 1700	1	5
1800 to 2000	2	10
2100 to 2400	3	15_

Table 9 - Number of occupantsTable 10 - Power input from lights

	Zone	
Time of day	A, D, E, F, G, H	B, C, I
0100 to 0300	40 watt	400 watt
0400 to 0600	20	200
0700 to 1700	0	0
1800 to 2400	160	1600

Table	11	_	Rate	ഹ	heat	gain	Der	occupant	(9)
taote	11	-	nate	OI.	neat	Ean	Per	occupant	1-1

Input Code (I50)	Heat Btu/hr	Typical application	Degree of activity
1	350	Theater evening	Seated at rest
2	400	Offices, Hotels, Apartments	Seated, very light work
3	450	Offices, Hotels, Retail store	Moderately active office work
4	500	Bank, Drug store	Standing, working slowly
5	550	Restaurant	Sedentary work
6	750	Factory	Light bench work
7	850	Dance hall	Moderate dancing
8	1000	Factory	Moderate heavy work
9	1450	Bowling alley, Factory	Heavy work

Cfm/person Recommended	Application	Smoking
20	Average apartment	Some
7.5	Department store, Theater	None
10	Bank, Drug store	Occasional
30	Hotel rooms	Heavy
50	Meeting rooms	Very heavy
15	General offices	Some
12	Restaurant	Considerable
	20 7.5 10 30 50 15	RecommendedApplication20Average apartment7.5Department store, Theater10Bank, Drug store30Hotel rooms50Meeting rooms15General offices

Table 12 - Ventilation requirements (10)

Table 13 - Infiltration rate (17)

Input Code (I52)	Number of air changes	Types of Construction	Degree
1	0.5	Concrete or steel, with steel sash	Good
2	1.0	Concrete or steel, with steel sash	Medium
3	1.5	Masonry, with steel sash	Medium
4	2.0	Masonry, with wooden sash	Medium

Table 14 - Shading coefficient and U-value of various glasses (10)

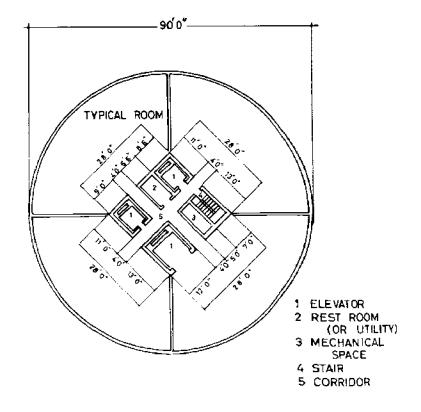
Input Code (153)	Shading Coefficient	U-Value	Type of Glass
1	1.00	0.81	 1/8", 3/32" of regular sheet glass 1/8" of grey sheet glass 1/8" of double strength glass 3/16" of heat absorbing glass
2	0.78	0.81	
3	0.90	0.81	
4	0.72	0.54	

B. Buoyancy Tank

The floor plan and the elevation of the buoyancy tank are shown in Figures 25 and 26. Zoning is not necessary, for the entire tank has similar heat gain characteristics. The cooling load of a typical floor has been calculated by assuming a weighting factor of 1. Therefore, the heat gains and cooling load are identical in this case.

Eight different types of building materials (Table 15) were used for calculating the rate of heat flow through the wall in accordance with Equation 3-8. Finally, four different types of wall materials were selected for calculating cooling load.

Equations for heat gains due to ventilation and light are identical to those for the superstructure. Heat gains due to infiltration and total solar radiation transmitted and conducted through the glass are ignored, as the buoyancy tank is located in sea water.



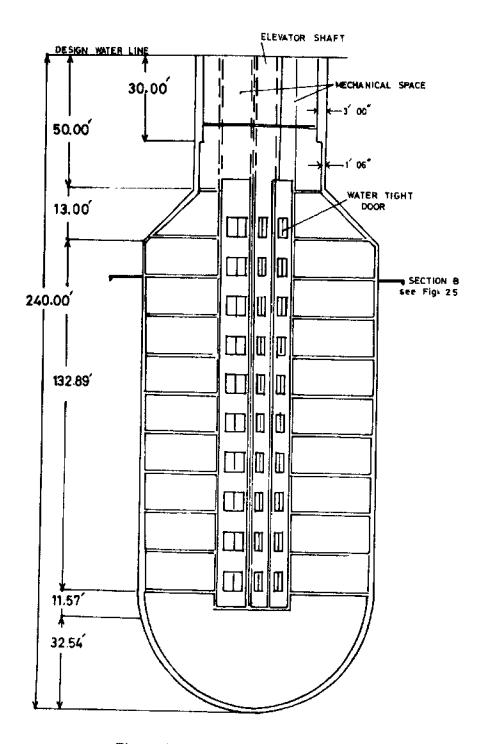


Figure 26 - Elevation of buoyancy tank.

Description of Wall	Overall heat transmission coefficient (Btu/hr-ft ² - ^o F) @ depth			Rate of heat flow (Btu/hr-ft ²) @ depth		
	70 ft	105 ft	140 ft	70 ft	105 ft	140 ft
a	0.397	0.310	0.253	0.556	0.527	0.886
b	0.364	0.296	0.244	0.510	0.503	0.854
с	0.396	0.309	0.253	0.554	0.525	0,886
d	0.356	0.284	0.236	0.498	0.483	0.826
е	0,292	0.233	0.200	0.409	0.396	0.700
f	0.259	0.219	0,200	0.363	0.372	0.662
g	1,973	1,967	0.189	2.762	3.344	6.864
ĥ	0.675	0.481	1.961	0.945	0.818	1,684

Table 15 - Different types of wall configurations for the buoyancy tank and respective rates of heat flow

Symbols:

a = bare concrete

- b = 3/4" gypsum plaster + concrete (outside)
- c 3/8" steel plate + concrete
- d = 3/8" steel plate + concrete + membrane (epoxy)
- e = 3/4" gypsum plaster + 4" air space + concrete
- $f = 3/4^{11}$ gypsum plaster + 4¹¹ air space + concrete + membrane (epoxy)
- g = steel (1% carbon)
- h = 3/4" plaster + 1/2" gypsum board + 4" air space + steel (outside)
- Note: Thicknesses of steel and concrete of buoyancy tank vary in accordance with the depth from the design water level.

depth (ft)	70	105	140	
concrete thickness(ft)	1.0	1.385	1.77	
steel thickness (ft)	0.167	0.208	0.25	

C. <u>Results and Discussion</u>

To facilitate the inspection of the results, the heat gains and cooling loads from the output of the computer program and the calculated values of cooling loads have been plotted.

Figure 27 illustrates the rates of heat gain through 1/8-inch double strength glass with a shading coefficient of 0.9 and an overall heat transmission coefficient of 0.61 Btu/hr-ft^{2-O}F, plotted in accordance with orientations of windows. The glass facing east causes a high heat gain before noon due to direct solar radiation, and the glass facing west receives maximum heat flow in the afternoon. The heat gains of glass facing south and north are always symmetrical about noon time regardless of the time of year. It is surprising to note that the heat gain through a south glass is much lower than that of an east or west glass because of the relationships among solar angles. Sclection of the glasses is one of the most important factors in the design of an air conditioning system. For example, selection of glass with a shading coefficient of 0.72 and an overall heat transmission coefficient of 0.54 Btu/hr-ft²-OF (Table 14) reduces the cooling loads of the superstructure to 60 to 70 percent of that for the superstructure with 1/8-inch double strength glass. This indicates that the selection of glass affects the cooling loads of a superstructure and the capacity of air-handling units as well. Hence, the glass with a smaller shading coefficient and smaller U-value reduces the operation cost of the air-handling units. On the other hand, it increases the initial cost of the superstructure. Therefore, the final decision depends upon the owner's interest and the function of the superstructure.

Cooling loads of a superstructure vary as a function of wall azimuth angles (wall orientations). The total radiative heat and solar heat gain factors at any orientation at any time of year may readily be calculated. Cooling loads for the entire superstructure are easily estimated by specifying the proper wall or window orientation. The note in Table 8 indicates the sample wall orientations.

Figures 28 to 36 show the heat gains from various sources and the total cooling load of typical rooms in the superstructure. The pattern of cooling loads in one zone is entirely different from that in another, which reinforces the concept of dividing the superstructure into several zones for the satisfactory control of indoor environment.

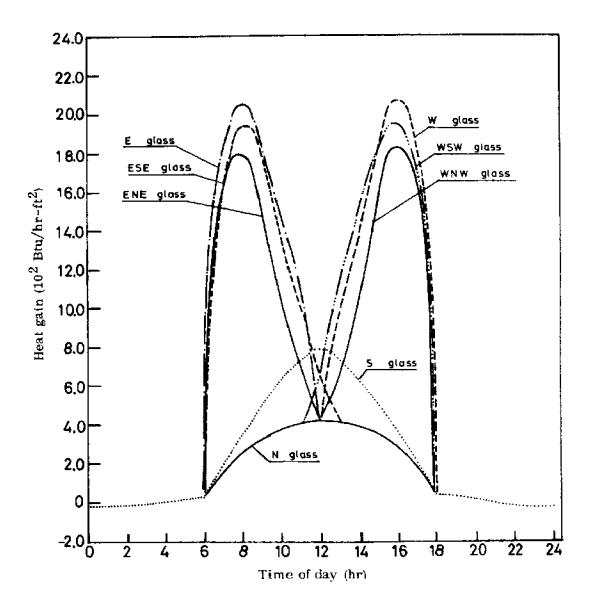


Figure 27 - Heat gain through glass.

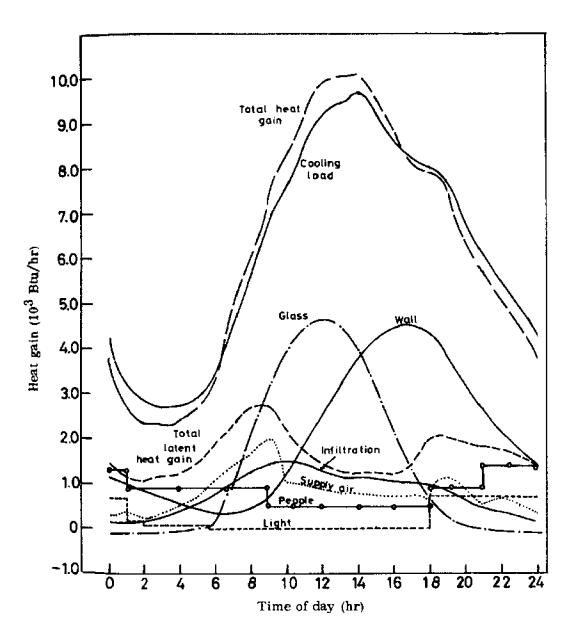


Figure 28 - Heat gains and cooling load of a typical room in superstructure zone A.

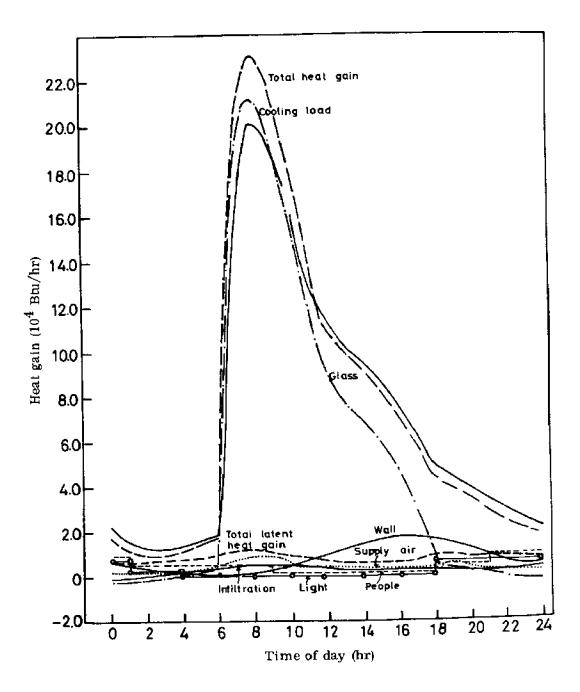


Figure 29 - Heat gains and cooling load of a typical room in superstructure zone B.

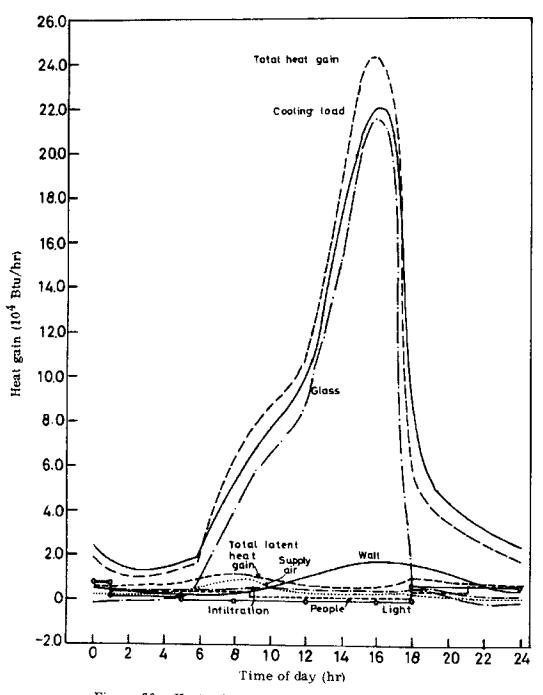


Figure 30 - Heat gains and cooling load of a typical room in superstructure zone C.

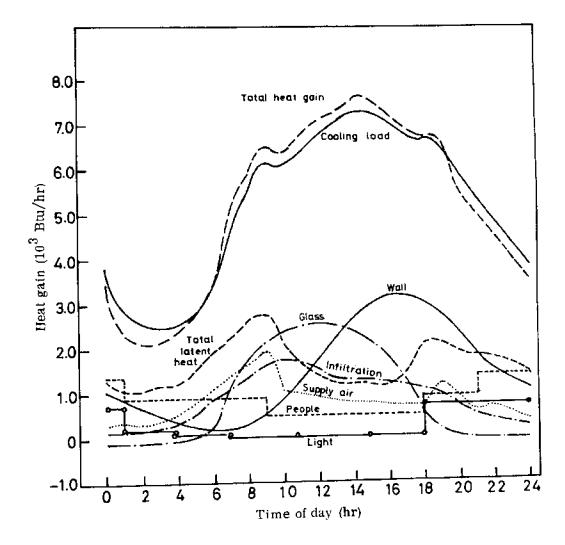


Figure 31 - Heat gains and cooling load of a typical room in superstructure zone D.

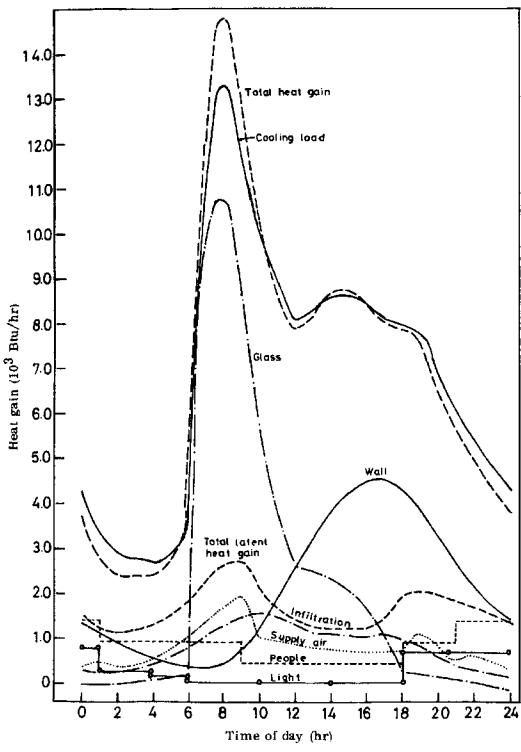


Figure 32 - Heat gains and cooling load of a typical room in superstructure zone E.

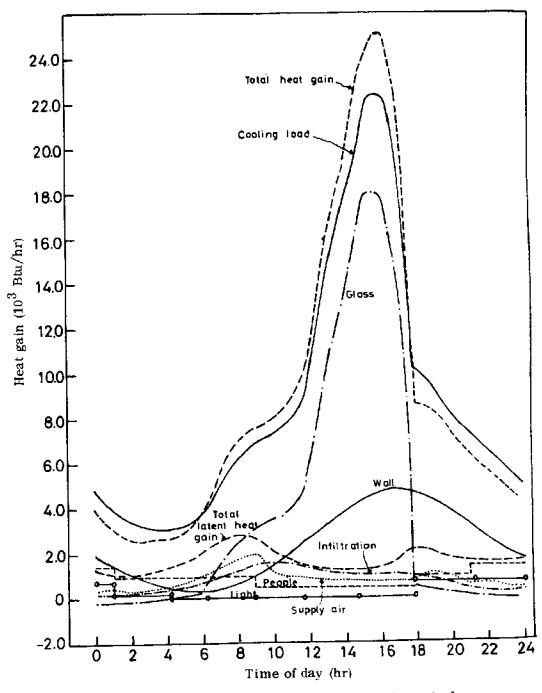


Figure 33 - Heat gains and cooling load of a typical room in superstructure zone F.

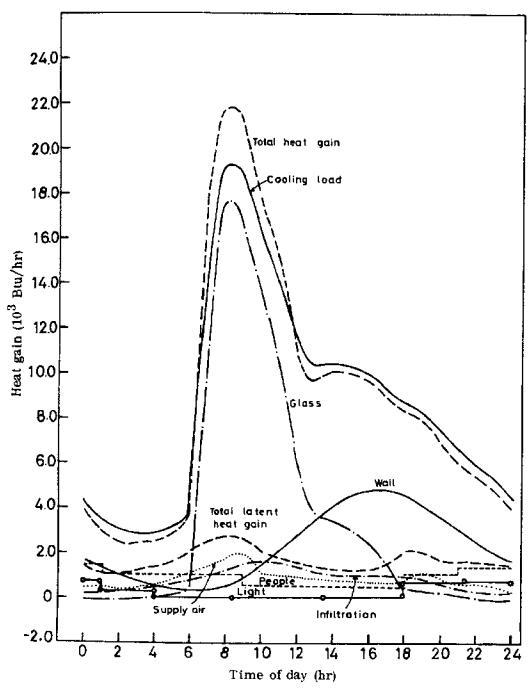


Figure 34 - Heat gains and cooling load of a typical room in superstructure zone G.

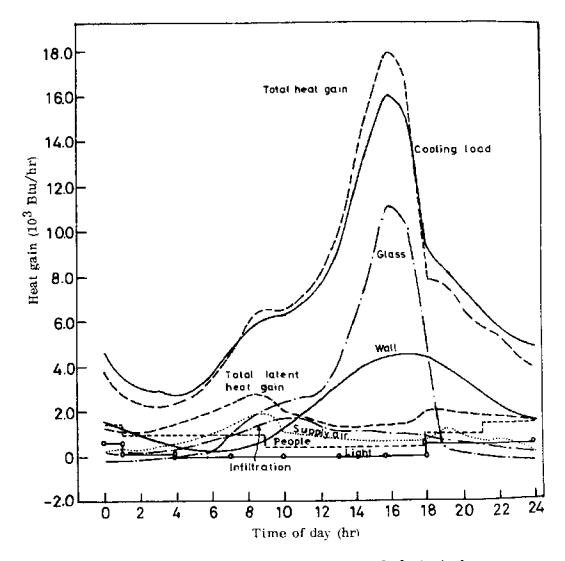


Figure 35 - Heat gains and cooling load of a typical room in superstructure zone H.

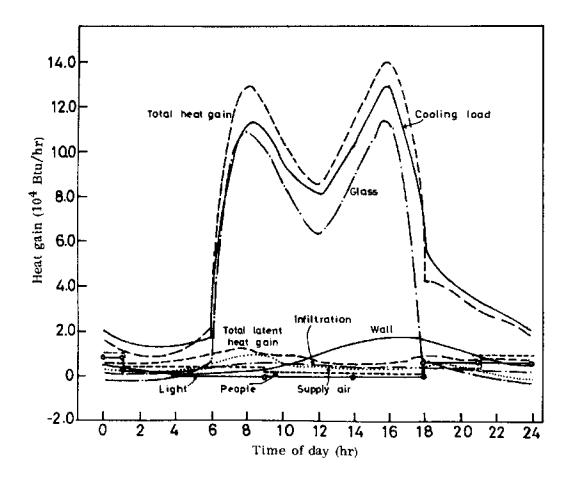


Figure 36 - Heat gains and cooling load of a typical room in superstructure zone I.

Figures 37 to 39 show the cooling load from various sources in a typical room in the buoyancy tank, in conjunction with the depth and the various wall materials. No zoning is required for a typical floor of a buoyancy tank. Heat transfer through buoyancy walls to the sea is not very significant. In fact, for steel, insulation is required.

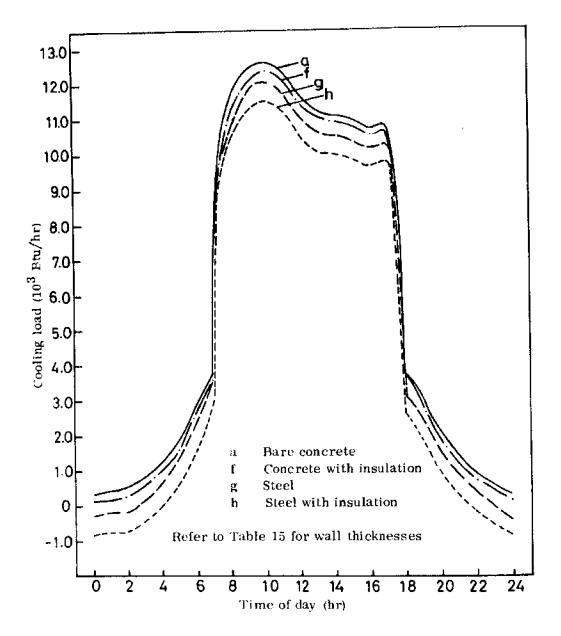


Figure 37 - Cooling load of a typical room in buoyancy tank at the depth of 70 feet from design water line.

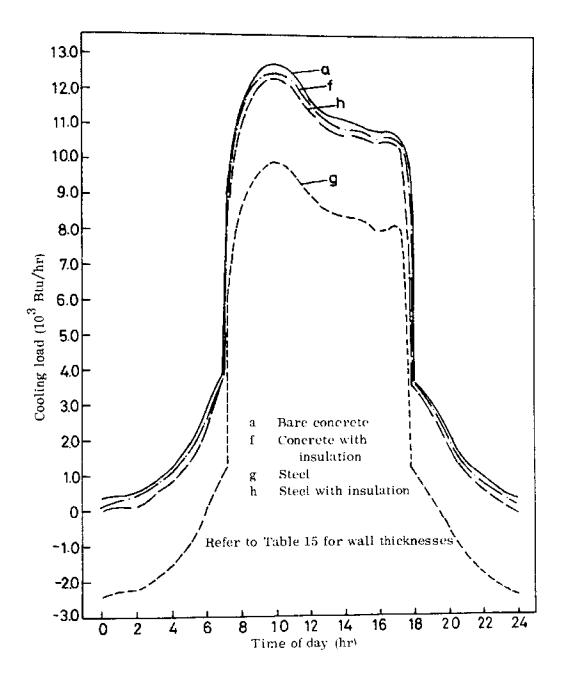


Figure 38 - Cooling load of a typical room in buoyancy tank at the depth of 105 feet from design water line.

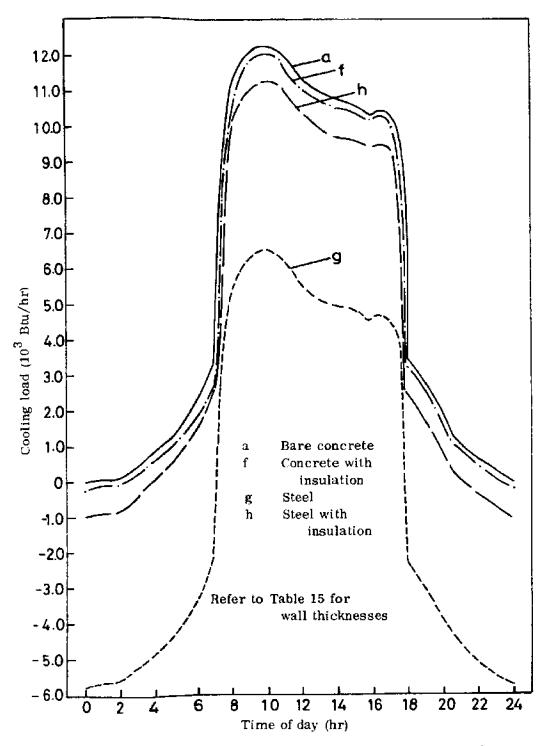


Figure 39 - Cooling load of a typical room in buoyancy tank at the depth of 140 feet from design water line.

VI. REFRIGERATION

A. Energy Considerations

Full-time air conditioning of a large occupied space often contributes a significant portion of the overall power cost for the facility. In the case of the Floating City, the increased size of the electrical power plant required to handle air conditioning demand, along with lighting, mechanical, and other uses of electricity, will have direct cost consequences for the hull itself, in increased fuel storage requirements.

It therefore seems especially important to consider the option of a total energy system. Any system that makes use of waste heat from the power plant to provide drive for air conditioning and refrigeration and for desalination of the city's drinking water will effect a gain in fuel economy. In this case, because the designer has complete control of power plant design, as well as other machinery, the total energy concept would seem to be conspicuously attractive.

B. <u>Superstructure</u>

Application of an absorption cycle for refrigeration is one of the convenient ways to utilize the exhaust heat from the city's power plant. Steam or hot water of approximately 200° F is fed into this cycle, and about 40° F chilled water may be obtained.

Calculations for refrigeration by absorption cycle are performed in accordance with the maximum cooling load of a typical floor, which occurs at 4 p.m. in the superstructure. Values for each zone are shown in Table 16. Water is used for the refrigerant, while lithium bromide serves as the absorbent. All the procedures for calculation of the refrigeration cycle in this section are found in the ASHRAE Handbook (10)

It is seen that the maximum cooling load of 87.43×10^4 Btu/hr should be removed by refrigeration. The refrigeration load of a typical floor is determined by

Refrigeration load =
$$\frac{\text{Cooling load}}{1.2 \times 10^4}$$
 = $\frac{87.43 \times 10^4}{1.2 \times 10^4}$ = 72.86 tons

Zone	Cooling load of a room in each zone (10 ⁴ Btu/hr)	Number of rooms in each Zone	Total cooling load of each Zone (10 ⁴ Btu/hr)
A	0.85	7	5.95
В	7.5	1	7.50
С	21.8	1	21.80
Ð	0.70	3	2.10
E	0,84	10	8,40
F	2, 22	4	8,88
G	1.00	4	4.00
H	1.60	10	16.00
ſ	12, 8	1	12,80
	Cooling load of a typical fl	00r	<u>Σ</u> 87.43

Table 16 - Cooling load of a typical floor in the superstructure at 1600

The cycle for a water-lithium bromide absorption refrigeration machine is shown in Figure 40. This cycle includes a liquid heat exchanger for the absorbent and refrigerant-absorbent streams. The design conditions listed below are selected for high performance. Figure 40 is a flow diagram for the cycle.

1.	Refrigeration load:		tons/hr
2.	Evaporator temperature:	40° F	(this low temperature is desirable for achieving good dehumidification as well as cooling in air conditioning)
3.	Absorbent outlet		
	temperature:		(The absorbent temperature should be kept at about 100° F or lower to reduce the danger of crystallization)
4.	Condenser temperature:	110 [°] F	(This temperature is not critical and may be set higher than the absorber temperature to achieve better use of the cooling water)

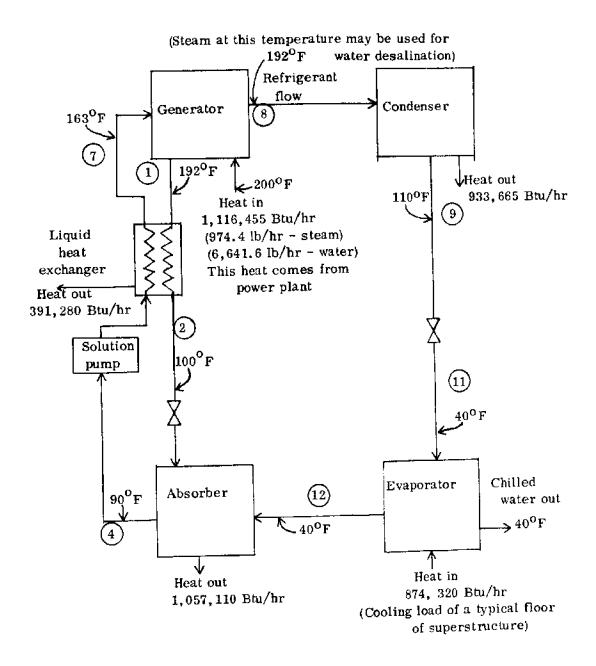


Figure 40 - Lithium bromide-water absorption refrigeration cycle for a typical floor of superstructure.

5. Generator temperature:	192 ⁰ F (This temperature is related
J. Generation	to the condenser temperature
	in such a way that the absorbent
	will be in the feasible
	concentration range)

Pressure drops in this system are assumed to be negligible except for expansion devices. Table 17 is set up and a start is made at filling in the values. Pressures on the low side and high side are the water vapor pressures for the evaporator and condenser, respectively. Enthalpies for water and steam are found in steam tables. Concentrations and enthalpies for llthlum bromide are found in the ASHRAE Handbook (10)

Point	Temp (⁰ F)	Pressure (mm Hg)	Weight (Fraction LiBr)	Flow (lb/lb Refrigerant)	Enthalpy (Btu/lb)
1	192	66	0.61	11.2	-30
2	192	66	0.61	11.2	-70
4	90	6,3	0.56	12.2	-75
7	163	66	0.56	12.2	-38.3
8	192	66	0.0	1.0	1147
9	110	66	0.0	1.0	78
11	40	6.3	0.0	1.0	78
12	40	6.3	0.0	1.0	1079

Table 17 - Conditions	in	lithium	bromide	cycle
-----------------------	----	---------	---------	-------

Relative flow rates are determined from material balance as follows:

$$w_a/w_d = x_b/(x_a - x_b)$$

where

 $w_a = flow rate of absorbent, lb/hr$

- $w_b = flow$ rate of refrigerant, lb/hr
- $x_a =$ concentration of LiBr in absorbent, lb/lb solution
- x_b = concentration of LiBr in refrigerant-absorbent solution, lb/lb solution

$$w_a/w_d = 0.56 (0.61 - 0.56) = 11.2$$

$$w_{h}/w_{d} = (w_{a}/w_{d}) + 1 = 12.2$$

where $w_b =$ flow rate of refrigerant-absorbent solution, lb/hr

The enthalpy of the refrigerant-absorbent solution leaving the liquid exchanger is calculated from energy balance as follows:

$$h_7 = h_4 + [(h_1 - h_2) \times w_a/w_b]$$

= -75 + [(-30) - (-70) × 11.2/12.2]
= - 38.3 Btu/lb

The temperature of 163° F, corresponding to this enthalpy, is found in the ASHRAE Handbook (10).

The refrigerant flow rate is calculated from an energy balance at the evaporator as follows:

$$w_d = refrigerant load/(h_{12} - h_{11})$$

= (1.2 x 10⁴ x 72.86)/(1079 - 78)
= 873.4 lb/hr

The absorbent and refrigerant-absorbent solution rates are next calculated by:

The net heat input to the generator is calculated from an energy balance as follows:

$$q_g = w_d \cdot h_g + w_a h_1 - w_b \cdot h_7$$

= 873.4 (1147) + 9,782 (-30) - (10,656) (-38.3)
= 1,116,455 Btu/hr

Therefore, the flow rate of steam at 200° F is obtained by

$$w_s = q_g/h_s = 1,116,455/1145.78 = 974.4 lb/hr$$

and for hot water of 200° F.

$$w_{H_2O} = q_g / h_{H_2O} = 1,116,455/168.1 = 6,641.6 \text{ lb/hr}$$

where

 w_{g} = flow rate of steam to generator, lb/hr h_{s} = enthalpy of steam at 200° F, Btu/lb $w_{H_{2O}}$ = flow rate of hot water to generator, lb/hr $h_{h_{2O}}$ = enthalpy of hot water at 200° F, Btu/lb

The coefficient of performance on a net basis:

(COP) = refrigeration load/net heat input to generator

$$= 874,320/1,116,455 = 0.783$$

Heat transfer rates for the other components are:

Liquid heat exchanger

$$q_1 \approx w_a(h_1 - h_2) = 9,782 [-30 - (-70)] = 391,280 Btu/hr$$

Condenser

$$-q_c = w_d(h_8 - h_9) = 873.4 (1147 - 78) = 933,665 Btu/hr$$

Absorber

$$-q_{a} = q_{g} + q_{e} + q_{c}$$
$$= 1,116,455 + 874,320 - 933,665 = 1,057,110 \text{ Btu/hr}$$

where $q_e = refrigeration load.$

Results are illustrated in Figure 40.

C. Buoyancy Tank

Following the same procedure and design conditions, the refrigeration process for a typical floor in the buoyancy tank has been calculated in accordance with the different depths and construction materials. Temperatures at each process are kept the same as those for the superstructure. Resultant values are presented in Table 18.

tank
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Table

	Wall	Max. cooling	Refriger-	Refrigerant	Flow rate		Heat transier rate	te	
Depth	Depth descrip-	load	ation load	flow rate	of steam	Generator	Hes	Condenser	Absorber (Bhi/br)
	1001	(Ju/mg)	(600)	(Itu /on)	(m) mL)	(Jut /mg)		(111 /ma)	
	ದ	49,572	4.13	49.5	55.2	63, 290	22,160	52,916	59, 946
	4	50,300	4.19	50.2	56.0	64,159	22,480	53,664	60, 795
2	60	45,856	3.82	45.8	51.1	58, 553	20,520	48,960	55,449
	E	48,112	4.01	48.1	53, 4	61,483	21,560	51,419	58, 176
	ದ	49,684	4,14	49.6	55.3	63, 382	22,240	53,022	60,044
1	f	50,264	4,19	50.2	56.0	64,159	22,480	59,864	54,559
105	50	39,092	3.26	39.0	43.5	49,854	17,480	46,502	42,444
	. с	48,588	4.05	48.6	54.2	62, 136	21,760	51,953	58,771
	e.	48,332	4.03	48.3	53,9	61,729	21,640	51,633	58,428
-	Ŧ	49,172	4,10	49.2	54.9	62,882	22,040	52, 595	59,459
140	ы	25,856	2.15	25,8	28.8	32,988	11,560	27,580	31, 264
	£	45, 332	3.78	45.3	50.5	57,929	20,280	48,426	54,835

*from Table 15

VII. DESIGN OF DUCT SIZE

A. Superstructure

Ducting is one of the most convenient ways to convey the conditioned or ventilation air into a room. Duct size changes in accordance with the function and cooling load of a building and the selection of the air conditioning system. Maximum cooling load differs from one room to another, due to the different orientation of the walls and windows, and the time of day. The application of a zoning system appears reasonable for the design of air ducts. A multi-zone unit system may be best suited for the superstructure, since it can distribute the conditioned air into many different zones in response to the individual thermal requirements of each room. The size of the duct should be based on the maximum cooling load of each zone.

The method used for the calculations of duct size in this section, proposed by the Handbook of Air Conditioning System Design (9), is commonly used. Necessary design conditions for the calculations are based on the values described in Section V. However, the important values for the calculations of duct size are given as follows:

0 0 0	Air temperature of a room Specific humidity of a room Quantity of ventilation air for different zones in a typical floor (cfm _{oa})	78 ⁰ F 0.0125 lb/lb
	Zone A	420 cfm
	В	300
	C	300

С	300
D	180
Ε	600
F	240
G	240
Н	600
Ι	300

 Bypass factor (BF)
 0.15
 (the ratio between the quantity of air which doesn't contact the surface of cooling or heating coils and total amount of supplied air to these coils) By following the procedures proposed by the Handbook of Air Conditioning System Design, calculations of the required quantity of supply air have been made. These are based on the time of day when the maximum cooling load occurs, which may be different for each zone.

For Zone A (at 2 p.m.):

Effective room sensible heat (ERSH)

 \sim Room sensible heat (RSH) + (BF) x 1.08 x cfm_{off} x ($\theta_0 - \theta_i$)

 $\times 8732 \pm (0.15) \ge 1.08 \ge 420 \ge (88,60 - 78,0)$

- 9,453 Btu/hr

Effective room latent heat (ERLH)

= Room latent heat (RLH) + (BF) x 1.08 x $efm_{oa} x (W_o - W_i)$

 $= 1268 + (0, 15) \times 1,08 \times 420 \times (0,0154 - 0,0125)$

- 1,268 Btu/hr

Effective sensible heat factor (ESHF)

ERSH/(ERSH) ERLH) = 9,453/(9,453 + 1,268) = 0.88

Air-handling units should be kept dry mainly for the prevention of corrosion. Apparatus dew-point temperature (θ_{adp}) indicates the minimum allowable temperature to prevent the condensation of moist air. As the latent load for Zone A is not large in comparison with the sensible load for the same space, application of a dehumidification and cooling system is a suitable method (Figure 41).

Conditions of supply air change in accordance with the selection of the bypass factor (BF), outside and inside air conditions, mixing ratio between outside and inside air, selection of cooling coils and cooling load of a room. The mixing ratio, BF, and cooling coils may be selected arbitrarily to satisfy the thermal requirements of an individual room. Since Zone A is used for guest room purposes, a BF of 0.15 is recommended. The conditions of air at different points in Figure 41 can be found by the following formulas:

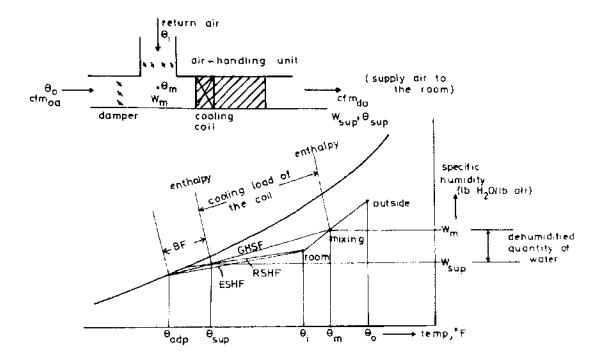


Figure 41 - Dehumidification and cooling system for the superstructure.

RSHF (Room sensible heat factor)

$$= \frac{\text{RSH} + (\text{BF}) [1.08 \text{ x} \frac{\text{cfm}_{oa}(\theta_{o} - \theta_{i})]}{\text{RSH} + (\text{BF})[1.08 \text{ x} \text{cfm}_{oa}(\theta_{o} - \theta_{i})] - 0.68 \text{ x} \text{cfm}_{da}(W_{i} - W_{sup})}$$
$$= \text{RSH}/(\text{RSH} + \text{RLH})$$

GSHF (Grand sensible heat factor)

$$= \frac{\text{RSH} + 1.08 \text{ x } \text{cfm}_{0a}(\theta_0 - \theta_i)}{\text{RSH} + 1.08 \text{ x } \text{cfm}_{0a}(\theta_0 - \theta_i) + \text{RLH} - 0.68 \text{ x } \text{cfm}_{0a}(W_0 - W_i)}$$

= (RSH + OASH)/[(RSH + OASH) + (RLH + OALH)]
- TSH/(TSH + TLH)

To facilitate the above process, resultant values for Zone A are illustrated in Figure 42.

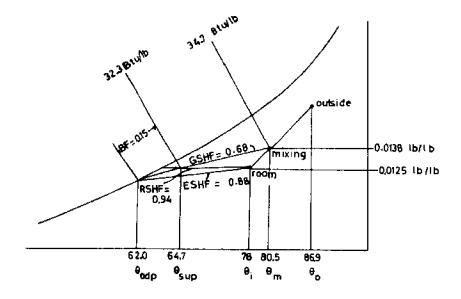


Figure 42 - Condition of air for Zone A.

The required quantity of supply air (cfm_{da}) for Zone A is estimated as follows \cdot

$$cfm_{da} = ERSH/[1.08 \times (1 - BF) (\theta_i - \theta_{adp})]$$

= 9453/[1.08 x (1 - 0.15) (78 - 62.0)]
= 686.5 cfm

In the same manner, the required quantities of supply air for the other zones have been calculated and are shown in Table 19.

To fulfill the function of ducting in a practical manner, the system must be designed within acceptable ranges of the following factors: friction, velocity, sound level, heat and leakage losses. Upon considering these items, sound level, heat and leakage losses can be neglected by selecting the proper duct size and insulation materials. Leakage loss is unpredictable, as it depends on quality of workmanship. Application of low velocity, 1200 - 2500 fpm, is suited for commercial comfort air conditioning, such as in offices, hotels, schools, and apartment houses. High velocity is applicable for factory use. At a constant low pressure, such as 0.15 inch water gage at all terminals, the recommended velocity is found in

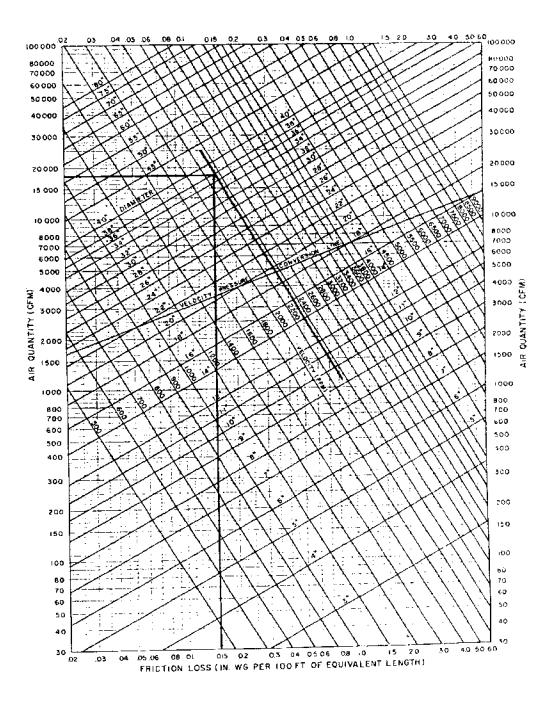


Figure 43 - Determination of air velocity in ducts for Zone A.

Zones	ERSH	ERLH	ERSH + ERLH	ERSH/ (ERSH+ERLH)	θ _{adp}	Required air quantity	Time of day
A B C D F G H 1	$\begin{array}{r} 9,453\\ 190,092\\ 207,233\\ 6,214\\ 11,461\\ 16,911\\ 21,428\\ 15,817\\ 123,204 \end{array}$	1,268 12,200 12,200 1,305 2,622 2,622 1,268 1,268 5,729	10,721 202,292 219,433 7,519 14,083 19,533 22,696 17,085 128,933	$0.94 \\ 0.83 \\ 0.81 \\ 0.87$	62 64 63.8 62.5 62.6 63.3 63.8 63.6 63.8	$\begin{array}{r} 687\\ 14,791\\ 15,892\\ 437\\ 811\\ 1,253\\ 1,644\\ 1,197\\ 9,451 \end{array}$	1400 0800 1600 1500 0800 0800 1600 1600 1600

Table 19 ~ Conditions of air and the quantity of supply air for each zone in the superstructure

conjunction with the quantity of supply air (Figure 43). In the process of determining the duct size, we must find the efm percentage, duct area percentage, and duct area. They are estimated by the following procedures:

efm percentage		<u>al supply air quantity</u> x 100 al supply air quantity
Duet area perce	entage	This is found in Table 20 in conjunction with cfm percentage
Duct area — Init	ial duct	area x duct area percentage

Duct sizes are then found in Table 21.

Therefore, the remaining important values for Zone A are estimated by following the above procedures. By taking into consideration Figure 43, an example calculation for Zone A of direction $B \sim 1$ is used for the determination of duct size. In addition, ducting for Zone A is considered to be one of the branches from the main duct, which takes care of

CFM CAPACITY	DUCT AREA SZ	CFM CAPACITY	DUCT AREA %	CFM CAPACITY %	DUCT AREA	CEM CAPACITY	DUCT
1	2.0	26	33.5	51	590	76	a · :
7	3.5	27	34.5	52	50 0	77	87.2
3	5.5	28	35.5	53	61.0	78	1 82 0
4	7.0	29	36.5	54	620	79	34.1
5	90	10	37.5	5.5	63.0	68	84 5
	10.3	31	39.0	5-6	64.0	81	83.5
7	11.5) 22	40.0	57	65.0	82	365
8	13.0	33	41.0	58	65.5	63	87.0
P	14,5	14	42.0	59	56.5	84	67.5
10	\$6.5	35	43.0	60	67.5	85	85.36
- 11	17.5	36	44.0	61	68.0	86	89.2
12	18.5	37	▲ 5.0	62	69.0	87	90.0
13	19.5	38	46 C	63	70.0	ê B	92.5
14	20.5	39	47.C	64	71.0	₿9	9.2
15	21.5	40	48.D	65	71.5	¢0	920
16	23.C		49.0	66	71.5	• • • •	93.0
17	24.0	42	50.0	67	73.5	92	94.0
18	25.0	43	\$1.0	63	74.5	C9	94.5
19	28.0	44	52.0	69	75.5	94	\$5.0
20	27.0	45	53.0	70	76.5	55	96.0
21	29.0	45	\$4.0	71	77.0	96	98.5
22	29.5	47	55.D	72	78.0	97	97.5
23	30.5	48	56.0	73	79.3	89	9 8 ()
24	31.5	439	57.0	74	60.0	64	\$9.5
25	32.5	5D	58.0	75	60.3	100	19972
_							
OF (FM Copor	·	60% (PM C	an est-				
1007° Areo	~	67.5% Acen]				
		<u> </u>					

Table 20 - Percent section area inbranches for maintaining equal friction

Zones A, C and D. Initial supply air quantity is the sum of these zones, namely 18,520 cfm.

Initial duct velocity = found from Figure 43 in conjunction with the friction loss of 0.15 in. water gage and the initial supply air quantity of 18,520 cfm

Initial duct a rea = $18,520/2,300 = 8.05 \text{ ft}^2$

cfm percentage = $(3,500/18,520) \ge 100 = 18.9$

Duct area percentage = 25.9 (found from Table 20 by interpolation of cfm capacity)

Duct area = initial duct area x duct area percentage

 $= 8.05 \times 0.259 = 2.08 \text{ ft}^2$

		6			1	0		12	יו	14	• •	6	1	8	2	0	2	2
H04	Aree eq fi	Duarn in.	Area aq fi	Diam in.	Area sq ft	Diam in-	Area sqft	Diam in.	Ares aq fi	Diam m.	Ana 1	Diam in.	Area sq ft	Diem in.	Ares sq ft	Drent in.	Area 19 H	Dıa in
10	39	81	.51 /	9.8	.63	10.9							r					
12	.45	9.1	.62	,	.97	11.9	j.94	13.1							•		•	
14	.52	9.8	.72	- 1 5.5	.91	12.9	1.07	14.2	1.28	15.3								
14	.59	10.4		12.2	1.02	13.7		15.1	1,45	16 J	1.67	17.5						
18		110	.91	12.9	1.15	14.5		16.0	1.63		1.47	18.5	2.12	19.7				
20	.72	115	.99	13.5	7.26	13.2	1.54	- 16.8	1.01	18.2	2.07	19.5	2.34	20.7	2.61	21.9	.	
<u></u>	70	12.0	1.00	14.1	1.30	159	1.69	17.6	1.99	19.1	2.27	20.4	2,57	21.7	2.86	22.9	3.17	24
24	#4	12.4	1.16	14.6	1.50	166	1.83	18.J	2.14	19.8	2.47	21.3	2.78	22.6	3.11	23.9	3 43	?
26	.89	11.8	1.26	15.2	1.61	17.2	1.97	19.0	3.31	20.6	7.64	22.1	3.01	23.5	3.35	24.8	3.71	20
24	.95	13.2	1.33	15.6	[1.71 _D	1.45	2.09	19.6	2.47	21.3	2.86	22.9	1.25	24.4	1.60	25.7	4.00	23
10	1.01	13.6	1.41	16.1		5 19.3.	2,72	20.2	Z.64	22.0	3 06	23.7	3.46	25.2	3.89	26.7	4.27	20
32	1.07	14.0	1.46	16,5	1.93	-18.8	2.36	20.8	2.81	12.7	3.25	24.4	3.68	26.0	4.12	27.5	4.55	2.
34	1.13	14 4	1.56	170	2.03	19.3	2.49	21.4	j 2.96	23.J	3.43	25.1	3.89	26.7	4.17	28.3	4.81	25
44	1.10	14.7	1.65	17.4	2.14	19.8	2.61	21.9	3.11	23.9	3.63	25.8	4.09	27.4	4.58	29.0	5.07	3
38	1.23	15.0	1.73	17.8	2.25	20.3	2.76	22_5	8.27	24 5	3.60	26.4	4.30	28.1	4.84	29.8	5.87	3
40	1.20	15.5	1.81	18.2	2.33	20.7	2.00	23.0	3,43	25.2	3.97	27.0	4.52	28.8	S.07	30.5	5.62	3
43	1 33	156	1.84	18.5	2.43	21.5	2.90	23.4	2.57	25.6	4.15	27.6	4.21	29.4	5.31	31.2	5.86	3
44 	1.38	15.9	1.95	18.9	2.52	21.3	3.11	23.9	1.71	26.1	4.33	28.2	4.90	30.0	5.5\$	31.9	6.12	3
46	1.43	16 2	2.01	19.2	2.61	21.9	3.22	24.3	3.66	26.7	4,49	28.7	5.10	30.6	3.76	37 5	6.37	3
48	1.48	16.5	2.07	196	2.71	22.3	3.35	24.8	4.03	27.2	4 65	29.2	5.30	31.2	5.97	33.1		3
50			2.14	199	2.01	22.7	3.44	25.2	4,15	27 6	4.84	29.8	5.31	31.8	4.19	33.7	6.87	3
52			2.32	20.2	2.91	23.1	3.57	25.6	4 30	28.1	5.00 L	00.J	5.72	J2.4	6.41	343	7.14	J
54			2.29	20.5	2.98	234	3.71	26 1	4,40	28.5	3.17	30.8	5.90	32.9	6.64	34.9	7.35	3
56			2.38	30.9	2.09	23.8	3.03	26.5	4.55	28.9	5.31	31.2	6.08	33.4	6.87	35.5	7.62)
58	1		2.43	28 1	3.19	24.2	3.94	26.9	4.14	29 3	5.48	31.7	6.26	33,9	7.Dé	36.0	Z 47	3
60			2.50	21.4	3 27	24.5	4.06	27.5	4.14	29.8	5 65	32.2	6.50	34.5	7.26	36.1	8.12	3
64 			2.64	22.0	3.44	25.2	4.24	27.9	\$. 10	30.6	5.91		6.87	35.5	7,71	37.6	8.59	3
64	1				3.63	35.8	4.49	28.7	5.17	31.4	6.26	33.9	7.10	36.3	B.12	38.6	9.01	4
73	†				3.83	26.5	4.71	29.4	\$ 69	32.3	8,60	34.8	7.54	37.2	8.50	39.5	9.52	_4
74		~ ~			407	27.4	4.91		5.86	32.8	4.63	35.4	7.95	38.2	6.90	40.4	998	4
80	ł –				4.13	27.6	5.17	J0.8	6.15	33.6	7.72	36.4	8.29	39.0	9.21	6 211	10.4	4
84	[5.41	31.5	6.41	J4 5	7.54	37.2	8.55	39.6	9.75L	- 42.3	10.8	4
D.C	l						5.58	32.0	<u>+ 14</u>	34.9	7.17	0.80	8.94	4 0.5	10.1 `	40.1	11.2	
63						1	5.79	J2.6	6.91	35.6	# 12	38 6	9.39	41.5	10.4	43.8	11.7	- 4
94 00	1						5.90	33.0	7.14	36.2	\$.40	39.1	9.70	42.1	10.0	44.5	12.1	•
									7.40	36.9	8.50	39,5	9.80	42.5	11.3	45.5	12.3	4
04	1								7.60	37.4	B.90	40.5	10.3	43.5	11.6	46.2	13.0	4
08 12		:							7.90 8.10	38.0 38.6	9.20	41.2	10.6	44.0	12.0	47.0	13.4	4
	· ··· ·	··							•	38.6	9."0	41.8	10.9	44.2	12.3	47.5	13.8	
16		1									9.40	\$2.4	11.3/	45.5	72.6	48.1	14.3	5
20 24		i									10.0 10.3	42.8	11.3	° 46.0	13.1	49.1	14.4	5.
												43.5	13.9	46.7	13.4	49 6	15.0	5
28											10.6	44.1	12.1	47.1	13.8	59.4	15.5	5.
32 36				i									12.5	47.9	14.1	50.9	15.8	Ş
~ -	.						<u> </u>		├				12.0	48.5	14.5	516	16 2	5
40													13.0	48.5	14.7	52.0	16.5	52
44					_					-			13.3	49.4	15.2	52.9	T 6.8	- 51

Table 21 - Duct dimensions, section area, circular equivalent diameter, and duct class

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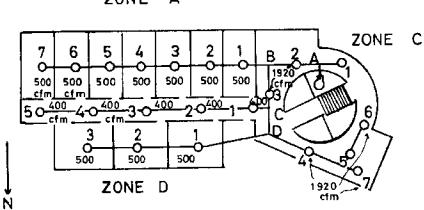
SIDE		24		26		28	_	30		32	ļ	34		36		38	- <u>-</u>	40
	Area sq fi						n Area sq fi		Area sq ft	Dian in.	n Area sqft					Dian	Arec	
10			·									<i>.</i>	sq ft	in.	sq f	t in.	sq f	t in
12					ļ		Í						1					
14		·													1			
16 18									T				+					
20																		
22			+															
24	3.74	26.	,						i i									
26	4.03	27.		28.	4								ĺ		1			
28	4.33	28.2	2 4.74														1	
30	4.68	29.3		30.:			1						1				+	• <u>-</u>
32	4.94	30.1	5.37	31.		32.6	1	32.8 33.8	6.68	35.0								
34	5.24	31.0	5.69	32.	3 6.15	33.6			+				_				}	
36	5.58	32.0		33.0	1	34.6	6.99	34.8 35.8	7.06	36.0		37.2					1	
38	5.86	32.8	6.38	34.2		35.5	7.34	36.7	7.46	37.0 38.0	7.95	38.2	8.46	39.4				
40	6.15	33.6	6.71	35.)	7.22	36.4	7.71	176	+			39.2	8.89	40.4	+	41.6		
42	6.45	34.4	7.03	35.9	1 .	37.3	8.12	- 3 8 .6	8.29 8.68	39.0 39.9	8.81 9.21	40.2	9.34	41.4		42.6	10.5	43.
44	6.75	35.2	7.34	36.7	7.91	38.1	8.50	39.5	9.07	40.8	9.61	41.1 42.0	9.80	42.4		43.6	11.0	44.
46	7,03	35.9	7.63	37.4	8.25	38.9	8.85	40.3	9.48	41.7	10.1			43.4	10.8	44.6	11.4	45.
48	7.30	36.6		38.2	8.59	39.7	9.25	41.2	9.89	42.6	10.1	43.0 43.9	10.7	44.3	11.3	45.6	11.9	46.
50	7.58	37.3	8.25	38.9	8.90	40.4	9.61	42.0	10.3	43.5	10.9	44.8	11.1	45.2 46.1	11.8	46.5	12.4	47.
52	7.87	38.0	8.55	39,6	9.25	41.2	9.98	42.8	10.7	44.3	11.4				+	47.4	13,0	48.
54 56	8.16	38.7	8.85	40.3	9.61	42.0	10.4	43.6	11.0	45.0	11.8	45.7 46.5	12.1 12.6	47.1 48.0	12.7	48.3	1,3.5	49.
	8.42	39.3	9.16	41.0	9.94	42.7	10.7	44.3	1.4	45.8	12.2	47,3	13.0	48.8	13.2	49.2 50.1	14.0	50.0 51.5
58 60	8.63	39.8	9.48	41.7	10.3	43.4	11.0	45.0	11.8	46.6	12.6	48.1	13.4	49.6	14.2			
64	8.89 9.43	40.4 41.6	9.75 10.3	42.3	10.5	44.0	11.4	45.8	12.2	47.3	13.0	48.9	13.8	50.4	14.6	51.0 51.8	15.0 15.5	52.4
68	+			43.5	11.2	45.4	12.1	47.2	12.9	48.7	13.8	50.4	14.7	52.0	15.5	53.4	16.5	53.3 55.0
72	9.98	42.8	10.9	44.7	11.8	46.6	12.8	48.4	13.7	50.2	14.6	51.8	15.6	53.5	16.5	55.0	17.5	
76	10.8	43.8	11.5	45.9 47.0	12.4 13.1	47.8	13.5	49.7	14.4	51.5	15.4	53.2	16.4	54.9	17.4	56.5	18.3	56.6 58.0
80	11.5				{	49.0	14.1	50.8	15.1	52.7	16.2=0		17.3	56.3	18.3	57.9	19.3	59.5
84	12.0	46.0 46.9	12.6 13.2	48.0 49.2	13.7	50.1	14.7	52.0	15.8	53.9	17.0	55.8	18.1	57.6	19.2	59.3	20.3	61.0
88	12.5	47.9	13.7	49.2 50.1	14.2 14.8	51.1 52.2	15.4	53.2	16.5	55.0	17.7	57.0	18.9	58.9	20.1	60.7	21.2	62.4
92	12.9	48.7	14.2				16.1	54.3	17.3	56.3	18.5	58.2	19.7	60.1	20.9	62.0	22.1	63.7
96	13.3	49.5	14.8	51.1 52.2	15.5 15.9	53.4 54.0	16.7 17.2		18.0	57.4	19.2		20.5	61.3	21.8	63.2	23.0	65.0
100	13.9	50.6	15.0	52.5	16.7		17.9		18.6 19.2	58.5	19.7		21.1	62.2	22.7	64.5	24.0	66.3
104	14.6	51.8	15.8	53.9	17.1	+				+	20.6		21.6	63.0	23.4	65.5	24.8	67.5
108	14.8	52.1	16.2	54.6	17.6	1	18.6 19.2		19.9 20.5		21.4		22.7	64.5	24.1	66.5	25.6	68.5
112	15.1	52.7	16.8	55.5	18.3		19.7		21.1		22.0 22.5		23.5	65.7	24.8		26.5	69.7
116	15.8	53.9	17.3	56.4	18.9	-58.9	20.3						24.5	67.0	25.7	68.7	27.1	70.5
120	16.2	54.6	17.8	57.1	19.4	-59.6	20.3		22.0 22.7	•	23.5		24.8	67.5	26.2	1	28.2	71.9
24	16.6	55.2	18.4	58.1	19.8		21.6		23.2		24.2 25.2		26.1 26.5	69.2	27.2		29.0	73.0
28	17,1	56.0	18.8	58.8	20.3	61.1	22.3								28.2		29.8	74.0
32	17.4	56.5	19.3	59.5	20.8		22.6	1			25.6 26.3		27.3 28.2		28.7	1	30.2	74.5
36	17.9	57.3	19.7	60.2	21.4	62.7	23.0				26.9		28.7		29.8 30.5		32.0 32.6	76.6
40	18.5		20.3	61.0	22.3	64.0	24.1	66.5 2		·	27,5		9.4				·	77.3
	18.8	58.7	20.6	61.5	22.7	64.5 $1.3 \frac{(ob)}{(a + b)}$	4.8				28.2		(9.4 19.9		31.5 32.0		33.4 34.0	78.3 79.0

Table 21 - Duct dimensions, section area, circular equivalent diameter, and duct class (cont.)

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Duct size = 22×16 (found from Table 21) which has a greater duct area than that for the direction B-1 of 2.08.

In the same manner, the other necessary values are estimated and presented in Table 22. Figure 44 shows the supply air distribution of Zones A, C and D.



ZONE А

Figure 44 - Air supply diagram for Zones A, C and D.

Table 22 - Duct sizes for Zones A, C and D

Operation pressure for all terminals Initial duct velocity Duct area (18, 520/2, 300) 0.15 inch water gage 2,300 fpm 8.05 ft²

		Air	cfm	Duct area	Duct	Duct size
		Quantity	percentage	percentage		width x height
Zone	Direction	<u>(cfm)</u>	(%)	(%)	(ft^2)	(inches)
	to A	18,520	100	100	8.05	60 x 22
	A - 1	1,920	10.4	16.9	1.36	16 x 14
	A - 2	16,600	89.6	92.0	7.41	56 x 22
	2 - B	14,680	79.3	84.2	6.78	50 x 22
С	В-3	11, 180	60.4	67.7	5.45	40 x 22
	3 - C	9,260	50.0	58.0	4.67	34 x 22
	C - D	7,260	39.2	56.2	4.52	32 x 22
	D - 4	5,760	31.1	39.1	3.15	22 x 12
	4 - 5	3,840	20.7	27.7	2.23	22 x 16
	5 - 6	1,920	10.4	16.9	1.36	16 x 16
	5 - 7	1,920	10.4	16.9	1.36	16 x 14
	В-1	3,500	18.9	25.9	2.08	22 x 16
	1 - 2	3,000	16.2	23.2	1.87	18 x 16
	2 - 3	2,500	13.5	20.25	1.63	16 x 16
	3 - 4	2,000	10.8	17.3	1,39	18×12
A	4 - 5	1,500	8.1	13.2	1.06	14 x 12
	5 - 6	1,000	5.4	9.6	0.77	12 x 12
	6 - 7	500	2.7	4.9	0.39	12 x 6
	C - 1	2,000	10.8	17.3	1.39	18 x 12
<u>ម</u>	1 - 2	1,600	8.6	14.2	1.14	16 x 12
Corridor	2 - 3	1,200	6.5	11.25	0.91	12 x 12
11	3 - 4	800	4.3	7.6	0.61	12 x 8
ပိ	4 - 5	400	2.2	3.9	0.31	12 x 6
	D - 1	1,500	8.1	13.2	1.06	14 x 12
D	1 - 2	1,000	5.4	9,6	0.77	12 x 12
	2 - 3	500	2.7	4.9	0.39	12 x 6

In the same manner, other necessary values are estimated for Zones B, E and F along with the necessary air supply diagram (Table 23 and Figure 45).

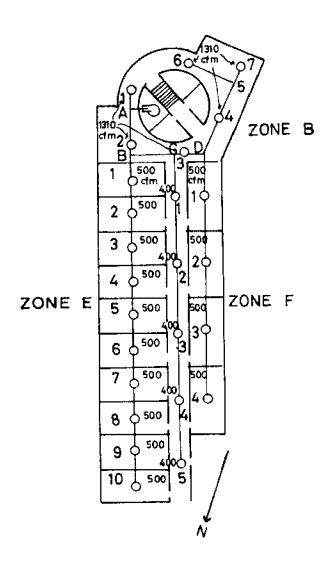


Figure 45 - Air supply diagram for Zones B, E and F.

Table 23 - Duct sizes for Zones B, E and F

0.15 inch water gage
2,300 fpm
17,460 cfm
7.59 ft ²

•						Dust
		Air	cfm	Duct area	Duct area	Duct size width x heigi
Zone	Direction	Quantity	percentage	percentage	(\mathbf{ft}^2)	(inches)
None	Direction	<u>(efm)</u>	(%)	<u>(%)</u>	(11-)	(incles)
	to A	17,460	100	100	7.59	56 x 22
	A - 1	1,310	7,5	12.25	0.93	$12 \ge 12$
	A - 2	16,150	92.5	94.25	7.15	52 x 22
	2 - B	14,840	85.0	88.5	6.72	44 x 22
в	B - C	9,840	56.4	64.4	4.89	36 x 22
	C - 3	7,840	44.9	53.0	4.02	30 x 22
	3 - D	6,530	37.4	45.4	3.45	26 x 22
	D - 4	3,930	22,5	29.75	2.26	22 x 16
	4 - 5	2,620	15,0	21.5	1.63	16 x 16
	5 - 6	1,310	7.5	12.25	0.93	16 x 10
	5 - 7	1,310	7.5	12.25	0.93	16 x 10
	B - 1	5,000	28.6	36.25	2.75	$24 \ge 18$
	1 - 2	4,500	25.8	33.4	2.54	$22 \ge 18$
	2 - 3	4,000	22.9	30.4	2.31	20 x 18
	3 - 4	3,500	20.0	27.0	2.05	18 x 18
Е	4 - 5	3,000	17.2	24,2	1.84	18 x 16
	5 - 6	2,500	14.3	20.8	1.58	16 x 16
	6 - 7	2,000	11.5	18.25	1.39	16 x 14
	7 - 8	1,500	8.6	13.9	1.06	14 x 14
	8 - 9	1,000	5.7	11.5	0.88	14 x 10
	9 - 10	500	2.9	5.3	0.40	10 x 10
	C - 1	2,000	11.5	18.25	1.39	16 x 14
л С	1 - 2	1,600	9.2	14.7	1.12	14 x 14
Corridor	2 - 3	1,200	6.9	11.4	0.87	14×10
or 1	3 - 4	800	4.6	8.2	0.62	10 x 10
Ŭ	4 - 5	400	2.3	4.1	0.31	10 x 6
	D - 1	2,000	11.5	18.25	1.39	1 6 x 14
F	$\frac{1}{1} - 2$	1,500	8.6	13.9	1.06	10 x 14 14 x 14
	2 - 3	1,000	5.7	11.55	0.88	14×10 14 x 10
	3 - 4	500	2.9	5.3	0.40	14×10 10 x 10

In the same way, necessary values for Zones G, H and I are found as shown in Table 24. Figure 46 is the air supply diagram.

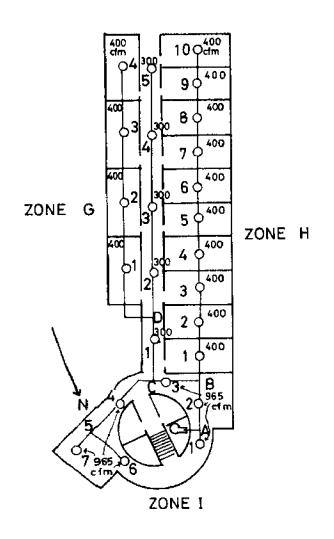


Figure 46 - Air supply diagram for Zones G, H and I.

Table 24 -	Duct	sizes	for	Zones	G,	H and I
------------	------	-------	-----	-------	----	---------

Operation pressure for all terminals	0.15 inch
Initial duct velocity	2,150 fpn
Duct area (12,890/2,150)	6.0 ft 2

		Air	cfm	Duct area	Duct	-
		Quantity	percentage	percentage	area	١
Zone	Direction	<u>(cfm)</u>	(%)	(%)	(ft^2)	
	to A	12,890	100	100	6.0	
	A - 1	965	7.5	12.25	0.74	
	A - 2	11,925	92.5	94.25	5.66	
	2 ~ B	10,960	85.0	88.5	5.31	
1	B - 3	6,960	54.0	71	4.26	
	3 - C	5,995	46.5	54.5	3.27	
	C – 4	2,895	22.5	29.75	1,79	
	4 - 5	1 ,9 30	15.0	21.5	1.29	
	5 ~ 6	965	7.5	12 . 2 5	0.74	
	5 - 7	965	7.5	12.25	0.74	
	B - 1	4,000	31.0	39.0	2.34	
	1 - 2	3,600	27.9	35.5	2.13	
	2 - 3	3,200	24.8	32.1	1.93	
	3 - 4	2,800	21.7	28.8	1.73	
Н	4 - 5	2,400	18.6	25.6	1.54	
	5 - 6	2,000	15.5	22.25	1.34	
1	6 - 7	1,600	12.4	18,9	1.13	
	7 - 8	1,200	9.3	14.8	0.89	
	8 - 9	800	6.2	10.7	0.64	
1	9 - 10	400	3.1	5.7	0.34	
	C - 1	3,100	24.1	31.6	1.90	
L L	1 - D	2,800	21.7	29.1	1.75	
- 2	D - 2	1,200	9.3	15.1	0.91	
Corridor	2 - 3	900	7.0	11.5	0.69	
l S	3 - 4	600	4.7	8.4	0.50	
	4 - 5	300	2.3	4.1	0.25	
	D - 1	1,600	12.4	18.9	1.13	
G	1 - 2	1,200	9, 3	15.1	0.91	
Ĭ	2 - 3	800	6.2	10.7	0.64	
	3 - 4	400	3.1	5.7	0.34	

B. Buoyancy Tank

Calculations for the determination of duct size for two zones in the buoyancy tank are based on the following design conditions:

- oAir temperature of a room 78° FoSpecific humidity of the rooms (Wi)0.0125 lb/lboQuantity of ventilation air360 cfmoBypass factor (BF)0.05
 - (Application residence, factory, wherever the high latent heat occurs)

Latent heat gain is fairly large in the buoyancy tank. The main heat gains depend on the heat from people and ventilation, both of which have high latent heat. This situation requires the use of cooling with dehumidification, and a reheat cycle to increase the efficiency of the air-conditioning system as well as to reduce the size of the air duct. This cycle is illustrated in Figure 47.

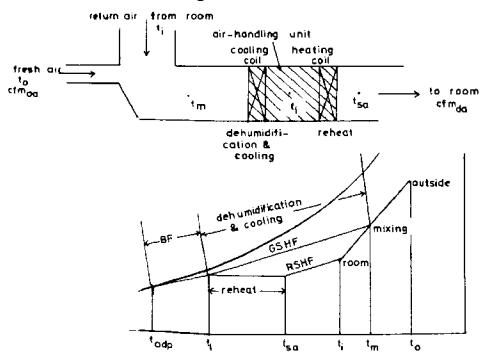


Figure 47 - Dehumidification with cooling and reheat.

The required air quantity is determined by the following procedu for bare concrete at 70 ft depth:

OASH = 1.08 x cfm_{oa} (
$$t_0 - t_i$$
) = 1.08 x 360 (86.9 - 78) = 3,460 (Bt
OALH = 0.68 x cfm_{oa} ($W_0 - W_i$)grain = 0.68 x 360 (120.5 - 86)
= 8,446 (Btu/hr)

Assume a bypass factor of 0.05 because of high latent load

ESHF =
$$\frac{\text{RSH} + (\text{BF}) (\text{OASH})}{\text{RSH} + (\text{BF}) (\text{OASH}) + \text{RLH} + (\text{BF}) (\text{OALH})}$$

=
$$\frac{12,176 \div 0.05(3,460)}{12,176 \div 0.05(3,460) + 12,610 \div (0.05)(8,446)} = \frac{12,3}{12,349 \div}$$

= 0.487
where OASH = Sensible heat of outside air

here OASH = Sensible heat of outside air OALH = Latent heat of outside air cfm_{oa} = Ventilation (fresh) air from outside

When plotted on the psychrometric chart, this ESHF doesn't inten the saturation curve. Referring to the apparatus dew-point in Table 25 53° F is found in conjunction with the ESHF of 0.6.

Therefore, the amount of reheat (Btu/hr) required to produce an ESHF of 0.6 is

$$0.6 = \frac{12,349 + reheat}{12,349 + 13,032 + reheat}$$

reheat = 7,199 Btu/hr

Required air quantity is estimated by

$$cfm_{da} = \frac{ERSH}{1.08 \times (1 - BF)(t_{1} - t_{adp})} = \frac{12,349 + 7,199}{1.08 (1 - 0.05)(78 - 53)}$$
$$= \frac{19,548}{25,65} = 762$$

Temperature of air entering the cooling coil (t_m) is given by

$$t_{m} = \frac{(cfm_{oa} \times t_{o}) + (cfm_{ra} \times t_{i})}{cfm_{da}}$$
$$= \frac{(360 \times 86.9) + (402 \times 78)}{762}$$
$$= 82.2^{\circ} F$$

Leaving condition of air from cooling coil (t_1)

$$t_1 = t_{adp} + BF (t_m - t_{adp})$$

= 53 + 0.05 (78 ~ 53)
= 54.25⁰ F

Supply air temperature to the room (t_{sa})

 $t_{sa} = t_i - \frac{RSH}{1.08 (cfm_{da})} = 78 - \frac{12,176}{1.08 (762)} = 78 - 14.8$ = 63.2° F

Resultant values for this calculation (bare concrete at 70 ft depth) are illustrated in Figure 48. In the same manner, the other required air quantities are calculated and presented in Table 25.

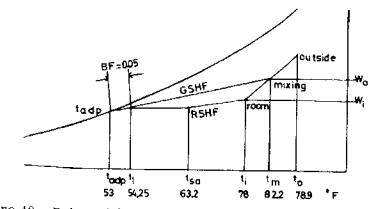


Figure 48 - Dehumidification with cooling, and reheat for buoyancy tank with bare concrete at depth of 70 feet.

$^{\rm tga}_{\rm (OF)}$	63. 2	63.2	66.0	62.7	63, 3	63.4	;	62.9	62.8	63.1	1	61.3	
cfm _{da} (cfm)	762	784	798	691	768	796	ł	715	702	743	ł	556	
Reheat load (Btu/hr)	7,199	7,745	4,412	6, 104	7,283	7,718	(-661)	6,461	6,269	6,899	(-10, 588)	4,019	
tadp (^O F)	53	53	53	53	53	53	53	53	53	53	53	53	
Corrected ESHF	0.6	0.6	0.6	0.6	0.6	0.6	0.6	0.6	0.6	0.6	0.6	0.6	
ESHF	0.487	0.494	0.446	0.471	0.488	0.493	0.353	0.476	0.474	0.482	0.036	0.440	
OALH (Btu/hr)	8,446 2,110	8,446	8,446	8,446	8,446	8,446	8,446	8,446	8,446	8,446	8,446	8,446	
OASH (Btu/hr)	3,460	3,46U	3,460	3,460	3,460	3,460	3,460	3,460	3,460	3,460	3,460	3,460	
RLH (Btu/hr)	12,610	12,610	12,610	12,610	12,610	12,610	12,610	12,610	12,610	12,610	12,610	12,610	
RSH (Bu/hr)	12,176	12,040	10,318	11,446	12, 232	12,522	6,936	11,684	11,556	11,976	318	10,056	: : :
wall descrip- tion*	તાં પ	1	ы¢.	г	ಣೆ	f	භ	ч	æ	Ŧ	ත	а	
Depth (ft)	02	2				105				140			

Table 25 - Required air quantity for two rooms in a typical floor

Table 25 shows that the amount of supply air required for a typical floor of the buoyancy tank at a depth of 70 ft is fairly similar for different wall configurations. At a depth of 105 ft, bare steel causes a lot of condensation on the inner surface of the wall. To maintain comfort conditions in a room, it may be necessary to install huge refrigeration machines and boilers. Hence the use of a bare steel wall for the buoyancy tank at this depth sounds impractical. However, the addition of insulation such as air space, gypsum board and/or plaster finish reduces this problem. The required quantity of supply air for a room with bare concrete walls is similar to that for steel with insulation. This means the applicability of steel with insulation is equivalent to that of bare concrete. Therefore the problem of condensation is no longer a disadvantage with a steel wall.

At a depth of 140 ft, the use of steel with insulation materials seems more economical than bare concrete in terms of the operation cost of the air-handling unit. Reheat load and required air quantity are the least among the four different configurations, because this configuration has the smallest total heat gain.

Following the same procedures described previously, design of duct size for a typical floor in the buoyancy tank is estimated for a depth of 105 ft. Bare concrete is selected as the sample material for the outside wall, and the necessary design conditions for the ducting are shown in Table 26. The supply air diagram is shown in Figure 49. Table 26 - Duct sizes for buoyancy tank

Operation pressure for all terminals	0.15 inch wate
Initial duct velocity	1,300 fpm
Required air quantity to be	
supplied to buoyancy tank	1,800 cfm
Duct area (1,800/1,300)	1.38 ft ²

Direction	Air Quantity	cfm percentage	Duct area percentage	Duct area	Duet width :
<u> </u>	(cfm)	(%)	(%)	(ft^2)	<u>(in</u>
to A	1,800	100	100	1.38	22
A - 1	900	50.0	58.0	0.80	14
1 - 2	750	41.7	49.7	0.58	10
2 - 3	600	33.3	41.3	0.46	10
3 - 4	450	25.0	32.5	0.35	10
4 - 5	300	16.7	23.7	0,23	10
5 - 6	150	8,3	13.2	0.11	10
A – 7	900	50,0	58.0	0.80	14
7 ~ 8	750	41.7	49.7	0.58	10
8 - 9	600	33.3	41.3	0.46	10
9 - 10	450	25.0	32.5	0.35	10
10 - 11	300	16.7	23.7	0.23	10
11 - 12	150	8.3	13.2	0.11	10

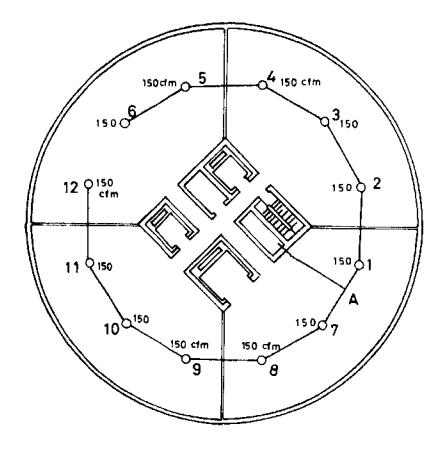


Figure 49 - Supply air diagram for buoyancy tank.

VIII. SUMMARY AND CONCLUSIONS

1. The climatic data show in Section I would indicate that refrigeration requirements for the superstructure would be relatively small because of the low internal heat gains and the relatively open structural plan. This was not found to be the case. Total heat gain is rather large and is dominated by sun loads on walls and glass, as shown in the curves in Section V. C. Proper attention to shading, reflective exterior finishes, etc., would significantly reduce total loads, perhaps leading to a condition where part-time air conditioning would suffice for the superstructure. The method used for investigating heat loads lends itself readily to an optimization of the thermal design by tracing the effect of each material or configuration change through the heat flow simulation. Thus, useful comparisons can be made between refrigeration and ventilating costs on the one hand and structural and finish costs, or even esthetic merit, on the other.

2. Analysis of heat flow in the exterior walls of the buoyancy chambers (Section V. C) shows that even though the area in contact with the sea is very large, its contribution to the heat budget of the city's underbody is not important. In fact, when uninsulated steel buoyancy chambers were examined, an <u>increase</u> in refrigeration load was required, accompanied by reheating, to limit condensation on the inside surface (Section VII, p. 98). It seems clear that, at least for Hawaii's climate, the fact of the city's immersion in the sea has no value thermally. Removal of the city's rejected heat will have to be obtained conventionally, i.e., by pumped cooling water.

3. For urban applications of very large floating platforms, comfort air conditioning will demand large amounts of energy. The use of a steam absorption cycle for refrigeration, followed by distillation desalination, appears to be an efficient way to minimize the city's total fuel bill. It is rendered feasible by the fact that the entire mechanical plant for the city can be designed at one time, in contrast to the usual urban case.

2405

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APPENDIX A

LIST OF SYMBOLS

All the special uses of symbols are described wherever they occur.

A	Surface area, ft ²
A _{fl}	Surface area of floor, ft ²
Aw	Surface area of wall or roof, ft^2
а	Thermal diffusivity, ft^2/hr
CL	Cooling load, Btu/hr
с _р	Specific heat, Btu/lb- ^O F
$\mathbf{F}(t)$	Temperature excitation, ⁰ F
нс	Total convective heat gain, Btu/hr
HG	Total radiant heat gain, Btu/hr
h _i	Inside unit surface conductance, Btu/hr-ft $^{2-0}$ F
ь _о	Outside unit surface conductance, Btu/hr-ft ^{2_0} F
^I d	Diffuse solar radiation, Btu/hr-ft ²
I nd	Direct solar radiation, Btu/hr-ft ²
τ	Transmitted solar radiation, Btu/hr-ft 2
k	Thermal conductivity, Btu/hr-ft- ⁰ F
l	Length of wall, ft
L	Thickness of wall or roof, ft

L_{eq}	Equivalent thickness, ft
L _s	Thickness of equivalent single-layer wall, ft
Q, q	Rate of heat transfer, Btu/hr or Btu/hr-ft ²
r _o , r _i	Radius, ft
R	Resistance, hr-ft ^{2-o} F/Btu
SC	Shading coefficient
SHGF	Solar heat gain factor, Btu/hr-ft ²
t	Time, hr
U	Overall heat transmission coefficient, Btu/hr-ft ^{2_0} F
v	Volume of room air, ft ³
w _i	Specific humidity of room air, lb/lb
w _j	Weighting factors
w _o	Specific humidity of outside air, lb/lb
x	Distance, ft
$\mathbf{x}_{\mathbf{j}}$	Response factors, Btu/hr-ft ² - ⁰ F
Yj	Response factors, Btu/hr-ft ²⁻⁰ F
z_j	Response factors, Btu/hr-ft ² - ^o F
a	Absorptivity
aj	Absorptances of double-strength glass
Δt	Time interval, hr
η	Incident angle, deg

0	Temperature, ⁰ F
θ _f ī	Surface temperature of floor, ^O F
θ _i	Temperature of room air, ^O F
θo	Temperature of outside air, ⁰ F
θ _s	Surface temperature of wall or roof, ^{O}F
ρ	Density, lb/ft^3
τ_{j}	Transmittances of double-strength glass

APPENDIX B

PROGRAM FLOW DIAGRAM

The program flow diagram is presented in the following pages. The entire program was written in FORTRAN IV and the calculations were performed on the IBM 360/65 computer. The subroutines are described briefly below.

Subroutine SUN determines the intensities of direct, diffuse and total solar radiation. The heat gains through sunlit double-strength sheet glass can be calculated for different orientations at any time of the year.

Subroutine RESFAC, in conjunction with subroutines SLOPE, FALSE, MATRIX, DER and ZERO, is for the calculation of response factors. Table 6 contains all the necessary input data for subroutine RESFAC. Subroutines for the calculation of response factors are taken from the computer program for analysis of energy utilization in postal facilities (18).

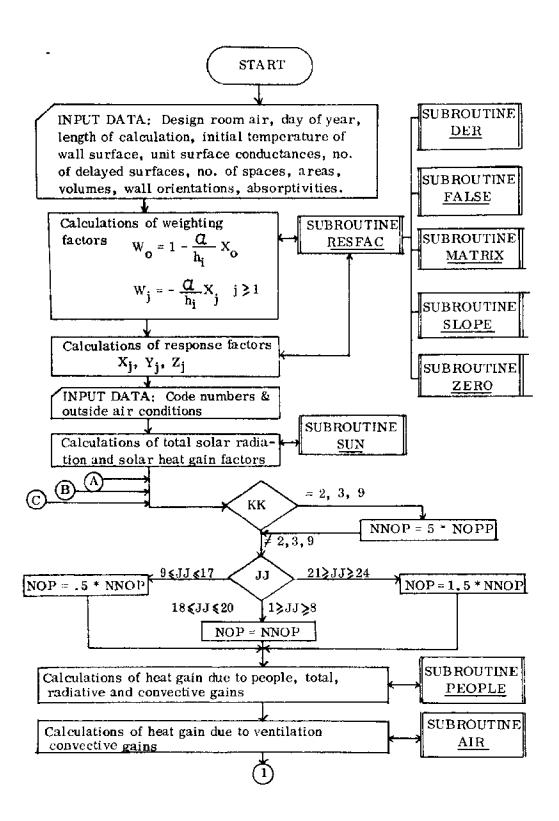
Subroutine AIR calculates the total heat gain due to ventilation in accordance with Equation 3-8 and data from Tables 7, 9 and 12.

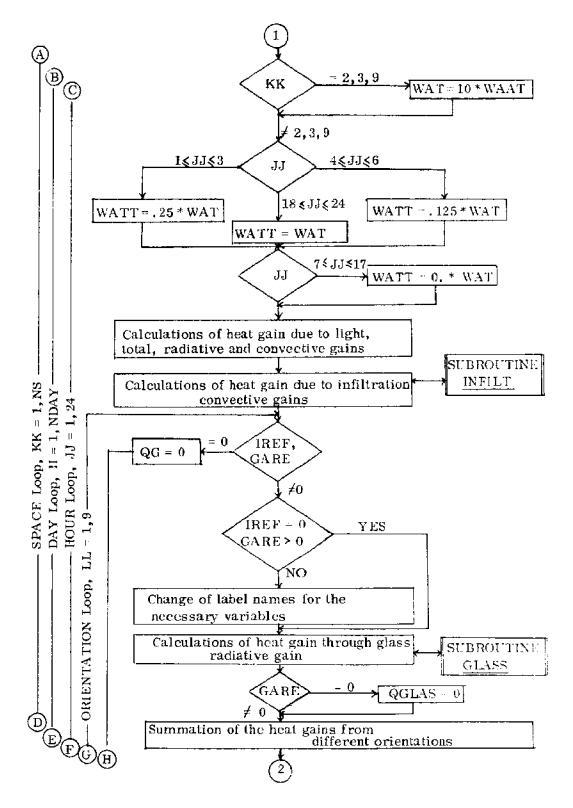
Subroutine INFILT calculates the heat gain due to infiltration of outside air through cracks in the windows and doors. Calculations are based on Equation 3-9, with the proper code numbers selected from Tables 7 and 13.

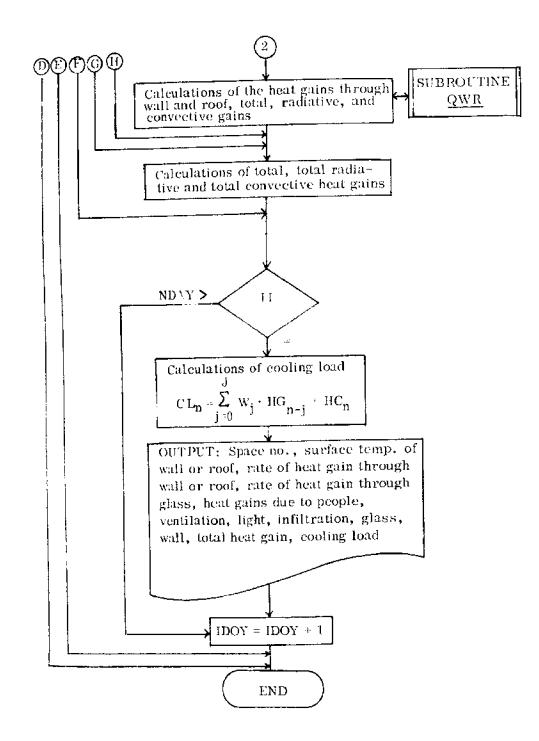
Subroutine GLASS calculates the heat gain through glass by using Equation 3-2 and Table 14. Subroutine QWR calculates the heat gain through the wall or roof by the response factor method. Calculations are based on Equation 3-5 with data from Tables 6 and 7.

Weighting factors, from Equations 4-1 and 4-2, and heat gain due to lights are programmed in the main program.

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APPENDIX C

PROGRAM LISTING AND SAMPLE OUTPUTS

1	8 JO 8	YOSHI YAMASHITA.TIME=1.PAGES=100 .LINES=60 DIMENSION REX(100).REY(100).REZ(100).TIR(100).RX(10.100)
2 3 4 5		DIMENSION REFILO, DUG, XCI(1001, YG1(1001, XG2(1001, YG2(100) DIMENSION DX1(1001, GX2(100), GY1(100), GY2(1001, GG12', 9) DIMENSION TOTROD(24, 91, SHGE(24, 9), TR:D(24), SHEAC(24) DIMENSION GG(24), HG(24), TTO(24), WHO(24), TD(9, 100)
6 7 8 9 10 11		DIMENSION IS(100), QGAIN(24,9),0P(24),0P(24),0P(24) DIMENSION DAIR(24),0L124F,0INF(24),0DTCT(48),CCR(10) DIMENSION OUNT 24,4),TTS(24,9),0U5(24),00G(24,9) DIMENSION ARF(10,9),GANET(10,9),42B(10,9),VOL(10),1NEF(10,9) DIMENSION ALFA(5),WTL 10,201,0P(2010),0TTCT(10), W1000)
ĨŹ	ç	DIMENSION UPR(24),0PC(24),0LF(24),0LC(24) DIMENSION OTUTE(48),0TDTC(48),0CONV(48),WCR(48),WCC(48)
13	с с с	READ AIR TEMPERATURE(DEG.F) AND SPECIFIC FUMIDITY(LB/LB) OF THE RCOM READ(5.500) TR,WR
14	c c	READ THE DAY OF YEAR PE4D(5,501) IDDY
15	C C	READ THE LENGTH OF CALCULATION (DAYS) READ(5,502) NDAY
10	C	READ THE INITIAL SURFACE TEMPERATURE OF WALL AND ROCFIDEG.F) READ(5,504) TDB
17	c c	T S(1) =708
16	с с с	READ THE OUTSIDE AND INSIDE UNIT SURFACE CONDUCTANCES (BTU/HR-FT*FT/F) READ(5,500) FD,FI
19 20	C	READ THE NUMBER OF DIFFERENT DELAYED SURFACES[WALL AND REOF] READ(5.504) ww NGW#W#+0.1
21	с с с	READ THE NUMBER OF SPACES IN THE BUILDINGIZONE A TO IA READ(5,504) FNS
22	c	NS=FNS+0.1
23		READ THE SURFACE AREA OF THE OUTSIDE WALL AND ROCF(FT*FT). SUFFACE AREA DE OUTSIDE GLASS(FT*FT), AND THE ABSORPTIVITY OF OUTSIDE WALL AND ROCE SURFACE READ(5,531) ((ARE(1,J),GARE(1,J),AAB(1,J),J=1,9),I=1,NS)
24	C C	PEAD THE VOLUME OF A ROOM READ(5,504) (VOL(1),1=1,NS)
25	с с с	READ THE WALL ORIGNTATIONS AS GIVEN IN THE NUTE IN TABLE III READ(5+530) ((IREA(1+J)+J=1+9)+I=1+NS)
26	ι ι ι	READ THE ARSORPTIVITY FOR THE WALL OF EQUIVALENT THICKNESS (BTU/HR-FT=FT), EQS.(4-1), (4-2) READ(5.500) (ALFA(J),J=3,4)
27 28 29 30	C	CALCULATION OF THE RUGH WEIGHTING FACTORS DD 33 I=3.4 CALL RESFAC(R1.RFX.RFY) AA=ALFA(I) B=AA/FI

31			WT(I+1)=1+U-8* RFX(1)
32			00 30 L=7,20
ۇ ۋ			WT[1+L]=-6* RFX1L1
34		- 30	CONTINUE
35		33	CONTINUE
36			00 100 I=1.NCW
20	С		
- 1	-		CALL HESFAC (RL, RFX, RFY)
37	~		CHEL RESTACTORINI ALKERT
	C		
38			CCRITIAN
	C		
	C		K DENOTES THE CAFITAL J IN EQUATION (3-5)
37			K=20
40			I [K (I)=K
41			CCK(I)=RL
			NNIR=K-1
42			
43			$\cup \mathbf{X} \mathbf{I} = \mathbf{O}$.
44			UY]=0.
45			00 101 J≏1+NNOR
40			F X{[;;]}=``FX{]}
47			b
48			UX1=UX1+FFX(J)
49			
		104	CONTINUE
50 53		103	C DHIINGE RXLI→KI=PFX{K]
51			
52			RY(I,K)=KFY(K)
53			TD50P=TC6 -TR
54			XQ1431=0X1*T0PDP
55			XQ2(1)=(UX1+PFX(K)/11-0-R1))=TDROP
50			YQ1 LI)≃UYI≪TOPOP
57			¥JZ[[]={U¥1+RFY[K}/[1.0-R1)]#TDROP
58		1.00	CONTINUE
59		100	00 115 J=L,100
-			DD 116 IT1.9
00			
61			TO(I,J)=TDB
62		112	CONTINUE
	C		
	C		READ THE CODE NUMBERS AS SPECIFIED IN TABLES VI. VII.
	<u>_</u>		VIII AND IN, REPERINCE NUMBERS OF PEUPLE AND POWER INPUT
	Ç		FRUM LIGHTS (WATT)
63			READ(5,507) 150,151,152,153,NUPP,WAAT
	C		
	č		PEAD DRY-BULE TEMPERATURE(DEG.F) AND SPECIFIC HUMIDITY
	ũ		LEVLED OF OUTSIDE AIR
	~		READ(5,508) (T10(1), +++0(1), 1=1, 24)
64			REAU();)007 (+10/17+************************************
	C		
65			CALL SUNTIDOY, SHGE, TETRAD
	C		
	¢		SPACE LOUP STARTS FROM HERE
66			DO 120 KK=1-NS
67			0 = 4 M
	C		
	Ē		DAY LOUP STARTS FROM HERE
68	-		DO 104 11=1, HDAY
	Ċ		
	č		HOUR LODE STARTS FROM HERE
,	L,		
67			DO 105 JJ=1,24
-	¢		
Τù			TO=TTO(JJ)
71			wij=wwetjj}
72			NN 3P = 93PP
73			IF(KK.30.2.08.KK.FJ.3.08.KK.E0.9) NNOP=5*NOPP
14			IF(11.3F.21.4ND.JJ.LF.24) NOP=1.54NNOP
75			IF(JJ.J.J.I.AND.JJ.LF.BJ NCP=NNOP
76			IF(JJ.5E.9.AND.JJ.LE.17) NCP=0.5*NNOP
77			1F(JJ.GE.18.AND.JJ.LC.20) NOP=NNOP
			TITUTATICANALASALLADI. NO. LADI

C 78 CALL PEOPLE(150,NCP,OPP) C OPP IS THU REDIATIVE PART OF H D D D D D D D D D D D D D D D D D D D	
C OPP IS THE REDIATIVE PART OF H	
U UPP IS THE REDIATIVE PART OF H	
U UPC IN THE CONVECTIVE PART OF I	SAUGAIN DUE TE PENPLE Heat cain cue ta ceraie
UPC IS THE CONVECTIVE PART OF I UP IS THE TOTAL HEAT GAIN DUP :	TC PEARLS DUE EU MEUMES
	IG FEDFLE
/9 Q₽(JJ)=Q₽P	
80 QPR(JJ)≠0.4≠CPP	
81 UPC(JJ)=0.2*CPP	
Ĺ	
82 CALL AIRLISI, NOP, TO, TR, WO, WR, Q	
C HEAT GAIN DUE TO VENTILATION H	AS NO RADIATIVE PART OF
C HEAT GAIN TO COOLING EDAD C	
JAND=(LL) RIAG 68	
by HATSHAAAT	
85 1FIKK.::Q.2.0P.KK.2Q.3.0R.KK.2Q	.9] WAT=10.##A&T
85 1F(JJ-GE-18-1NO-JJ-LF-24) WATT	
87 IF(JJ.GE.1.AND.JJ.LE.3) mATT=0	.25*#AT
88 IF(JJ.GE.4.AND.JJ.LE.6) wATT=0	.125*WAT
89 IF(JJ.GE.7.AND.JJ.LE.17) WATT=	0.=WAT
6	
C CALCOLATION OF HEAT GAIN DUE TH C DE 15 THE TOTAL HEAT GAIN DUE	
C OF IS THE TOTAL HEAT GAIN DUE C OFF IS THE RADIATIVE PART OF G	
C JLC IS THE CONVECTIVE PART OF I	
90 XLT=1.25=3.4+W4TT	
91 ÚEÍJJ)≑XLT	
9∠ ⊋L∺IJJ)=0.5+XLT	
93 OLGIJJJ=0.5+XLT	
C	
94 V=VGL(KK) C	
95 CALL INFILTIISZ,VyTC,TK,NO,AK,	1 () (6) ()
L HEAT GAIN DUL TO IMPLITRATION I	HAS NO PADIATIVE
C HEAT GAIN DUE TO INFLUTRATION I C PART OF HEAT GAIN TO COULING L	
C PAST OF HEAT GATS TO CUGLING L. C 95 GINF(J3)≃QINFL	
C PAST OF HEAT GAIN TO CUOLING L. C 95 GINF(J3)=QINFL 97 QM=Q.	
C PAST OF HEAT GAIN TO CUOLING L. C 95 GINFLJ3J=QINFL 97 QW=0. 98 GGL=0.	
C PAST OF HEAT GAIN TO CUOLING L. C 95 GINFLJ33=QINFL 97 QW=0. 98 GGL=0. C	UAC
C PAST OF HEAT GAIN TO CUOLING L. C 95 GINFLJ3J=QINFL 97 QW=0. 98 GGL=0.	UAC
C PAST OF HEAT GAIN TO COULING L. C	DAD TS FROM HERF
C PART OF HEAT GAIN TO CUULING L. C GINF(JJ)=QINFL 97 OH=0. 98 GGL=0. C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL=1.9 C IF(IRFF(KK,LL).EQ.0.AND.GARE(K)	DAD TS FROM HERF
C PART OF HEAT GAIN TO CUULING L. C GINF(JJ)=QINFL 97 QH=Q. 98 GGL=O. C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL = 1,9 C IF(IRFF(KK,LL).EQ.Q.AND.GARE(KI 100 IF(IRFF(KK,LL).EQ.Q.AND.GARE(KI 101 SHG=SHGF(JJ+LL)	DAD TS FROM HERF
C PART OF HEAT GAIN TO CUULING L. C GINF(JJ)=QINFL 97 OH=0. 98 GGL=0. C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL = 1,9 C I I I F(IKFF(KK,LL).EQ.0.AND.GARE(KI 100 IF(IKFF(KK,LL).EQ.0.AND.GARE(KI 101 SHU=SHUF(JJ+LL) 102 TTK=ICIRAD(JJ+LL)	DAD TS FROM HERF
C PART OF HEAT GAIN TO CUULING L. C GINF(J3)=QINFL 97 QM=0. 96 GGL=0. C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL=1.9 C IF(IRFF(KK,LL).EQ.0.AND.GARE(KM LOI SHU=SHUF(JJ.LL) 102 TTK=TCIRAD(JJ.LL) 103 4B=AA3(KK,LL)	DAD TS FROM HERF
C PART OF HEAT GAIN TO CUULING L. C GINF(J3)=QINFL 97 QH=0. 98 QGL=0. C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL=1.9 C IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 100 IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 101 SHU=SHUF(JJ+LL) 102 TTK=TCIRAD(JJ+LL) 103 4B=AA3(KK,LL) 104 ASEA=ARE(KK,LL)	DAD TS FROM HERF
C PART OF HEAT GAIN TO CUULING L. C G 96 GINF(JJ)=QINFL 97 QHR0. 98 GGL=0. C C C C C C C C C C C C C C C C C C C	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO CUULING L. C GINF(J3)=QINFL 97 QHR0. 98 QGL=0. C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL=1.9 C IF(IRFF(KK,LL).EQ.OAAND.GARE(KI 100 IF(IRFF(KK,LL).EQ.OAAND.GARE(KI 101 SHURSHUF(JJ.LL) 102 TTK=TCIRAD(JJ.LL) 103 ABRA3(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL)	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO CUULING L. 0 0 96 GINF(JJ)=QINFL 97 0H=0. 98 GGL=0. C 000 OF WALL ORIENTATIONS STAR 99 00121 LL=1.9 C 100 100 IF(IRFF(KK,LL).EQ.0.AND.GARE(KILO) 101 SHU=SHUF(JJ.LL) 102 TTK=TCIRAD(JJ.LL) 103 4B=A43(KK,LL) 104 ASEA=ARE(KK,LL) 105 GAREAREGKK,LL) 106 IF(IREF(KK,LL).EW.0.AND.GARE(KIL)) 107 IRC=TIRE)	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO CUULING L. C GINF(J3)=QINFL 96 GINF(J3)=QINFL 97 QM=0. 96 GOLEO. C C 100 IF(IRFF(KK,LL).EQ.O.AND.GARE(K)) 101 SHUESHUF(JJ.LL) 102 TTK=TCIRAD(JJ.LL) 103 AB=AA3(KK,LL) 104 ASLA=ARE(KK.LL) 105 GAREAKE(KK.LL) 106 IF(IREF(KK.LL).EW.O.AND.GARE(K)) 107 IREFILE(KK.LL) 108 CHECCPLIREX 109 IR=TIF(TPE)	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO COULING L. 0 0 96 QINF(JJ)=QINFL 97 QHR0. 98 QGL=0. C C C D0 I21 LL=1.9 C If(IFFF(KK,LL).EQ.0.AND.GARE(KI 100 IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 101 SHUFSHUF(JJ.LL) 102 TTK=ICIRAD(JJ.LL) 103 ABEAA3(KK,LL) 104 ASEA=ARE(KK,LL) 105 GAREAREGARE(KK,LL) 106 IF(IREF(KK,LL).EQ.0.AND.GARE(KI 107 IRE=IFF(KK,LL) 108 CR=CPIIRE) 109 IR=IIF(TFE) 110 DXI(LL)=XQI(IRE)	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO COULING L. C C 96 GINF(J3)=QINFL 97 QHR0. 98 GGL=0. C C C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL=1.9 C IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 100 IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 101 SHUFSHUF(JJ+LL) 102 TTK=ICIRAD(JJ+LL) 103 AB=AA3(KK+LL) 104 ASEA=ARE(KK+LL) 105 GAREA=GARE(KK+LL) 106 IF(IREF(KK+LL).EQ.0.AND.GARE(KI 107 IF(IREF(KK+LL).EQ.0.AND.GARE(KI 108 CR=CPIIRE) 109 IR=IIF(TFE) 109 IR=IIF(TFE) 110 OXI(LL)=XQ1(IRE)	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO CUULING L. C QINF(J3)=QINFL 97 QHR0. 98 QGL=0. C C 100 IF(IFFF(KK,LL).EQ.0.AND.SARE(KI 100 IF(IFFF(KK,LL).EQ.0.AND.SARE(KI 101 SHGF(JJ.LL) 102 TTK=ICIRAD(JJ.LL) 103 AB=AA3(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(AK,LL) 106 IF(IREF(KK,LL).EQ.0.AND.GARE(KI 107 TREFINERCE KK,LL) 108 CHECCPITRED 109 IRETIF(KK,LL) 109 IRETIF(KK) 110 OXI(LL)=XQ1(IRE) 111 CX2(LL)=XQ2(IRE) 112 OYI(LL)=YQ1(IRE)	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO COULING L. C C 96 GINF(J3)=QINFL 97 QHR0. 98 GGL=0. C C C LOUP OF WALL ORIENTATIONS STAR 99 DO 121 LL=1.9 C IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 100 IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 101 SHUFSHUF(JJ+LL) 102 TTK=ICIRAD(JJ+LL) 103 AB=AA3(KK+LL) 104 ASEA=ARE(KK+LL) 105 GAREA=GARE(KK+LL) 106 IF(IREF(KK+LL).EQ.0.AND.GARE(KI 107 IF(IREF(KK+LL).EQ.0.AND.GARE(KI 108 CR=CPIIRE) 109 IR=IIF(TFE) 109 IR=IIF(TFE) 110 OXI(LL)=XQ1(IRE)	0AD TS FROM HERF K,Ll).20.0.) 60 TO 20
C PART OF HEAT GAIN TO CUULING L. C GINF(JJ)=QINFL 97 QHR0. 98 QGL=0. C C 100 IF(IFF(KK,LL).EQ.0.AND.SARE(K)) 101 SH0*SH0F(JJ.LL) 102 TFK=TCIRAD(JJ.LL) 103 AB=AA3(KK,LL) 104 ASEA=ARE(KK,LL) 105 GAREARE(KK,LL) 106 IF(IREF(KK,LL).EQ.0.AND.GARE(K)) 107 IF(IREF(KK,LL).EQ.0.AND.GARE(K)) 108 CARCEPIRES 109 IRETIF(IREF(KK,LL).EQ.0.AND.GARE(K)) 104 ASEA=ARE(KK,LL) 105 GAREAREGKK,LL) 106 IF(IREF(KK,LL).EQ.0.AND.GARE(K)) 107 IRETIF(IREF(KK,LL).EQ.0.AND.GARE(K)) 108 CARCEPTIRES 109 IRETIF(IFE) 110 OXI(L)=XQI(IRE) 111 GXI(L)=XQI(IRE) 113 OY2(LL)=YQZ(IRE)	ОАО TS FROM HERF K,LL).EQ.Q.) GU TO 20 K,LL).GT.Q.) GD TO 15
C PART OF HEAT GAIN TO COULING L. C GINF(J3)=QINFL 97 QHR0. 98 GGL=0. C C 100 IF(IFF(KK,LL).EQ.0.AND.GARE(KI)) 101 SHOF(JJ+LL) 102 TTK=ICIRAD(JJ+LL) 103 ABRA3(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL) 107 IRC=IAE(KK,LL) 108 CAPCAISE 109 IREIF(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL) 107 IRC=IAE(KK,LL) 108 CAPCAILES 109 IREIF(IKE) 110 OXI(LL)=XQ1(IRE) 111 GXI(LL)=XQ2(IRE) 112 OYI(LL)=YQ1(IRE) 113 OY2LLL)=YQ2(IRE) 114 15 CALL GLASS(I53,SHG,TC, TR,QGL)	ДАД TS FROM HERF K,LL).EQ.Q.) 60 TO 20 K,LL).GT.Q.) 60 TO 15
C PART OF HEAT GAIN TO COULING L. C QINF(J3)=QINFL 97 QHR0. 98 QGLEO. C C 100 IF(IFFF(KK,LL).EQ.O.AND.GARE(KI) 101 SHORE(JJ.LL) 102 TTK=ICIRAD(JJ.LL) 103 ABEAA3(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL).EQ.O.AND.GARE(KI) 107 TK=ICIRAD(JJ.LL) 108 CBRE(KK,LL) 109 IRETIF(IKE) 100 IF(IREF(KK,LL).EQ.O.AND.GARE(KI) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL).EQ.O.AND.GARE(KI) 107 IRE TAREARE (KK,LL) 108 CRECPIERE) 109 IRETIF(TKE) 110 OXI(LL)=XQI(IRE) 111 OXI(LL)=XQI(IRE) 112 OYI(LL)=YQI(IRE) 113 OYI(LL)=YQI(I	ДАД TS FROM HERF K,LL).EQ.Q.) 60 TO 20 K,LL).GT.Q.) 60 TO 15
C PART OF HEAT GAIN TO COULING L. C GINF(J3)=QINFL 97 QHR0. 98 QGL=0. C C 100 IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 101 SHGF(JJ).LL 102 TTK=ICIRAD(JJ.LL) 103 CBARAG(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL).EQ.0.AND.GARE(KI 107 TTK=ICIRAD(JJ.LL) 108 CBARE(KK,LL) 109 IRETIF(IREF(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL) 107 IRETIF(IKK,LL) 108 CH=CP(IRE) 109 IRETIF(IKE) 110 OX1(LL)=XQ1(IRE) 111 QX2(LL)=XQ2(IRE) 112 QY1(LL)=YQ1(IRE) 113 QY2(ILL)=XQ2(IRE) 114 15 CALL GLASS(I53.SHG, TC, TR-QGLING) 114 CDIASS HAS NO Q 115 CA	ДАД TS FROM HERF K,LL).EQ.Q.) 60 TO 20 K,LL).GT.Q.) 60 TO 15
C PART OF HEAT GAIN TO COULING L. C GINF(J3)=QINFL 97 QHRO. 98 QGLEO. C C 100 IF(IFFF(KK,LL).EQ.O.AND.GARE(KI 101 SHOF(JJ)LL 102 IF(IFFF(KK,LL).EQ.O.AND.GARE(KI 103 C 104 ASEAA3(KK,LL) 105 GARE(KK,LL) 106 IF(IFFF(KK,LL).EQ.O.AND.GARE(KI 107 TK=ICIRAD(JJ+LL) 108 CBARE(KK,LL) 104 ASEAA3(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL).EQ.O.AND.GARE(KI 105 GARE(KK,LL) 106 IF(IREF(KK,LL) 107 IREFIELF(KK,LL) 108 CHECPIENE 109 IREFIELF(KK,LL) 108 CHECPIENE 110 OX2(LL)=XQ2(IRE) 111 OX2(LL)=XQ2(IRE) 112 OY1(LL)=YQ1(IRE) 113 OY2(LL)=YQ2(IRE) 114 15 CALL GAIN DUL TO GL	ДАД TS FROM HERF K,LL).EQ.Q.) 60 TO 20 K,LL).GT.Q.) 60 TO 15
C PART OF HEAT GAIN TO COULING L. C GINF(J3)=QINFL 97 QHR0. 98 QGL=0. C C 100 IF(IFFF(KK,LL).EQ.0.AND.GARE(KI 101 SHGF(JJ).LL 102 TTK=ICIRAD(JJ.LL) 103 CBARAG(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL).EQ.0.AND.GARE(KI 107 TTK=ICIRAD(JJ.LL) 108 CBARE(KK,LL) 109 IRETIF(IREF(KK,LL) 104 ASEA=ARE(KK,LL) 105 GARE(KK,LL) 106 IF(IREF(KK,LL) 107 IRETIF(IKK,LL) 108 CH=CP(IRE) 109 IRETIF(IKE) 110 OX1(LL)=XQ1(IRE) 111 QX2(LL)=XQ2(IRE) 112 QY1(LL)=YQ1(IRE) 113 QY2(ILL)=XQ2(IRE) 114 15 CALL GLASS(I53.SHG, TC, TR-QGLING) 114 CDIASS HAS NO Q 115 CA	ДАД TS FROM HERF K,LL).EQ.Q.) 60 TO 20 K,LL).GT.Q.) 60 TO 15

118		QGL≠QGL+CG(JJ,tL)
119		1F(LL. C.9) GQ(JJ)≠QGL
120		IF(1xFF(KK,(L).EQ.0) GG TO 21
121	k 7	GU 122 1=1.1R
122		ARKX*FK(IRE,I)
123		RFX ()= RFRX
124		PRK V=PY(IRE,I)
125		
125		
127 128	1 7 7	TS(I)=TTT CONTINUE
129	122	GO TU 117
130	20	QG(JJ+LL)=U.
131	L V	000 dJJ.LLJ=0.
132	21	QQml JJyll}=O.
134		TTSEJJ.LL)=0.
134		QDS((L1)=0.
135		GO TO 121
	C .	
136		CALL GAR(FO, REX, FEY, TR, TO, TS, ODS(L), 28, TTR, OX1(LL),
		HQXZ(LL)+DY1(LL)+QY2(LL)+IR+CK) WQC IS THE CONVECTIVE PART OF HEAT GAIN THROUGH
	ç	WALL LA FOOF
	ί C	NACE OF FOUR NOR 15 THE RADIATIVE PART OF HEAT GAIN THROUGH
	C C	WALL CR RUOF
	C	HALL LA ROOT
137	•	TTS(JJ,LL)=TS(1)
130		PO 112 1=1,1K
139		TD(LL,1)=TS(I)
140	114	CONTINUE
141		QQw(JJ,EL)≃QQS(EL)
142		UW=QW+QDS(LL)*AREA
145		NJ(JJ)≠UN
144		₩ÚK (JJ)×U×O*WÚJJ3)
142		wQC(JJ)=0.4*WQ(JJ)
140		CONTINUE
	C	
	ŕ	OTOTAL DENOTES THE TOTAL HEAT GAIN
	C C	OTOTAL DENOTES THE TOTAL HEAT GAIN OTOTA DENOTES THE TOTAL RADIATIVE HEAT GAIN
	C C	OTUTAL OFNOTES THE TOTAL HEAT GAIN QTUTE DENOTES THE TOTAL RADIATIVE HEAT GAIN QTUTE DENDTES THE TOTAL CONVECTIVE HEAT GAIN
		QTUTE DENOTES THE TOTAL RALIATIVE HEAT GAIN OTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN
147	с С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTETAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QENF(JJ)+GQ(JJ)+WQ(JJ)
147 148	с С	QTOTE DENOTES THE TOTAL RADIATIVE HEAT GAIN OTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTETAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QENF(JJ)+GQ(JJ)+WQ(JJ) UTETF(JJ)=QPF(JJ)+QER(JJ)+ GQ(JJ)+WQR(JJ)
148 149	с С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTETAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QENF(JJ)+GQ(JJ)+WQ(JJ) QTETE(JJ)=QPF(JJ)+DER(JJ)+GQ(JJ)+WQR(JJ) QTETE(JJ)=QPC(JJ)+DEC(JJ)+QAIR(JJ)+QTEF(JJ)+WQC(JJ)
148 149 153	с С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) UTOTE(JJ)=QPF(JJ)+QER(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QHFAT=QTOTE(JJ)
148 149 151 151	с С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QP(JJ)+QEC(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QHFAT=QTOTE(JJ) MM=MM+1
148 149 150 151 152	с С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTIVTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QPF(JJ)+QER(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QHFAT=QTOTR(JJ) MM=MM+1 QQTOT(MM)=QHEAT
148 149 151 151 152 153	5 6 6	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTHTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QPF(JJ)+QLE(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QHFAT=QTOTE(JJ) MM=MM+1 QQTOT(MM)=QHEAT QCUNV(MM)=QTOTE(JJ)
148 149 151 151 152 153 154	5 6 6	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTIVEAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) UTITE(JJ)=QPE(JJ)+QLE(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPE(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPE(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPE(JJ) MM=MM+1 QCJNV(MM)=QTEAT QCJNV(MM)=QTEC(JJ) CONTINUE
148 149 151 151 152 153	c C 105	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTHTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QPF(JJ)+QLE(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QHFAT=QTOTE(JJ) MM=MM+1 QQTOT(MM)=QHEAT QCUNV(MM)=QTOTE(JJ)
148 149 151 151 152 153 154	5 6 6	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QP(JJ)+DER(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+UEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(MM)=QHFAT QCUNVIMM)=QTOTE(JJ) CONTINUE IF(II)-LT.NDAY) GO TO 106 DO 32 L=1+20
148 149 151 151 152 153 154 155	c C 105	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) OTOTE(JJ)=QPC(JJ)+QEC(JJ)+QG(JJ)+WQR(JJ) OTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QEIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QEIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QEIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+QEC(JJ)+QEIR(JJ)+QINF(JJ)+WQC(JJ) QCUNV(MM)=QFAT QCUNV(MM)=QTOTE(JJ) CONTINUE IFLII-LT-NDAY) GO TO 106
148 149 151 151 152 153 154 155	c C 105	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) UTOTE(JJ)=QP(JJ)+QLE(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) MM=MM+1 QTOTE(MM)=QHEAT QCUNV(MM)=QTOTE(JJ) CONTINUE IFLII.LT.NDAY) GO TO 106 DO 32 L=1,20 IFLKK.tQ.2.0K.KK.EQ.3.DR.KK.EQ.9) GO TO 31 WIL = WT(3.L)
148 149 151 151 152 153 154 155 156 157 158 159	c C 105 C	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTHTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+QINF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) MM=MM+1 QQTOT(MM)=QHEAT QCUNV(MM)=QTOTE(JJ) CONTINUE IFLII.LT.NDAY) GD TO 106 DO 32 L=1+20 IFLK.+Q.2-OR.KK.EQ.3-DR.KK.EQ.9) GO TO 31 HILJ=WT(3-L) GO TO 32
148 149 151 152 153 154 155 156 157 159 159	с С 105 С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTHTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+GQ(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(JJ)=QPC(JJ)+ULC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTOTE(MM)=QHEAT QCUNV(M
148 149 151 152 153 154 155 155 155 159 161	с С 105 С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTUTE(JJ)=QP(JJ)+QE(JJ)+QG(JJ)+WQR(JJ) QTUT(JJ)=QPC(JJ)+QEC(JJ)+QAIR(JJ)+WQC(JJ) WHEAT=QTOTE(JJ) WHEAT=QTOTE(JJ) MM=MM+1 QCJUV(MM)=QTETC(JJ) CONTINUE IF(II.LT.NDAY) GD TO 106 DO 32 L=1+20 IF(KK.+Q.2.CM.KK+EQ-3.DR.KK+EQ-9) GO TO 31 W(L)=wT(3.L) GD TD 32 ALL=FT(4.L) CONTINUE
148 149 151 152 153 154 155 156 157 159 161 161	с С 105 С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QP(JJ)+DER(JJ)+GO(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+UEC(JJ)+QAIR(JJ)+WQC(JJ) WHEAT=QTOTR(JJ) MH=MH+1 QCJOT(MM)=QHEAT QCJNV(MM)=QTOTC(JJ) CONTINUE IF(II.LT.NDAY) GD TO 106 DO 32 L=1+20 IF(KK.+Q.2.CK.KK.E0.3.DR.KK.EQ.9) GD TO 31 H(L)=NT(3.L) GD TO 32 A(L)=NT(4.L) CONTINUE DO 108 NL=25.48
148 149 151 152 153 154 155 156 157 159 161 162 163	с С 105 С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+WQR(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+WQR(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QLE(JJ)+QAIR(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QLE(JJ)+QLE(JJ)+QTNF(JJ)+WQC(JJ) QTOTE(JJ)=QP(JJ)+QLE(JJ)+QL
148 149 151 152 153 154 155 156 157 159 161 161	c C C J1 32	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTOTE(JJ)=QP(JJ)+DER(JJ)+GO(JJ)+WQR(JJ) QTOTE(JJ)=QPC(JJ)+UEC(JJ)+QAIR(JJ)+WQC(JJ) WHEAT=QTOTR(JJ) MH=MH+1 QCJOT(MM)=QHEAT QCJNV(MM)=QTOTC(JJ) CONTINUE IF(II.LT.NDAY) GD TO 106 DO 32 L=1+20 IF(KK.+Q.2.CK.KK.E0.3.DR.KK.EQ.9) GD TO 31 H(L)=NT(3.L) GD TO 32 A(L)=NT(4.L) CONTINUE DO 108 NL=25.48
148 149 151 152 153 154 155 156 157 159 161 162 163	с С С С 31 32 С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTMEAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+QQ(JJ)+QD(JJ)+QD(JJ)+QQ(JJ)+Q
148 149 151 152 153 154 155 155 157 159 161 165 165 165 165 165	c C C J1 32	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTDTE DENOTES THE TOTAL CONVECTIVE HEAT GAIN UTOTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTDTE(JJ)=QP(JJ)+QLE(JJ)+QAIR(JJ)+QR(JJ) QTDTE(JJ)=QPC(JJ)+QLC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QHFAT=QTOTE(JJ) MM= MM+1 QCJOT(MM)=QHFAT QCJNV(MM)=QTDTC(JJ) CONTINUE IF(II.LT.NDAY) GD TO 106 DO 32 L=1.20 IF(KK.QL2.QK.KK.EQ.3.DR.KK.EQ.9) GO TO 31 W(L)=WT(3.L) GO TO 32 A(L)=WT(4.L) CONTINUE DO 108 NL=25.48 QQL=0. NNN=NN+1 CALCULATION OF CUBLING LOAD GIVEN BY EQ.14-5)
148 149 151 152 153 154 155 155 157 159 161 165 165 165 165	с С С С 31 32 С	QTOTE DENOTES THE TOTAL RALIATIVE HEAT GAIN QTUTE DENOTES THE TOTAL CUNVECTIVE HEAT GAIN UTMEAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+QQ(JJ)+QD(JJ)+QD(JJ)+QQ(JJ)+Q
$ \begin{array}{r} 148 \\ 149 \\ 151 \\ 152 \\ 152 \\ 153 \\ 154 \\ 155 \\ 156 \\ 157 \\ 161 \\ 164 \\ 165 \\ 16$	с С С С З 105 С З 2 С С С С С	QTDTR DENDTES THE TOTAL RALIATIVE HEAT GAIN QTDTR DENDTES THE TOTAL CONVECTIVE HEAT GAIN UTMTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTDTF(JJ)=QP(JJ)+QIR(JJ)+QAIR(JJ)+WQR(JJ) QTDTC(JJ)=QPC(JJ)+QAIR(JJ)+QAIR(JJ)+WQC(JJ) QTDTC(JJ)=QPC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QTDT(MM)=QHFAT QCJNV(MM)=QHFAT QCJNV(MM)=QTDTC(JJ) CONTINUE IF(II.LT.NDAY) GD TO 106 DO 32 L=1+20 IF(KK.+Q.2.OK.KK+EQ.3.DR.KK+EQ.9) GD TO 31 H(L)=WT(3.L) GD TD 32 A(L)=NT(4.L) CJNTINUE DO 108 NL=25.48 QQL=0. NNN=NN+1 CALCULATION OF CUDLING LOAD GIVEN BY EQ.14-5) DD 107 M=1+15 QUL=QL+*(N)=QTOT(NNN-M)
148 149 151 152 153 154 155 155 157 159 161 165 165 165 165	с С С С З 105 С З 2 С С С С С	QTDTR DENDTES THE TOTAL RALIATIVE HEAT GAIN QTDTR DENDTES THE TOTAL CONVECTIVE HEAT GAIN UTMTAL(JJ)=QP(JJ)+QAIR(JJ)+QL(JJ)+Q(NF(JJ)+GQ(JJ)+WQ(JJ) QTDTF(JJ)=QP(JJ)+QLF(JJ)+GQ(JJ)+WQR(JJ) QTDTC(JJ)=QPC(JJ)+QLC(JJ)+QAIR(JJ)+QINF(JJ)+WQC(JJ) QHFAT=QTOTR(JJ) MH= MH+1 QQTJT(MM)=QHFAT QCJNV(MM)=QTDTC(JJ) CONTINUE IFLII.LT.NDAY) GD TO 106 DO 32 L=1.20 IFLKK. Q_L 2.CK.KK.EQ.3.DR.KK.EQ.9) GO TO 31 HLJ=WT(3.L) CONTINUE DO 100 NL=25.48 QQL=0. NNN=NN+1 CALCULATION OF CODLING LUAD GIVEN BY EQ.14-5) DD 107 M=1.15

```
109
         108 CONTINUE
 170
             WRITE (6,1001)
 171
             WRITE (6,998) KK
 172
             WRITE (6+1006)
173
             WRITE(6+1002) (JJ+ITS(JJ+IL),LL=1,91,JJ=1,24)
 174
             WRITE 16,10031
 175
             WRITE (6,1002)
                           {JJ, (QQXEJJ, LL+L, 9}, JJ=1, 24)
175
             WRITE [6,1001]
 177
             WRITE (5,1004)
 170
             WRITE(6,1002)
                           {JJ, (QQG{JJ,LL),LL=1,9},JJ=1,24}
179
             #BITE (6+10051
            WRITE(6,1000) (JJ, QP[JJ), QAIR(JJ), QE(JJ), CINF(JJ), GQ(JJ),
180
            +WQ(JJ),QTOTAL(JJ),QLGAD(JJ+24),JJ=1,24)
181
            WRITE (6.1001)
182
        106 ID0Y=100Y+1
183
        104 CONTINUE
164
        120 CONTINUE
185
        500 FORMAT(2F10.4)
        501 FURMAT(13)
186
187
        502 FORMAT(II)
188
        504 FORM4T(FL0.4)
        507 FORMAT(511, F10.2)
189
190
        508 FDAMAT(6F10.5)
191
        530 FORMAT(9)1)
192
        531 FURMAT(9F6.2)
193
        998 FORMATION ,1X, SPACE NO = 1,14/ }
194
       LUUU FORMAT(1X,15,7F10,1,4X,F10.1)
195
       1001 FORMATLINII
196
       1002 FORMATL1X,15,9F9.3)
197
       1003 FORMATELH-.*HEAT GAIN THROUGH WALLS (BTU/HR#FT##2)*/1
       IUU+ FORMATIIH-,1X, "HEAT GAIN THROUGH GLASS (BTU/HR*FT**2)//)
198
199
       1005 FORMATLIN-, 1X, "HEAT GAIN FROM VARIOUS SUURCESIBTU/HRI //2X,
           + TIME - 5X, * PEOPLE - , 5X, *A IR *, 6X, *LIGHT *, 5X, * INF 1LT. +, 4X,
           + GLASS + 6X, WALL + 5X, TOTAL + 5X, COOLING LOAD / J
       1006 FORMATLING, 1X, "TEMPERATURE OF WALL SURFACE (DEG F)"/)
200
201
            STOP
202
            END
            SUBRUUTINE RESEACTREFREX.REY
203
            DOUBLE PRECISION R(LO), BET4(10), RODT( 100), KK( 100, 3), DT,
204
           *M1, M4 .H1 . H2, W3, BFT4X, BET 6Y, BETAZ, B1, B2, BP3, A, B, C, AA, BB,
           *FA,F8,FC,XX,YY,Z2,XL(10),XK(10),D(10),SH(10),RES(10),
           *K0.K1,CC.X,Y,Z
205
            DIMENSION REX41001.REV41001.REZ41001
      С
            THIS SUBROUTINE CALCULATES RESPONSE FACTORS
206
         10 FORMAT(SF10.5)
207
         11 FORMAT(5010.5)
208
            KARD=5
20.9
            DT=1.0
      С
            C
                        READING DATA
            FNOL IS THE NUMBER OF LAYERS OF A MULTI-COMPONENT WALL
      Ľ.
210
       110 READ(KARD, 10) FNOL
      С
            ************
            M=FNOL+0.1
211
212
            DO 150 I=1.M
            ******************
      C
                        READING DATA
      C
           XL IS THICKNESS OF EACH LAYER
            XK IS THEMAL CONDUCTIVITY OF EACH LAYER
      C
            D IS DENSITY OF EACH LAYER
      C
      C
            SH IS SPECIFIC HEAT OF EACH LAYER
      С
           RES IS RESISTENCE OF FACH LAYER
           READ(KARD,11)XL([),XK([],D([],SH(]),RES([)
213
                      ******************
214
           IF(XL(1)) 130,120,130
```

215	1	20	RIII=RESILI
216	-		8ETA(1)=0.0
-			
217			GO TO 150
218	1	30	R{[]=xL{[]}/xK{[]
219	1	40	BETAILI=XL4()=DSQRT(D(I)=SH(1)/XK(I))
		20	DETAILS ACTIVE SALIDITES ALTERNAL
220	-	-	CUNTINUE
221	1	60	DD 160 [#1.M
222			1FIXLI111 180,170,180
		7.5	
223			RES(1)=0.0
224	1	60	CONTINUE
225			N#100
226			IRODT=0
227			00 190 I=1.N
220			R001(1)=0.0
		. .	
229		AD	CONTINUE
	C		二字字 新式学校 教育 建带带 医黄疸 化合金
	C		
230	•		CALLING A SUB SUBROUTINE
230			CALL ZERDIF, BETA, RES, M, KO, KL, ML, M4)
	Ç		************
231			W1=30.0/DT
232			
			W2=10C.0/DT
233			NN=B
	c		*******
	č		
	5		CALLING A SUB SUBROUTINE
234			CALL FALSE(R. BETA, RES, W1, W2, W3, 31, 82, 8P3, M, NN)
	С		***************************************
375	•		
235			1ROOT=1
236			LAST=1
237			J=Z
•		• •	
236	- 2	uψ] → l = l
239			R00T(J)=W3
240			KK(J+2}=1.0/8P3/W3/W3
241			KK{\$;}1}=KX{J,2}#81
242			KKtJ+3}=KKtJ+2}≠82
243	ز	10	1FILAST-11 220,220,230
-			11 11 11 120 1220 1220 1230
244	۷.		#1=0.001/DT
245			GO TO 240
240			HI=ROOTILAST-11
247	24		H2=ROOT(LAST)
248			M2=42-0-00001/DT
249			w1=w1+U_00001/0T
2.17	-		
	٦.		****************
	C		CALLING A SUB SUBACUTINE
250			CALL SLOPE(R, BETA, KES, W1, W2, M, ICONT, LAST)
	r		
	C.		* *************************************
251			GO TO (250, 310),ICONT
2 5 2	2 5		NN=Q
	۰.		*******
	2		CALLING A SUB SUBROUTINE
253			CALL FALSE (R. BETA, KES, WI, W2, W3, 81, 92, 8P3, M, NN)
	C		\$*************************************
254			DO 270 1=L,IROOT
255			IF(W3-ROCT(1)) 260,260,270
250	2.6		Ja]+1
	~ ~		
257			GU TO 280
258	27	70 1	CONTINUE
2 5 9	2.0	9 C	IRUDT=IRUDT+1
26U			LAST=LAST+1
261			JJ≂IRCOT+1
26Z			IF(1RC)T-N} 290,290,320
	- -		
263	29		DO 300 I×J.IROOT
264			1 → L
265			RDUT(JJJ=ROOT(JJ-1)
200			(K[]],]]=KK(]]-[,])
267		E F	<k(jj+2}=kk(jj-1+2)< td=""></k(jj+2}=kk(jj-1+2)<>
268		N	(K(JJ+3)=KK(JJ+1+3)
2.44			······································

300 CONTINUE 269 60 TO 200 270 313 IF(LAST) 320,320,210 271 320 8ETAX =K1+M4*KQ 272 HE742=K1+M1*K0 273 DO 450 [=1,100 274 A=0.0 275 8=0.0 276 277 C=0+0 J≠1,1900T 046 00 278 IF(RUCT(J)*1=01-30.01 330,330,350 279 260 330 BETAY=DEXP(-ROOT(J)+I+DT) A=A+KK(J+1)*BETAY 281 H=B+KK[J.2]+BETAY 282 283 C=C+KK[J+3]*BETAY 340 CONTINUE 284 350 #=(A+{K1+M4=K0}+DT+I*K0}/0T 285 266 B=18+K0+DT=[+K1)/DT C=[C+(K]+N]*KU]+DT*I*K0)/DT 287 IF(1-2) 360,370,380 288 289 360 AA=A 66=8 290 291 0=00 292 GU TO 390 293 370 AA=4-2.0*X 88=8-2.0*Y 294 CC=C-2.0×Z 295 296 GU TO 390 380 A4=A-2.0+X+FA 297 298 88=8-2.0=Y+FB CC=C-2.0+2+FC 299 Ċ REX 15 RESPONSE FACTORS, X REY IS RESPONSE FACTORS, Y ¢ ί FFZ IS RESPONSE FACTORS, Z ¢ 390 REX(I H=AA 400 3 0 1 REYLLIABB 302 PFZ(1)=CC 1F(I-2) 430,430,400 303 400 JF(DABS(XX/FAA-AA/XX)-0.00001) 410,410,430 304 410 1F(DA85(YY/F88-88/YY)-0.000011 420,420,430 305 420 IF(DABS(22/FCC-CC/22)-0.00001+ 46C,46C,430 306 430 IF(DAES(AA)-0.0000001) 460.460.440 307 300 440 FA=X FB=Y 309 FC=Z 310 FAA=XX 116 312 X X= A A 313 £BB≃ΥΥ FCC=ZZ 314 315 ¥¥=88 12=00 316 X=A 317 318 Y≃B 319 Z = C 450 CONTINUE 320 460 R1=DEXP(-DT+ROOT(1)) 321 322 RETURN END 323 324 SUBROUTINE SLOPE(R, BETA, RES, W1, W2, M, ICONT, LAST) 325 DOUBLE PRECISION R(10), BETA(10), N1, W2, N3, BP1, BP3, #FF(2,2),F12,2),RES(10) THIS SUBPOLTING CALCULATES THE SIGN OF THE DERIVATIVE С C OF THE FUNCTION GIVEN BY D/DS#81SN1 1C=0 326

327 J=L 0ELTA= (W2 - W1) / 20.0 328 329 #3=#1+J*CELTA ************* C ¢ CALLING & SUB SUBROUTINE 330 CALL OBRIR.BETA.RES.WI.M.F.FF) ******* Ľ, *** ** ***************** 331 81-FF(1,2) 332 8P1=+ (1,2) £ *** ********************* CALLING & SUB SUBREUTINE C 100 CALL DERIRABLTA RESAWS - M.F. FF1 333 C 334 83=FF(1.2) 335 BP3=F11+21 [F(81) 110.110.120 110 [F(83) 130.130.210 330 337 338 120 18(83) 210,210,130 339 130 1F(BP1) 140,140,150 146 1F(8P3) 170,170,160 340 341 150 1F(BP3) 160,160,170 346 160 10=10+1 343 170 1F(10-2) 180,210,210 344 180 J=J+1 345 IF1J-201 190,190,200 346 190 81=83 347 8P1=8P3 346 W3*W1+J#DELTA 349 GO TO 100 35U 200 ICUNT=2 351 LAST+LAST-1 352 RETURN 353 210 1CONT#1 354 #2=#5 355 RETURN 356 END 357 SUBROUTINE FALSE(P.BFTA.HES.WI.W2.W3.BL,B2.BP3.M.N) DOUBLE PRECISION & (10) . HET4(10) . F(2.2) . FF(2.2) . W1. 356 *W2+W3+81+82+83+8P3+4+6+C+FA+F8+FC+RES(10) C THIS SUBFOUTINE CALCULATES ROOTS, SN. GIVEN IN C EQUATION 12-281 C 359 10 FURMATCITH NO ROOT IN FALSER 360 KAG11=6 100 IFINE 100.100.110 362 100 N=1 161 110 1+1 364 893=w1 £. *** ****** ********* C CALLING & SUB SUBROUTINE 305 CALL MATRIX(F, HETA, RLS, W1, P,F) ί ******* ********* ** ******** 366 81×F11,21 367 82=81 120 DELTA=1#2-#11/N/20.0 368 969 130 H3=W1+J+UELTA 370 IFE#3-#21 160,160,140 371 140 N=N+1 \$72 BP3=#1 373 82+81 374 1F(N-251 150,150,300 315 150 3+1 376 GO TU 120 ******* ************* C CALLING A SUB SUBROUTINE

377		160	CALL MATRIXIA,BETA,RES,W3,M,F)
	C		*******
378			B 3≠F(1,2)
379			1F(B1) 170,170,180
380			1F(B3) 190,190,200
381		-	1F(83) 200+200,190
382 383		190	J=J+1 82≂83
384			8235
385			GO TO 130
380		200	£=8P3
387			8=#3
388			FA≂ BZ
783			F8=83
390	-	210	(=(A+B)/?。) ★##### ###############################
	ç		CALLING A SUB SUBROUTINE
201	С		CALLING A SUB SUGNOUTINE CALL MATKIX(R.SETA.RES.C.M.F)
391	Ċ.		· · · · · · · · · · · · · · · · · · ·
392			FC=F(1,2)
393			1F(FC) 220,290,250
394		220	IF(FA) 230,230,240
395		230	FA=FC
396			A=C
397			GU TO 280
398		240	F∂=FC B≃C
399 400			GO TO 280
400		250	1F(FA) 260,260,270
402		-	FB=FC
403		•	B=C
404			GD TD 280
÷05		270	FA≖FC
400			A=C
407	~	280	1F(DABS(4-8)-1。0D-14) 290。290。210 ************************************
	C C		CALLING A SUB SUBROUTINE
4.08			
		290	
	c	290	
409		290	CALL DERIR, BETA, RES, C.M., F.FF)
409 410		290	CALL DERIR,BETA,RES,C,M,F,FF) ★₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩₩
410 411		290	CALL DER(R, BETA, RES, C, M, F, FF) ***********************************
410 411 412		290	CALL DER(R, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413			CALL DER(R, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414			CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 414			CALL DER(R, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414			CALL DERIR, BETA, RES, C.M., F.F.F.) ********************************
410 411 412 413 414 414			CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 415		300	CALL DER(R, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 416 417	C	300	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 416 417	c	300E	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 416 417	c c c	300E	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 416 417 415	c	300E	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 416 417 418 419	c c c	300E	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 416 417 415	c c c	300E	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 +11 412 +13 414 415 +16 417 +19 420 421 422	c c c	300	CALL DER(R, BETA, RES, C, M, F, FF) ***********************************
410 411 412 413 414 415 416 417 419 420 421 422 423	c c c	300	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 +11 412 +13 414 415 +16 417 +18 419 420 421 422 423 424	c c c	300	CALL DER(R, BETA, RES, C, M, F, FF) ***********************************
410 +11 412 413 414 415 416 417 418 419 420 421 422 422 422 424 425	c c c	300	CALL DERIR.BETA.RES.C.M.F.FF) ***********************************
410 +11 412 413 414 415 416 417 418 419 420 421 422 423 425 425 425	c c c	300	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 +11 412 413 414 415 416 417 416 417 419 420 421 422 423 425 425 425 425 427	c c c	300	CALL DERIR.BETA.RES.C.M.F.FF) ***********************************
410 +11 412 413 414 415 416 417 418 419 420 421 422 423 425 425 425	c c c	300	CALL DERIR, BETA, RES, C, M, F, FF) ***********************************
410 +11 412 413 414 415 416 417 416 417 418 419 420 421 422 423 425 425 425 427 428	c c c	300	CALL DER(R, BETA, RES, C, M, F, FF) ***********************************

431	120 (FURES(1)) 130,140,130
432	130 TEMP=1.0/(F1(1,2)+RES(1)) F1(2,1)=(F1(2,1)*FIS(1)+2-0*F1(1,1)-2-0)*TEMP
433	f1(1,1)=(F1(1,1)*HES(1)+F1(1,2))*TEMP
434 435	$F_1(2,2) = F_1(1,1)$
435	f1[1,2]=F1[1,2]FRESI11*TEMP
437	140 IF(4-1) 170,150,170 150 DD - 160 - L=1+2
438 439	150 CO 160 L=1+2 00 Le0 LL≤1+2
44J	F(L,LL)=F1(L,LL)
441	160 CONTINUE
442	G10 T13 270 170 D0 260 J¥2∎M
44\$ 444	P≏DSQKT(W]≮BLT4(J)
445	F=R(J)
440	1F(P) 190+180+190
447 448	190 F2(1,1)=1.0 F2(1,2)=P
449	F2(2,1)≠0.0
420	F2(2+2)=1=0
45L	GO ¥A 200 190 F2(1+1)=0COSIPI
452 453	F2[1,2]=+R/P=DSIN(P)
454	F2(2,1) = -P/R+OSIN(P)
455	F2(2,2)=0COS(P)
455 457	200 [F[ReS(J]] 210+220+210 210 TEMP=1+0/(#2(1+2)+FES(J])
456	£2(2,1)=(F2(2+1)*FLS(J)+2.J*F2(1,1)-2.0)FTEMP
459	F2(1,1)=(F2(1,1)=?F\$(J)+F2(1,2))=TEMP
460	# 2(2,2)≥F=F2(1,1) # 2(1,2)≤F2(1,2)#RFS(J)#TEMP
461 462	220 D0 230 Lal,2
463	00 230 LL=1,2
404	r(1,L1)20.0
465	230 CONTINUE DD 240 L=1,2
460 467	PD 240 LL=1,2
460	00 240 LEL=1.2
469	F (L,LL) #F (L,LL) +F 1 (L,LLL) +F2(LLL+LL)
470 471	240 LUNTINUE DO 250 L=1+2
472	DD 250 LL=1,2
473	Fl(LyLL)=F(LyLL)
474 475	250 CUNTINUE 260 CUNTINUE
470	270 NETURN
477	END
478	SUBPOUTIVE DER (RR.BETA, RES, W.M.F.FF)
479	LOUBLE PRECISION RK(10), BETA(10), FL(10, 2, 2),
	#F (2,2), FF (2,2), P, R, ALPHA, SQ, W, RES(10), TEMP, TEMP1,
	=+2(10,2,21,F3(10,2,2)
	C THIS SUBFOUTINE CALCULATES THE DERIVATIVE OF THE
	C FUNCTIONS GIVEN IN EDS. (2-33) TO (2-35)
400	JU 143 I=1,M
401	₽ ={\\$Q\$T[w]#BETA{]} ₽ ={ {{]}}
462 483	K=r<11 K=r<11
484	SQ=03C=T(w)
485	IF(P) 110,100,110
485	100 F1(1,1,1)=1.0
₩87 ₩88	F1([+2+2)=F F1([+2+1)=J=Ŭ
400 487	f(1,2,2) = 1.0
470	F2(I,1,1)=0.0

491	F2(1,1,2)=0.0
492	F 24 I , 2, 1 J = 0 . 0
+93	GO TÊ 120
494	110 F1(I+I+I)=DCCS[P]
495	$f(1, 1, 2) = n/P \approx DSIN(P)$
490	F1(1,2,1)=-P/F-DSIN(P)
497	$F_1(1, 2, 2) = OC(S(4))$
498	F 7(1,1,1) =+ AL P+ A* DS1.(ALPHA*S0)/2.0/S0
499	F2(1,1,2)=-R*JCUS(ALPHA*SQ)/2.U/A+P*DSIN(ALPHA*SJ)/
	*(LPHA/2.0/SQ/SQ/SQ
500	F 2(1, 2, 1) =+ ALPHA= 4LPHA= DCDS(ALPHA+Sq)/2.0/R+
200	=15141 AL PH/ = 501/2=0/50*AL PHA/R
501	120 F2(I+2+2)=F2(I+1+1)
502	[F(RES(1)) 130,140,130
503	130 1 EMP=1.0/(F1(1,1,2)+5ES(1))
ົ້ນບໍ່ຈ	F1(1,2,1)=(F1(1,2,1)*RES([)+2.0*F1([,1,1)+2.0)*TEMP
505	F1(1,1,1)=(F1(1,1,1)*RES(1)+F1(1,1,2)]*TEMP
506	F1(I,2,2)=F1(I,1,1)
507	F1(I,1,2)=F1(1,1,2)*F5S(I)*TEMP
508	TEMP1=F2(1,1,2)*TEMP
509	F2(1,2,1)=(F2(1,2,1)*RES(1)+2.0*F2(),1,1)*TEMP-
	<pre>#F1(1,2,1)*TEMPL</pre>
51J	F2(1,1,1)=(F2(1,1,1)*RES(1)+F2(1,1,2))+T0PP-F1(1,1,1)*
	*IEMP1
511	$F_2(1,2,2) = F_2(1,1,1)$
512	F2(1,1,2)=F2(1,1,2)++ES(1)=TEMP-F1(1,1,2)+TEMPE
513	140 CONTINUE
514	1F(M-1) 170,150,170
515	150 D(1 160 K=1,2
510	00 160 L=1+2
517	F(K+L]=F2{1,K,L}
518	FF(K+L)=F1(1+K+L)
519	160 CONTINUE
520	GO TO 330
521	170 DO 180 K=1,2
522	DO 18J L≖1,2
523	F(K+L)=0.0
524	160 CONTINUE
525	00 280 I=1,M
526	00 2c0 J=1,4
527	DO 210 K=1,2
528 529	00 210 L=1,2 IF(I-J) 190,200,190
530	190 F3(J+K+L)=F1{J+K+L}
531	GO TO 210
532	200 F3(J+*+L1=F2(J+K+L)
533	210 CONTINUE
534	IF(J-1) 220,260,220
535	220 DO 230 K=1,2
530	DO 230 L=1,2
537	FF(K,L)=0.0
538	230 CONTINUE
539	DO 240 K=1,2
540	DD 240 L=1,2
541	DO 240 N=1+2
542	FF(K,L}=FF(K,L}+F3(J-l,K,NJ*F3(J,N,L)
543	240 CUNTINUE
544	DO 250 K=1+2
542	DD 250 t=1.2
546	F3(J,K,L)=FF{K,L}
541	250 CONTINUE
548	260 CÚNTINUE
549	00 270 K=1,2
550 451	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
551 561	£{K,(};=FF{{K,(}}+F{K,L}) 270 €ONT1NUE
552	270 CONTINUE

553	280	CONTINUE
554		00 320 1≖2,M
555		DO 290 K=1+2
556		00 290 L=1+2
>57		FF(K,L)=0.0
558	290	CONTINUE
\$59		DO 300 K=1,2
99C		00 300 L=1+2
561		00 30J N=1,2
562		FF(K,L)=FF(K,L)+FL(I-1,K,N)*F1(1,N,L)
563	300	CONTINUE
364 565		00 310 K=1+2 00 310 L=1+2
565		DO 310 L=1+2 Fl{I,K,L}=Ff(K,L}
567	210	CONTINUE
500		
569		RETURN
570		ÉND
571		SUBROUTINE ZERD(RA, BITA, RES, M.KO, K1, M1, M4]
572		DOUBLE PRECISION ARLIUL, BETALIOLA, B, C, D, AA, BB, CC, DD,
		#F4+M1;M2+M3;M4+K0+K1;P;R;kES{10};F1;F2;F3
	C	THIS SUBFOUTINE CALCULATES THE VALUES OF DERIVATIVE IN
	C	EQUATIONS (2-33) TO (2-35) AT POLE S=0
573		KU=0.0
574		DO 120 I=1,M
575		1FIRES([)] 110,100,110
576 577	100	KO≠KU+RK(1) GD T0 120
578	110	- KU=KJ+PR([]+RES(])/(PR(]]+RES(]))
579		CONTINUE
580		KO=1.0/KO
581		N1=0_0
582		N2=0.0
583		M3=0.0
584		M4=0.0
585		00 260 I≖I.M
586		P=BET/(LI*BETA(1)
587		R≤RR(})
588		[F(I-1) 130+150+130
584	130	A=1.0
590		8 = R
591		
592 593		D=1.0
594	1.4.1	IF(RES(1)) 140,190,140 B≠R≠RES(1))/[P+RES(1)]
545	140	60 TO 190
596	150	A*+P/2.0
597		8++R+P/6+0
598		C++P/R
599		D=+P/2.0
600		IF(RES(1)) 160,170,160
601	160	A=RES(11*P/2.0/(R+RES(1))
602		B={1.0-R/(F+FES{1})}#RES(1)#R#P/6.0/(R+RES(1))
603		C=(RES(1)=P/R +1.0+P)/(R+RES(1))
604		
605		1F(M-1) 190,180,190
606	190	
507		K1=-K0*B
609 609		M4=D GD TO 270
61U	190	DO 250 J=2.M
611	170	P=BETA(J)+BETA(J)
612		R=RR[]]
013		1F(I-J) 200.220.200
614	200	AA=1.0

615 88=R 616 CC=0.0 617 00=1.0 IF(RES(J)) 210,240,210 618 210 B8=R*R35(J)/(R*RES(J)) 619 6 ZU GO TO 240 220 4A=+P/2.0 021 88= +P =R /6 .0 622 CC=+P/R 623 024 0D=+P/2.0 1F(RES(J)) 230,240,230 625 230 AA=RES(J)*P/2.0/18+RES(J) } 626 BB=(1.U-K/(R+RESIJ)))*RES(J)*R*P/6.0/(R+RESIJ)) 6Z7 CC=(RE3(JJ=P/R +1.0"P)/(R+RES(J)) 67d DD=AA 629 υŁο 24J F]=A=AA+B=CC F2=4*83+8*00 031 F3=C#AA+D#CC 632 F4=C=86+0400 o 33 634 A=F1 8=F2 635 C = F 3 636 637 0=F4 250 CONTINUE o3a M1=M1+F1 039 64Ú M2=M2+F2 M3=M3+F3 641 M4=M4+F4 642 643 260 CONTINUE 644 K1=-K0+K0+M2 270 RETURN 642 END 546 SUBROUTINE SUNLIDEY, SHGF, TOTRADI 647 DIMENSION AN191, AM(9) 648 649 DIMENSION ALPHA161, TAUL61, AZIM181 650 DIMENSION IDTRAD(24,9), SHGF(24,9) ٤ THIS SUBROUTING CALCULATES THE DIRECT, DIFFUSE AND TOTAL ¢ C SULAR RADIATION, AND THE SOLAR HEAT GAIN FACTORS AT ANY TIME OF YEAR AND LOCATION С 100Y IS THE TIME OF YEAR ĉ Ç SHGE IS THE SULAR HEAT GAIN FACTORS TOTRAD IS THE TOTAL SULAR PADIATION С L 651 508 FORMAT(6F10.4) 510 FORMAT (8F10.4) 652 С ALPHA IS ABSORPTANCE OF THE DOUBLE-STRENGTH GLASS TAU IS TRANSMITTANCE OF DJUBLE-STRENGTH GLASS С C C AZIM IS WALL AZIMUTH ANGLE 653 xEAD(5,508)(ALPH4(3), J=1.6) 654 RE40(5,508) (TAU(J),J=1,6) 655 READ(5,510)(4ZIM(J), J=1,8) SHG4 = 0.0 650 657 5HGT=0=0 00 7 J=1,6 4 J=J -1 658 659 SH=TAU(J)/(AJ+2.) 560 661 SHGT=SHGT+SH SHA=ALPHA(J)/(AJ+2.) ō62 7 SHGA=SHGA+SHA 663 064 00 30 J=1,24 665 00 31 K=1,9 TOTRADLJ.KJ = 0. 666 667 31 SHGE(J+K) =0.

668		30	CONTINUE
	۲ ۲		R IS GROUND REFLECTIVITY
66Y			R=0.2
	C C		CL IS THE NORTH LATIFUDE IN RADIANS
67J			CL = 21.25+3.1415926/180.
	C C		IDOY INDICATES THE DAY OF A YEAR
671			C1=C05(.01721*(D0Y)
672 673			S1=SIN(.U1721*100Y) C2=C1+C1-S1*S1
074			\$2=2.*\$1*Ci
675 676			C3=C1+C2+S1+S2 S3=C1+S2+S1+C2
010	с		33-61 36.31.62
	C		DEL 15 CECLINATION ANGLE IN RADINAS DEL = .005274001=01003990=02004240*03+.0672*SL
677 678			A * 368.44+2+.52*C1-1.14*C2-1.09*C3+.58*S1-
		-	*.18*\$2+.29*\$3
679			B = .17170344*C1*.0032*C2*.0024*C3- *.0043*:10008*53
5 6 U		_	C = .09050410*C1+.0073*C2+.0015*C30034*51+.0004*S2
681			DJOD-*S3 ANGLE = -TAN (CL) *TAN (DEL)
682			SUNR = AFCOS(AHGLE)
683			TANGLE = SUNR*12./3.1415926 1F(ANGLE) 1.1.2
684 685		1	SRT = TANGLE
686		-	SST = 24SRT
687 698		,	GO TO 15 SST = 12.+TANGLE
000		٤	SRT = 12 - TANGLE
690			TIME = SHT
691 692		د	TIME = TIME+1. ITIME = TIME
693			IF(ITIME.GT.13) GO TO 90
	C C		H GIVES THE HOUR ANGLE
694			H=u=25+((12-−TIME1≈60-)*3-14159/180.
	C C		COSZ, COSW AND COSS GIVES THE DIRECTIN COSINES OF SCLAR BEAM
o 95	•		COSZ=SIN(CL)*SIN(DEL)+COS(CL)*COS(DEL)*COS(H)
696 697			51NZ=11CUSZ##21##0.5 Z=0TAN2(51NZ.COSZ)
698			Z=Z*100./3.14159
	с с		ALTI IS THE SOLAR ALTITUDE ANGLE 'BETA', IN DEGREES
699	Ŀ		ALTI 13 THE SULAR ACTIVOLE ANOLE BETA 7 IN DEGREES
700			ALTITU=2.*ATAN(1.)-2
701 702			SINP=COS4DEL}*SIN{H}/CUS{ALTITU} CUSP={1SINP**2}**Q=5
, 01	Ċ		
703	Ç		PHI IS THE SOLAR 4/IMUTH ANGLE "PHI" IN DEGREES PHI=AT4N2(SINP,COSP)#180./3.14159
704			COS4=COS(DEL)=SIN(H)
7 05			COSS=-SUFT(1=-COSH*#2-COSZ##2)
706	с		C DSH=CJS(H)
	č		T IS USED HERE AS A DUMMY ARGUMENT
707			T=(SIN(DEL)/COS(DEL)//ISIN(CL)/COS(CL)) IF(COSH.GT.T) COSS==CCSS
703	с		trichananit chaa-eesa
	č		AIDN IS DIRECT SOLAR RADIATION
709 710			AIDN= A /EXP(B /CCSZ) TA=-((SIN(DEL)/COS(DEL))*(SIN(CL)/COS(CL))}
110			IN- ISTUCATON CALCULATERS, CONTRACTION CONTRACTOR

711 712 713 714	17	IF(COSH.GT.TA) GO TO 17 Alon=C.O BL=O.O DO 16 J=1.9
715 716 717 718 719 720	C C	J=9 DENUTES THE HORIZONTAL WALL IF(J.FQ.9) GD TO 19 AZ=AZIM(J)+3.1~159/180. AN(J)=COSIAZ] 4M(J)=SIN(AZ) IF((J.EQ.6).CR.(J.EQ.7).OR.(J.EQ.8)] AM(J)=-AN(J) GO TO 20
721 722 723	19 19	BL⇒1.0 AN(J)=0.0 AM(J)=0.0
724 725 726	С 20	COST IS THE COSINE OF THE INCIDENT ANGLE "THETA" COST=EL=COSZ+AM(J)*COSW+AN(J)*CCSS AID=AIDN+CCST IFICOST-LE=U+01 AID=D+O
727 728 729 734	51 C C	Y IS CALLED DIRECT INTENSITY AND IS DEFINED AS THE RATID OF SKY . VERTICAL SURFACE TO SKY DIFFUSE ON HORIZUNTAL SURFACE Y=0.45 IF(COST.GT.(21) GO TO 21 GO TO 22 Y=0.55+0.437*COST+0.313*COST**2
731 732 733 734 735 736 737 738 739	C C 22	AISD IS DIFFUSED SOLAR RADIATION AISD= & IDN*(C = Y+R/2=0*(C +COSZ)) E=C = #AIDN IF(J=E0=9) AISD=E SUMT=0=0 SUMT=0=0 DO 9 JJ=1+6 SUMI=TAU(JJ)*COST**(JJ-1) SUMT=SUMI+SUMT SUM2=&LPHA(JJ)*COST**(JJ-1) SUM2=&LPHA(JJ)*COST**(JJ-1)
740 741 742 743 744 745 744 745 747 747 750 751 752 755 755 755 755 755	32	SUMA=SUMA+SUM2 TRANS IS TRANSMITTED SULAR HEAT THPOUGH DOUBLE-SIRENGTH GLASS BBSORB IS ABSORBED SCLAR HEAT BY DUUBLE-SIRENGTH GLASS TRANS=AID*SUMT+AISD*2.0*SHGT ABSORB=AID*SUMA+AISD*2.0*SHGT ABSORB=AID*SUMA+AISD*2.0*SHGA ANI=0.267 TOTRAD(ITIME,J) = AID*AISD B SHGF(ITIME,J) = AID*AISD B SHGF(ITIME,J) = AID*AISD DO 32 K=1,9+4 TOTRAD(24-ITIME,K) = TOTRAD(ITIME,K) SHGF(24-ITIME,K)=SHGF(ITIME,K) C CUNTINUE DO 33 K=1,3 TOTRAD(24-ITIME,9-K) = TOTRAD(ITIME,K+L) TOTRAD(24-ITIME,9-K) = TOTRAD(ITIME,K+S) SHGF(24-ITIME,5-K) = TOTRAD(ITIME,K+S) SHGF(24-ITIME,5-K) = SHGF(ITIME,K+S) SHGF(24-ITIME,5-K) = SHGF(ITIME,5-K) SHGF(
759		SUBROUTINE PEOPLE(150,NOP,GPP) THIS SUBFOUTINE IS TO CALCULATE THE HEAT GAIN DUE TO OCCUPANTS IN A ROOM NOP IS NUMBER OF PEOPLE OP IS CODEING LOAD DUE TO PEOPLE

760		GB TD {lu,20,30,40,50,60,70,80,90} , 150
761		10 OPP = 350*NOP
762		RETURN
763		20 UPP = 400 NDP
764		RETURN
765		30 OPP # 450*NOP
766 767		KETURN
768		40 QPP = 500*NOP
769		RETURN 50 &PP = \$50≉N0P
774		RETURN
771		60 QPP = 750*NCP
772		RETUPN
773		7C QPP ± 850*NOP
774		RETURN
775		80 QPP = 1000∓NJP
776		RETURN
777		90 OPP = 1450+NOP
776 779		KETURN TNO
		END
780		SUBROUTINE AIR(151,NOP,TG,TR,HO,WR,QAR)
•	C	THIS SUBFOUTINE CALCULATES THE HEAT GAINED BY VENTILATION
	č	WAR IS THE TOTAL HEAT GAIN DUE TO VENTILATION
	C	TO IS TEMPLEATURE OF OUTSIDE AIR
	C,	WE IS SPECIFIC HUMIDITY OF DUTSIDE AIR
	C	TR IS TEMPERATURE OF INSIDE AIR
	C	WR IS SPECIFIC HUMIDITY OF LASTDE ATR
	c	WAS IS SENSIBLE HEAT GAIN DUE TO VENTH ATTON
781	C	WAL IS LATENT HEAT GAIN DUE TO VENTILATION
782		W = 0.01
783		G0 TU (20:30:40:50:60:70:80];151 20 CFM ≠ 20*NOP
784		G7 TG 15
785		30 CFM # 7.5*NOP
786		GO TO 15
787		40 CFM = 10+NUP
786		GJ TU 15
783		50 CFM = 30*NOP
790		GU TU 15
741 792		60 CFM = 50*NOP
793		GO TO 15 70 CFM = 15*NOP
794		GO TO 15
795		80 CFM = 12*NuP
796		
797		QAL = CFM+60.*0.075+10.24+0.45+W]+(TO -TR) QAL = CFM+60.*0.075+1076.+(WDWR)
798		WAR = QAS +QAL
799		KETURN
600		Ë ND
801		
001	ε	SUBROITINE INFILT(152.V.TQ,TR,WO,WR,QINFL)
	č	THIS SUBROUTINE CALCULATES THE HEAT GAIN DUE TO INFILTRATION AN IS THE WATE OF AIR CHANGE OF A FOOM PER HOUR
	ĩ	USINE IS SUNSIBLE HEAT GAIN DUE TO INFILTRATION
	¢	DLINE IS LATENT HEAT GAIN DUE TO INFILTRATION
	C	GINEL IS TOTAL HEAT GAIN OUE TO INFILTEATION
	C	TO IS TEMPERATURE OF OUTSIDE AIR
	C	WO IS SPECIFIC HUMIDITY OF OUTSIDE AIR
	Ć	TR IS TEMPERATURE OF INSIDE AIR
	Ç	WR IS SPECIFIC HUMIDITY OF INSIDE AIR
- 11 P	í.	V IS THE VULUME OF A ROOM
802 603		GO TO 110,20,30,401,152 10 xN=0.5
503 504		60 TO 50
605		20 XN = 1.0
~ • • •		EV NIT - FIA

806 GU TO 50 607 30 XN = 1.5 608 60 TO 50 809 46 XN = 2.0 50 QSINF = 0.018*XN*V*(TO - 1R àL⊍ à QUINE -= 79.5±XN*V*(∦3 – ⊮Ř 1 811 = QSINE +QLINE 812 QINFL 613 PETURN E ND 014 SUBRUUTINE GLASSII53, SHGF, TO, TR, UGLASI 815 THIS SUBROUTING CALCULATES THE HEAT GAIN THROUGH GLASS SC IS SHADING COEFFICIENT DESCRIBED IN SECTION III Ç ĉ SHUE IS THE SOLAR HEAT GAIN FACTOR С U IS LVERALL HEAT TRANSISSION COOFFICIENT OGLAS IS HEAT GAINED BY DUUBLE-STRENGTH GLASS С ÷ TO IS TEMPERATURE OF OUTSIDE AIR TR IS TEMPERTURE OF INSIDE AIR C С GD TD(10,20,30,40),153 810 817 10 SC = 1.0 U=0.81 816 GU TO 50 619 82Q 20 SC = 0.76 U≄0.81 821 GO TO 50 822 30 50 = 0.90 9529 U=0.81 824 GO TO 50 825 40 SC = 0.72 826 U=0.54 827 -TR SC#SHGF +U#110 3 50 BGLAS 823 KETURN 829 630 END SUBROUTINE QWR (FU, X, Y, TR, TO, TS, Q, ALPMA, TRAD, CX1, QX2, QY1, QY2, 831 +1R +CPF THIS SUBACUTINE CALCULATES THE HEAT GRAIN THROUGH WALL OR ROUF WHICH HAS DELAYED SURFACE Ç ۵ O IS TRANSMITTED HEAT THROUGH WALL OF ROOF GIVEN BY C BY EQ.(3-5). ¢ TS(1) ARE THE WALL AND ROOF SURFACE TEMPERATURES ¢ CR IS COMMON FATIO ĉ ALPHA IS THE ABSURPTIVITY OF THE SURFACE OF THE MATERIAL ۲, FO. IS THE OUTSIDE SURFACE FILM COEFFICIENT C TRAD IS THE TUTAL SCLAR RADIATION IMPINGING UPON THE С WALL OR FOOF SURFACE. ſ. DIMENSION X(100), Y(100), TS(100) 832 833 XSUM≠0. YSUM= 0. 834 TITIETS(L) è 36 J= IR-1 835 00 1J 1=2,J 837 T2=TS(I) 838 TSCLI=T1 o 39 TDIFF=T1-TR 840 T1=T2 641 X SUM= X SUM + X(I) + TDIFF ò42 YSUM=YSUM+Y(I) *TDIFF 543 10 CONTINUE 844 DIFF=72-TR 845 DX2=CH+ (0X2-QX1)+XSUM+X{ IR}*DIFF 846 QY2=C+*(0Y2-QY1)+YSU*+Y(1R)*DIFF 647 MU2Y=IYG 648 OX1=X SUM 849 TSELF=EXELETR+FO*TO+ALPHA*TRAD-0X2J/EXELEFDJ 350 0 =0Y2+Y{1}#tTSt1+TR1 651 RETURN 85Z FND 853

SPACE NO # L

TEMPERATURE OF HALL SUPFACE (DEG F)

L	0.4.3	0.0	0.U	0.0	76.793	0.0	0.0	0.0	80.012
2	6.4	0.0	0-Q	0.0	76.683	u,c	ີ່ມີ	0.0	79.105
3	0.0	0.0	0.0	0.0	77.013	0.0	0.0	0.0	78.701
+	0.0	0.0	0.0	0.0	77.680	0.0	0.0	0.0	78./05
5	U.U	0.0	0-0	C.J	78.65)	0.0	0.U	0.0	79.JPJ
ь	0.0	0.0	ü.u	0.0	79.423	0.0	Ú,Ú	0.0	79.908
ז	0.0	0.0	0.U	0.0	63.536	0.0	J • O	0.0	87.258
8	0.0	0.0	0+0	0.0	88.031	0.0	0.0	0.0	96.725
9	Ú.U	0.0	0.0	0.0	93.350	0.0	0.0	ل ₊ ل	106.790
10	0.0	0.0	0.U	0.0	46.105	0.0	3_0	0.0	116.201
44	u_3	0.6	0.J	0.0	101-250	0.0	0.0	0.0	123.329
12	0.0	0.0	U.U	0.0	103.585	0.0	0.0	0+0	129.169
13	ပဲနယ	0-0	ن ـ ن	u _ ()	103.900	0.C	0.0	0.0	131.930
L4	0.0	0.0	ن ۵۰	0.0	103.177	0.0	0.0	0.0	132,559
15	0.0	0.0	u. 0	0.0	100-479	0.0	0_U	C.O	129.519
16	0.0	0.0	Q. U	u. 0	96.111	V.U	J.0	0+0	121.334
17	0_0	0.0	ù∎ù	0.0	91.495	0.0	0.0	0.0	115.265
19	0-0	0.0	0.0	0.0	87.017	0.0	3-0	ာ.မ	103.926
19	5.0	0.0	0.0	0.0	8+-507	0.0	4.0	0.0	97 .4 36
20	910	0.0	0. ú	0.0	82.529	0.0	0.0	0.0	92.633
21	4+0	0.0	0.3	0.0	80.BC2	0.C	0.0	0.0	28.P27
22	0.0	0.0	0.0	0-0	79.351	0.0	0.0	0.0	85.77A
23	U.J	0.0	4.5	0.0	76.178	0.0	0.0	0.0	83.334
24	0.0	0.0	Ú.U	u. 0	77.284	u.C	0.0	0.0	61.410
1	U . U	0-0	4.0	0.0	1.065	0.0	0.0	0.0	2.175
2,	0.0	0.0	0.0	0.0	0.400	0.0	0.0	c.o	1.731
ذ	0.0	0.0	0.0	0.0	0.745	0.0	0-0	0.0	1,392
4	ui⊫ U	0.0	0-0	0.0	0.606	0.0	0.0	0.0	1-145
5	0.0	0.0	0-0	0.0	0.483	0-0	0.0	0.0	0-476
6 7	0.U	0-0	0-0	لي ⊫ليا	0.301	0.0	0.0	0.0	0.654
9	0.U	0.0	0_0	J _U	0.305	0.0	0.0	0.0	0.822
9	U.U	0.0	0-0 0-0	0.0 0.0	U-255 U-244	0.0	0+3 J_0	0.0 0.0	J.990 1.668
10	0.0 0.0	0.0	0.0	0.0	0.286	0.0	0.0	0.0	2.662
11	0.0	0.0	0.0	0.0	0.195	0.0	0.0	0.0	4.015
12	4.0	0.0	0.0	0.0	0.572	0.0	0.0	0.0	5.477
13	Ú.u	ີ່ ມູ. ບໍ	0.0	0.0	0.802	0.0	0.0	0.0	6.873
14	0.0	5.0	0.0	0.0	1.054	0.0	U.0	0.0	8.086
15	v. v	0.0	0.0	0.0	1.327	0-0	5.0	6.0	6.002
Ĩ.6	ů.u	0.0	0.0	0.0	1.564	0.0	0.0	0.0	9.513
17	4.4	0.0	Ú. U	0.0	1.752	0.0	0.0	0.3	9.561
16	4 .0	0.0	0.0	0.0	1.367	0.0	0.0	c. 0	9.392
19	V.U	0. 0	0_0	0.0	1.902	0.0	U.J	u. 0	6.111
20	 	ن م آن	U = 0	0.0	1.054	0.C	0.0	0.0	5.912
21	ن.ن	0.0	មភ្ម	0.0	1.743	0.0	0.0	0.0	5.53P
22	U.U	U.C	0±0	0.0	1.592	0.0	J.O	0.0	4.425
23	U - U	υ.ū	U_ 3	0_0	1.422	0.C	0.0	0.0	3.513
24	Q and	0.0	U_0	0.0	1.244	0.0	0.0	0.0	2.774